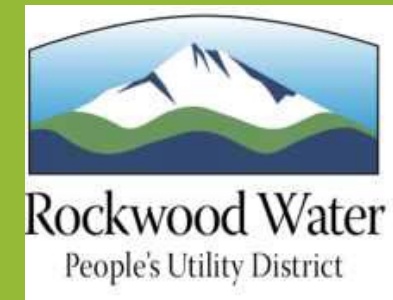


Pilot Testing for Iron and Manganese Removal: Successes and Challenges for Two Water Districts

Presented by:

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Aaron Gress, PE – Environmental Engineer (Murraysmith)



murraysmith





01

TPUD and RWPUD System Overviews

02

Pilot Testing Equipment and Setup

03

Thurston PUD – Pilot Testing and Results

04

Rockwood Water PUD – Pilot Testing and Results

05

Summary

06

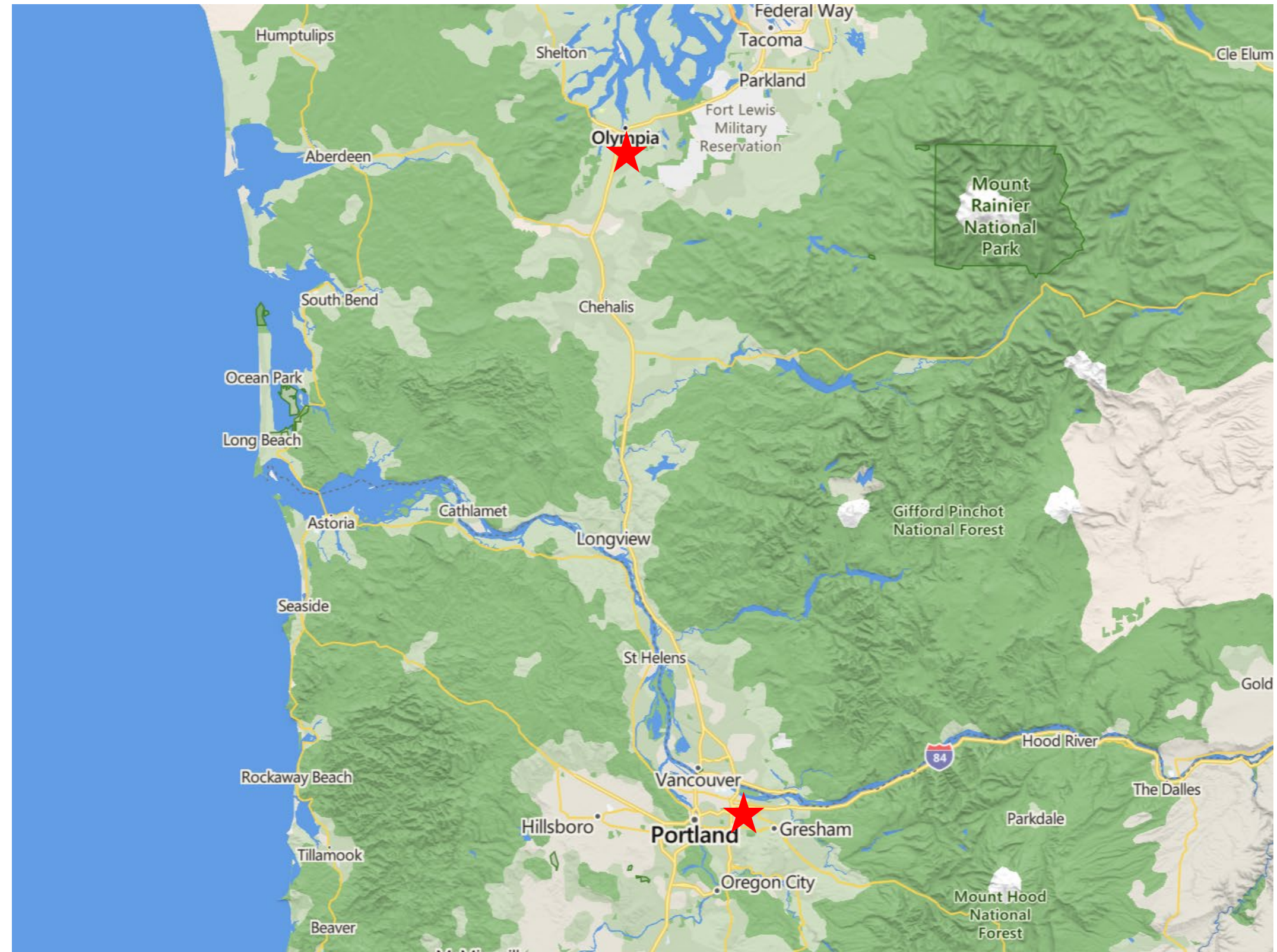
Q&A



1 - Systems Overview

A Tale of Two Water Systems

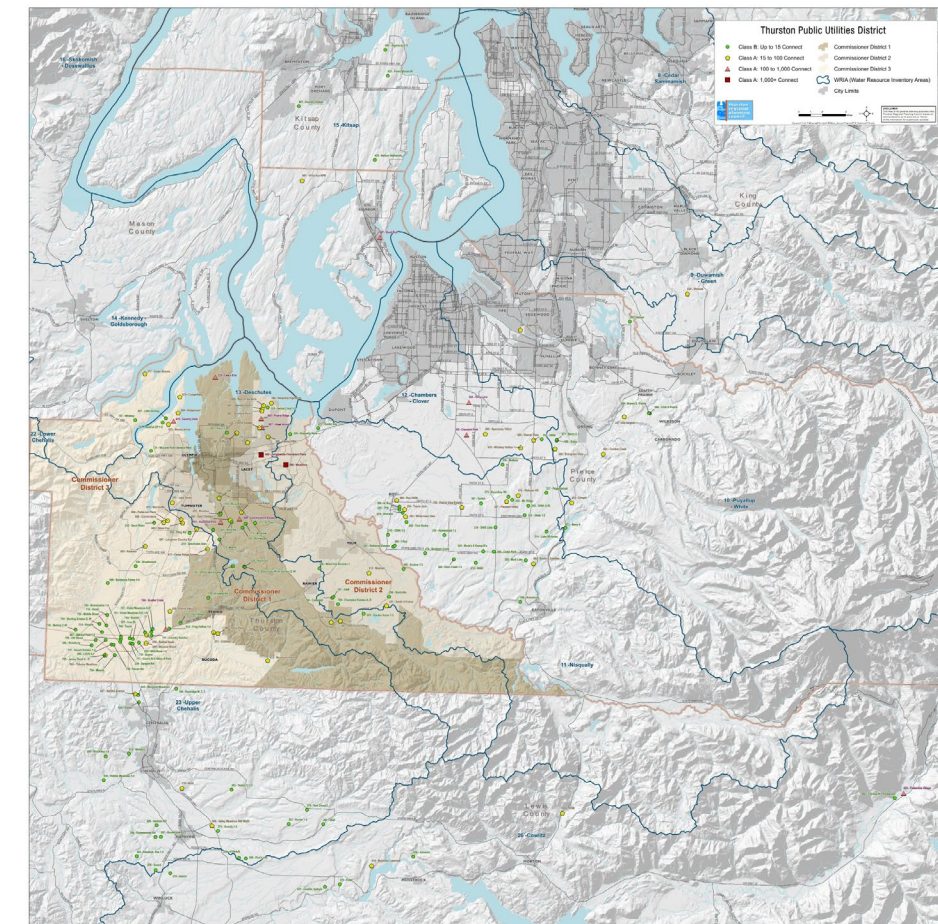
- Thurston PUD:
 - Washington
- Rockwood WPUD:
 - Oregon



TPUD System Overview

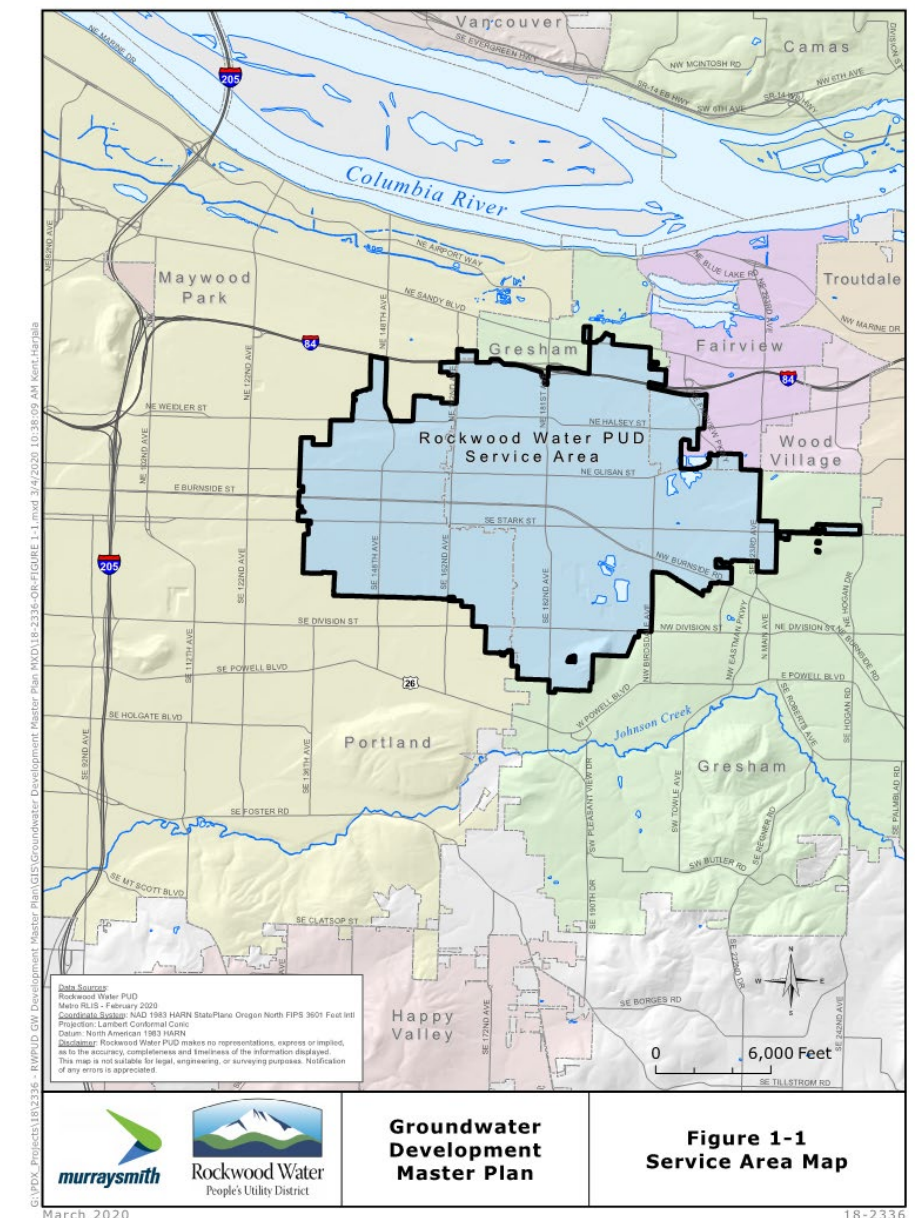
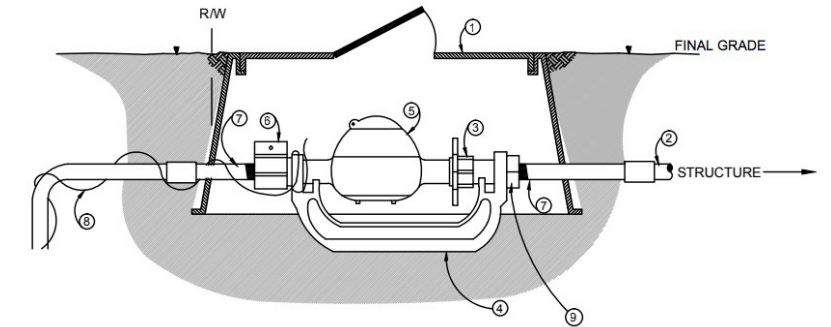


County	Number of Systems	Number of Connections
Thurston	147	5,690
Pierce	64	1,412
Lewis	54	672
Kitsap	5	28
King	1	76
Grays Harbor	4	37



Current Rockwood Water PUD System Overview

- 13,700 service connections serving approximately 65,000 residential, commercial/industrial customers in Portland, Gresham & Fairview
- 9.75 square miles
- 4 Pressure Zones
- 7 MGD average system demand
- Wholesale purchase the majority of our water from Portland Water Bureau
- Augment supply with our 3 production wells throughout the summer months





- The future of Rockwood Water PUD & City of Gresham
- Combined service to approximately 140,000 customers
- Partnering to develop groundwater as primary water source into the future
- Working together to drill 4 new wells (7 total), transmission piping, storage, disinfection & manganese removal treatment for 30 MGD by 2026
- Manganese removal is a significant part of this effort which is why we had MSA come out and do some pilot testing for us

The EPA has set a Secondary MCLs (not health threatening) for Iron and Manganese as concentrations above the SMCL can cause discoloration, staining and a bitter or metallic taste.



Iron SMCL .3mg/L

Rusty color; sediment;
metallic taste; reddish or
orange staining

Manganese SMCL .05mg/L

Black to brown color;
black staining; bitter
metallic taste

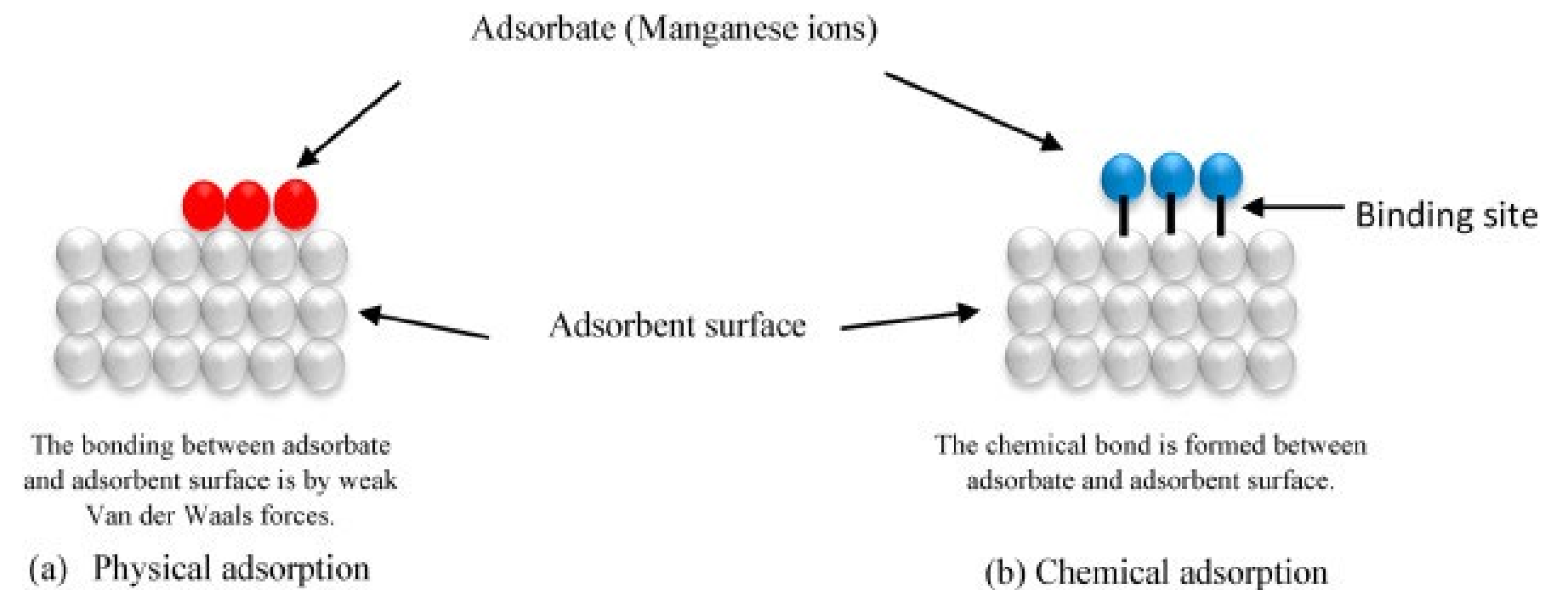
RWPUD Current Fe & Mn

Iron: <.1 mg/L
Manganese: >.1 mg/L

2 - Pilot Testing Equipment and Setup

Removal Mechanisms

- Precipitation,
- Adsorption,
- Ion exchange, and
- Biological uptake.



- Pilot testing setup is designed to maximize precipitation and adsorption mechanisms
 - Oxidation Using Chlorine and/or Permanganate
 - Adsorption using Oxidized Pyrolusite Media

Pilot Testing Equipment:

- Two Stage Filters
- 4" Columns
- 6" Gravel Under-Drain
- 42" Manganese Dioxide Media



Pilot System Design Criteria

Criteria	Value
Plant Capacity (gpm)	8
Operating Pressure, psig	75
Run Time (hours/day)	12
Average Day Run Time (hours/day)	12
Pilot Filters	
Diameter of Vessels, ft	0.33
Surface areas, per vessel, sq ft	0.1
Number of Vessels	4 (1 st Stage) and 4 (2 nd Stage)
Loading Rate, gpm/sq ft	5-12
Media Depth, in	42
Media Volume, Cubic ft	1.2
Media Weight, lbs	143
Backwash	
Backwash Flow Rate, Each Vessel	1.3
Backwash Frequency, Hrs	24
Backwash Duration (min)	5
Backwash Volume, Gal/Backwash	26
Number of Backwashes Per Day	1
Backwash % of Production	0.22%
Chlorine	
Dose, mg/L	4.0
Dose (lbs/day)	0.1
Solution Strength	8.9%
Solution Feed Rate (gal/hr) each	0.01
Chemical Feed Tanks	1
Chemical Feed Tank Volume (gal)	5
Tank Storage (days)	40

2

Pilot System – Chemical Feed Equipment



STENNER PUMPS

**Stenner Single Head
Adjustable Output Pump
0.2 - 3 GPD #1 Tube 120V
25 psi**

Part Number: 45MJL1A1S

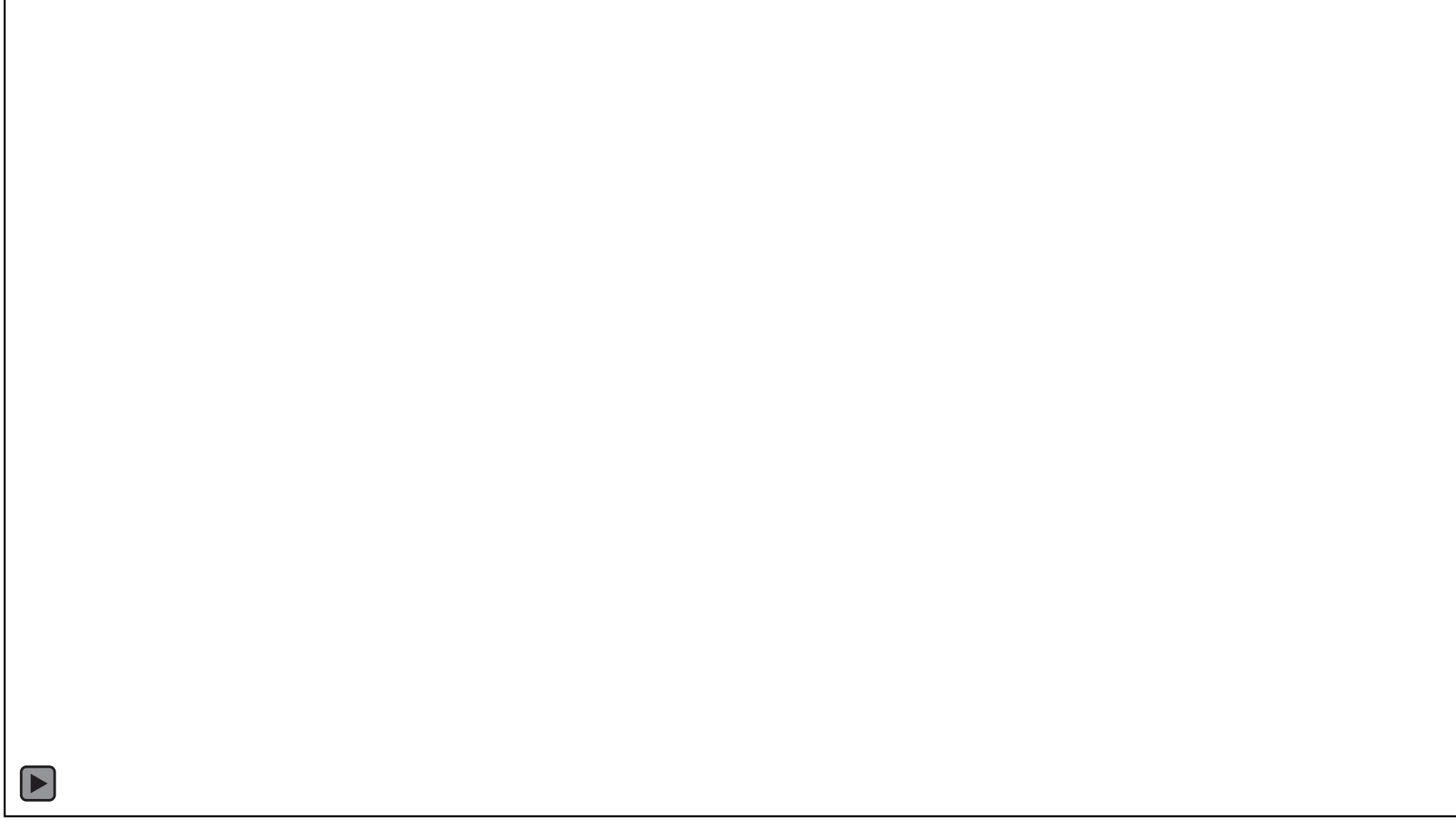


45 SERIES PUMP ADJUSTABLE OUTPUT

Single Head Model	Maximum Pressure	Pump Tube Number	Approximate Output @ 60 Hz						Approximate Output @ 50 Hz		
			gallons per day	liters per day	gallons per hour	liters per hour	ounces per minute	milliliters per minute	liters per day	liters per hour	milliliters per minute
45MHP2* 45M1	100 psi (6.9 bar) 25 psi (1.7 bar)	#1 #1	0.2 to 3.0	0.8 to 11.4	0.01 to 0.13	0.03 to 0.48	0.02 to 0.27	0.56 to 7.92	0.6 to 9.1	0.03 to 0.38	0.31 to 6.32
45MHP10* 45M2	100 psi (6.9 bar) 25 psi (1.7 bar)	#2 #2	0.5 to 10.0	1.9 to 37.9	0.02 to 0.42	0.08 to 1.58	0.04 to 0.89	1.32 to 26.32	1.5 to 30.3	0.06 to 1.26	1.04 to 21.04
45MHP22* 45M3	100 psi (6.9 bar) 25 psi (1.7 bar)	#7 #3	1.1 to 22.0	4.2 to 83.3	0.05 to 0.92	0.18 to 3.47	0.10 to 1.96	2.92 to 57.85	3.3 to 66.6	0.14 to 2.78	2.29 to 46.25
45M4	25 psi (1.7 bar)	#4	1.7 to 35.0	6.4 to 132.5	0.07 to 1.46	0.27 to 5.52	0.15 to 3.11	4.44 to 92.01	5.1 to 106.0	0.21 to 4.42	3.54 to 73.61
45M5	25 psi (1.7 bar)	#5	2.5 to 50.0	9.5 to 189.3	0.10 to 2.08	0.40 to 7.89	0.22 to 4.44	6.60 to 131.46	7.6 to 151.4	0.32 to 6.31	5.28 to 105.14

*Pump supplied with injection check valve for 26-100 psi (1.7-6.9 bar) applications





- Field Testing
 - HACH DR900
 - RW & FW
 - Iron & Manganese
 - Chlorine: Free & Total
 - H₂S
 - Ammonia
 - pH, temp, Pressure Drop



- Lab Testing
 - RW & FW
 - Iron & Manganese
 - Ammonia
 - Arsenic
 - Alkalinity
 - Ca, Cl, Na
 - Radon



3 - Thurston PUD:

Pilot Testing and Results

Testing Approach:

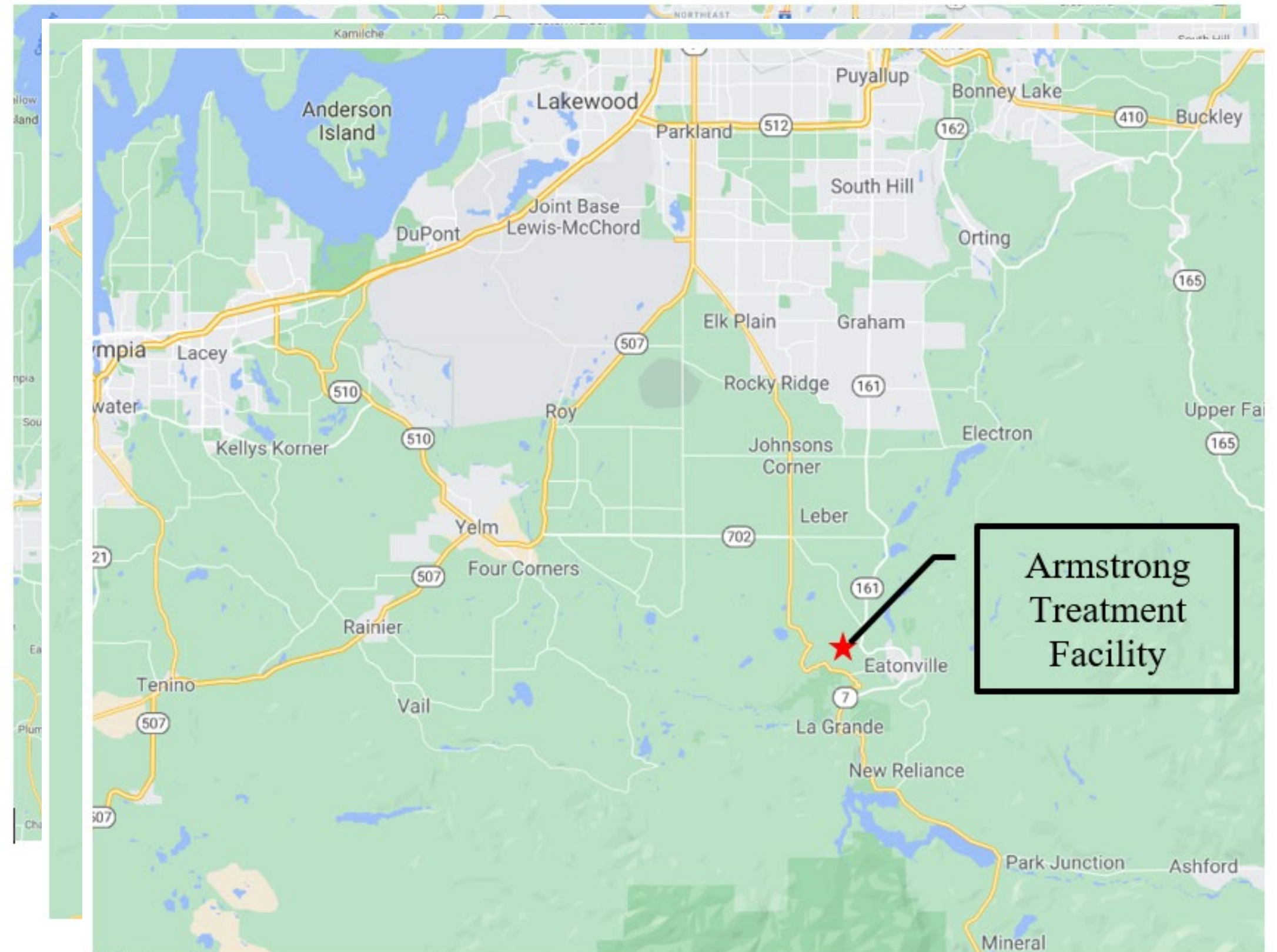
- Tested at 3 Locations:
 - Webster Hill
 - Eastridge West (2 Days of Testing)
 - Armstrong
- Observed elevated concentrations of Iron and Manganese at all sites
- Individual site challenges
- 20 – 100 gpm design capacity range
- 1 stage filtration and 2 stage filtration
- Chemical Feed: Chlorine, Permanganate
- Media: Pylox Advantage



Physical	Black granular media
pH Range	6.4–9.5
Max. Water Temp	115 degrees F
Specific Gravity	
Minimum Bed Depth	24"
Effective Size	
Freeboard	Minimum 40%
Uniformity Coefficient	< 1.8
Service Flow Rate	2 - 12 gpm/sq. ft.
Mesh Size	20 x 40
Bulk Density	88 lbs./sq. ft.
Backwash Flow Rate	10-20 gpm/sq. ft.
Backwash Expansion	15 - 50%
Packaging	20 or 1,000 kilo bags

Site Locations

- Webster Hill
 - Graham, WA
- Eastridge West
 - Centralia, WA
- Armstrong
 - Eatonville, WA

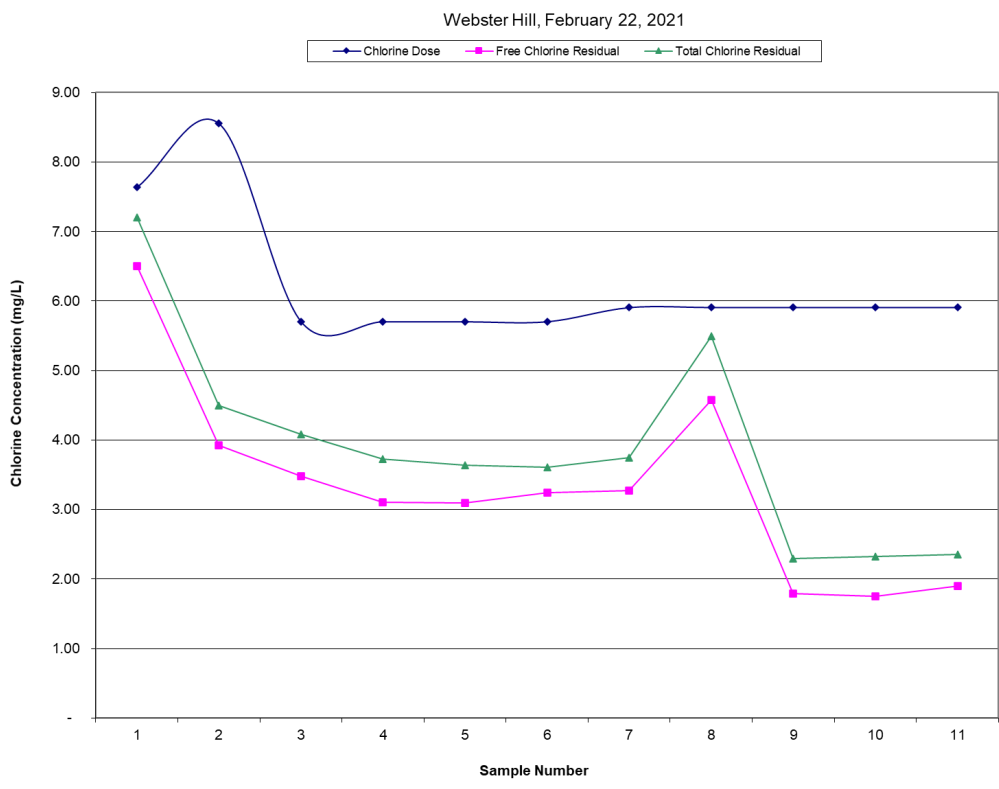


System Overview and Raw Water Quality

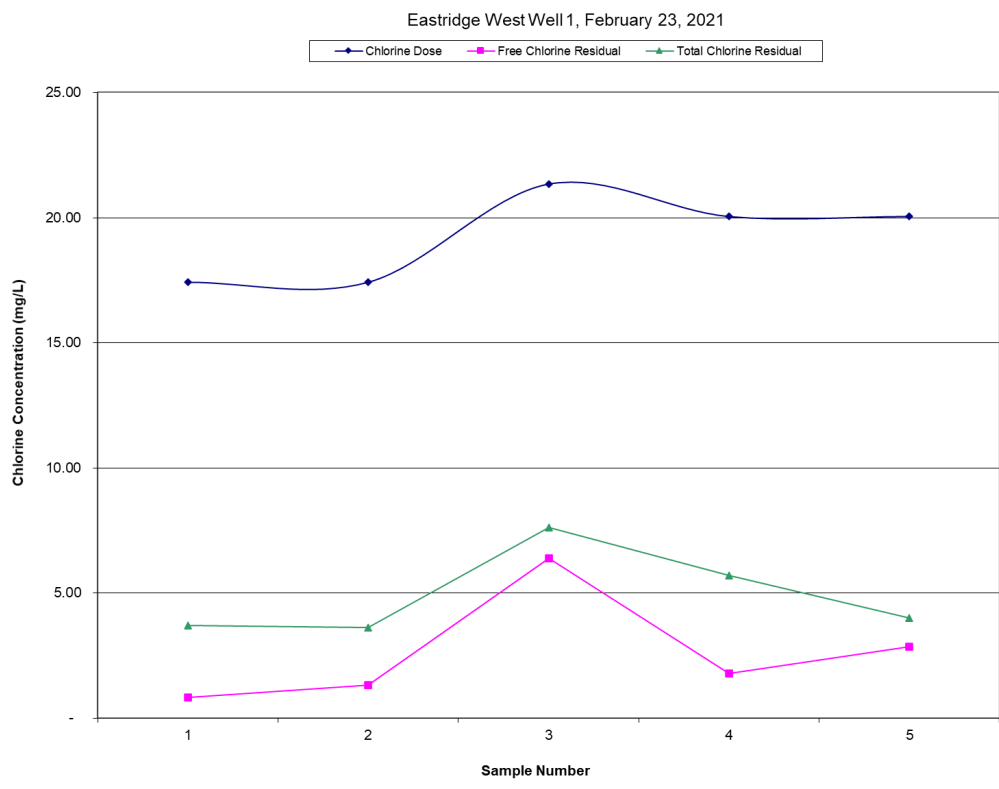
Planning Criteria	Webster Hill	Eastridge West	Armstrong
Well No. 1 Operating Flow, gpm	100	20	30
System Pressure, psi	75	75	75
Raw Water Quality			
pH, S.U.	6.3	6.49	7.87
Temperature, °C	15-20	15-20	15-20
Conductivity, umhos/cm ²	-	-	-
*Total Hardness, mg/L as CaCO ₃	58	96	40
Iron, Total, mg/L	0.08	8.7	2.7
Manganese, Total, mg/L	0.196	0.68	0.40

Chlorine Dosing

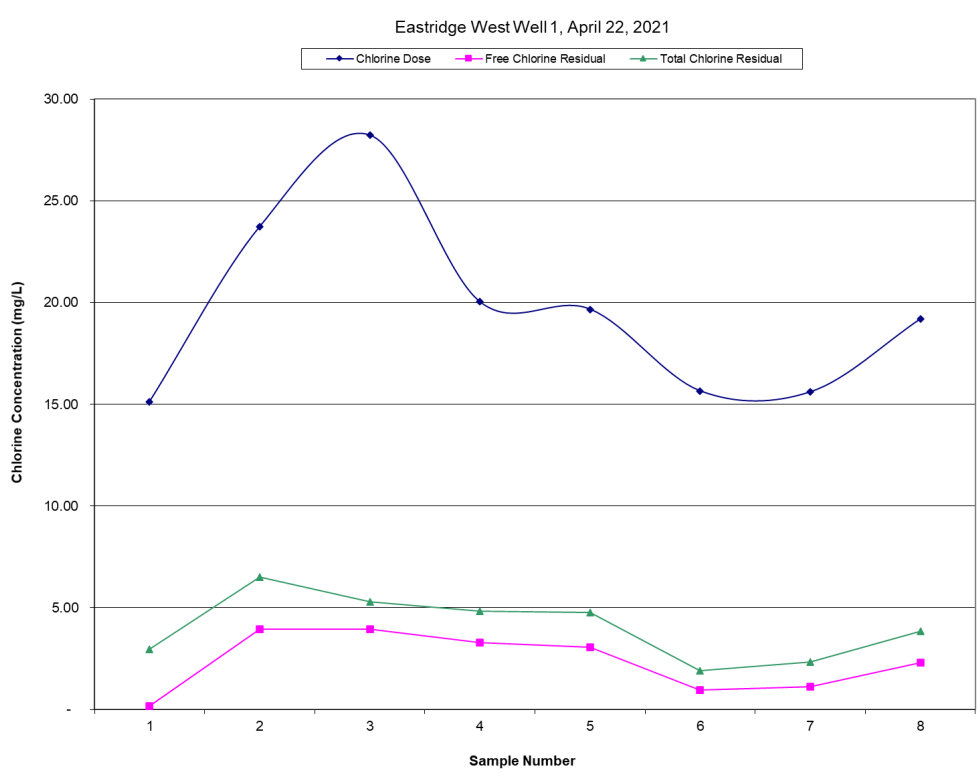
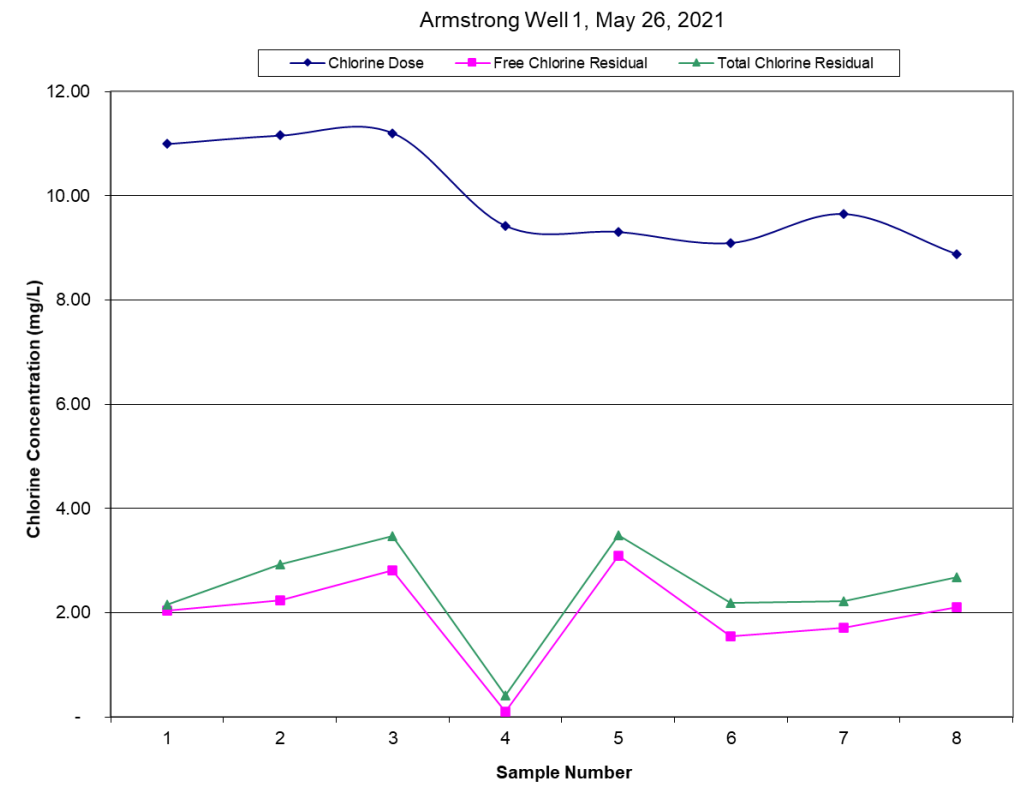
Webster Hill



Eastridge West

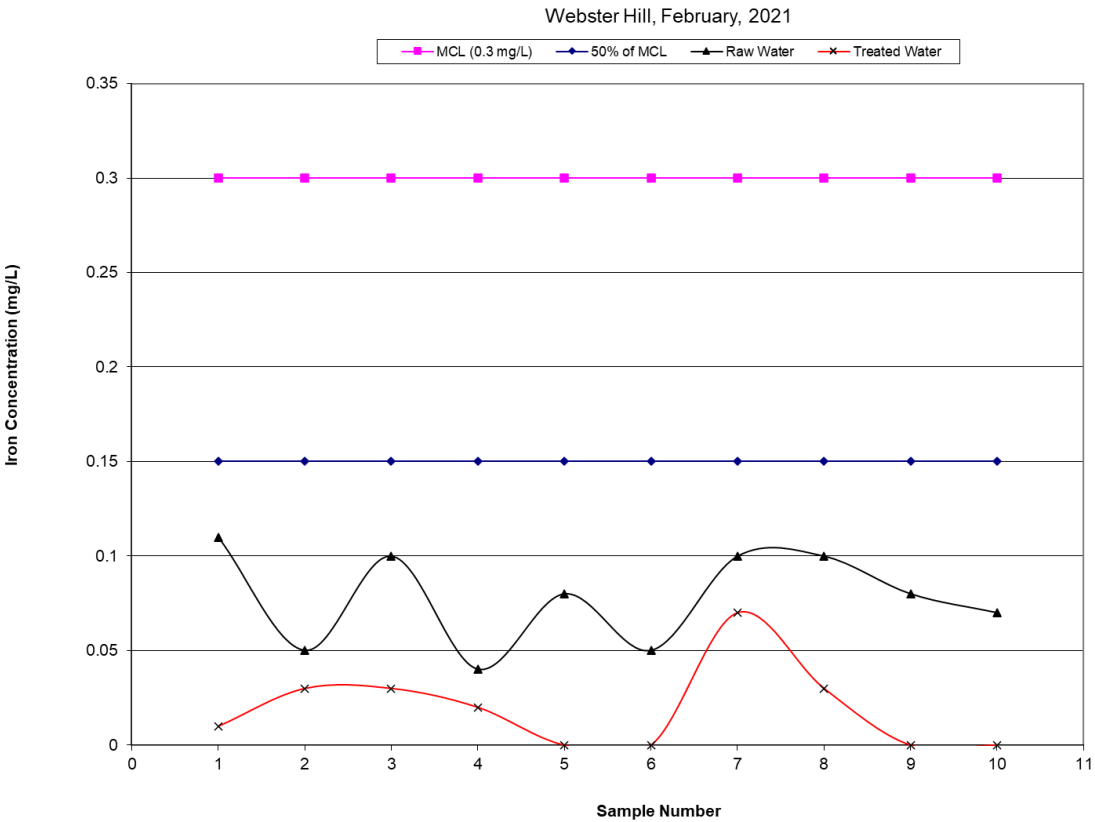


Armstrong

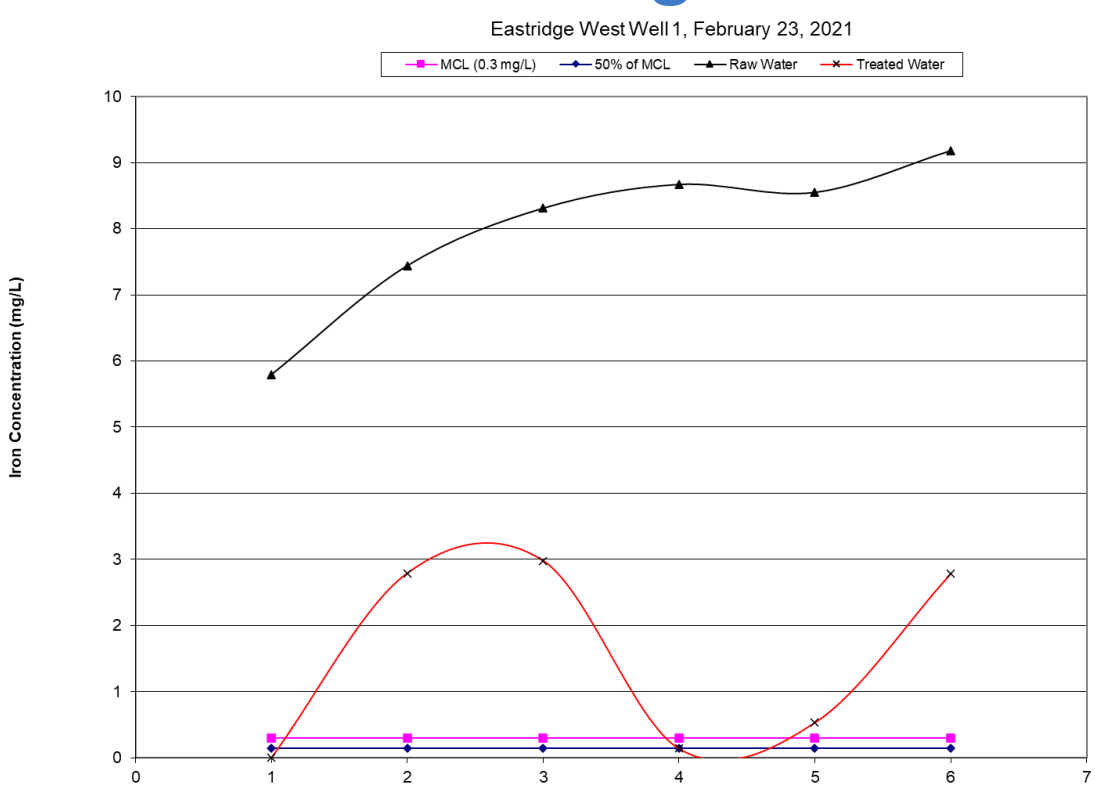


Iron Removal

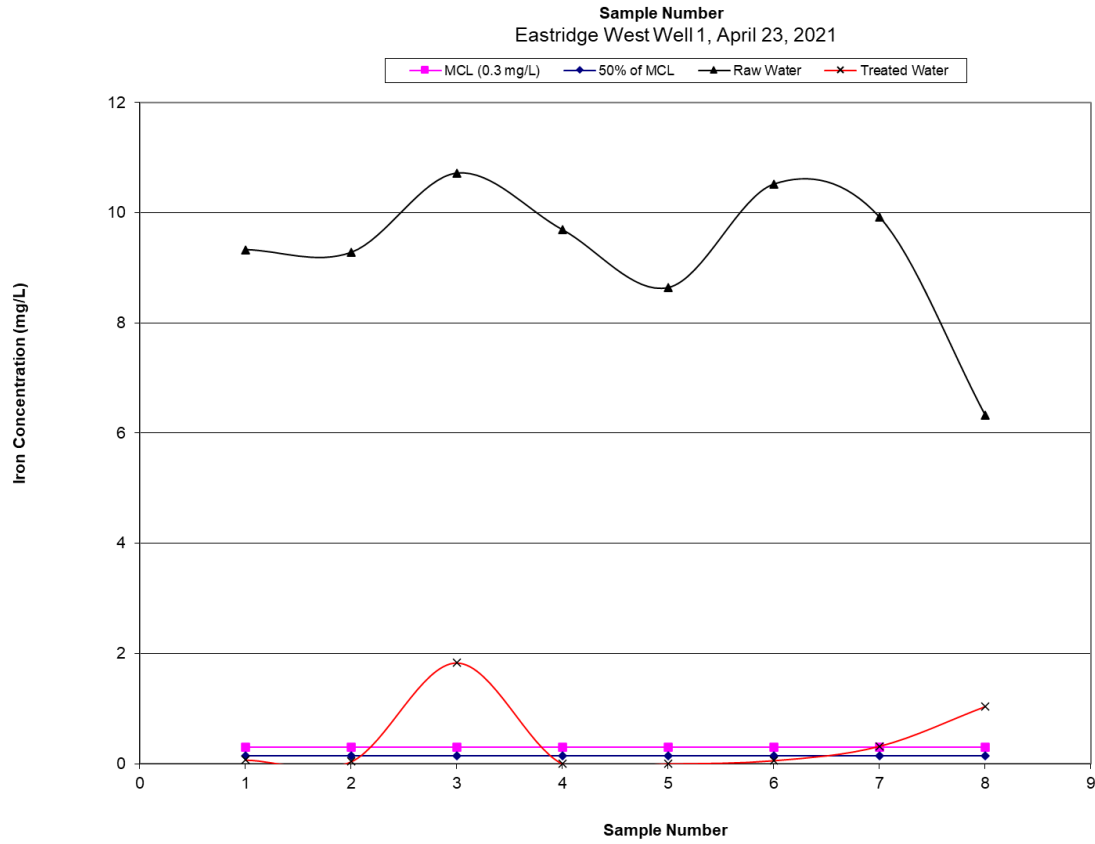
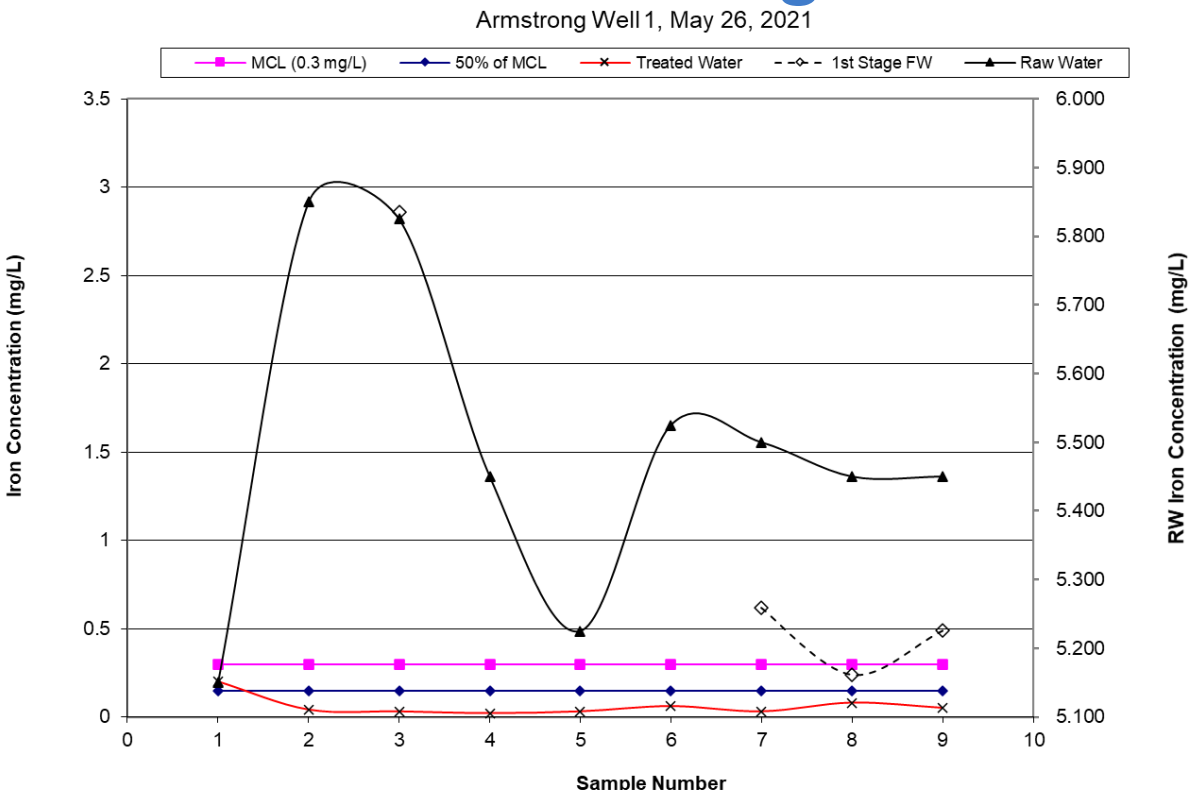
Webster Hill



Eastridge West

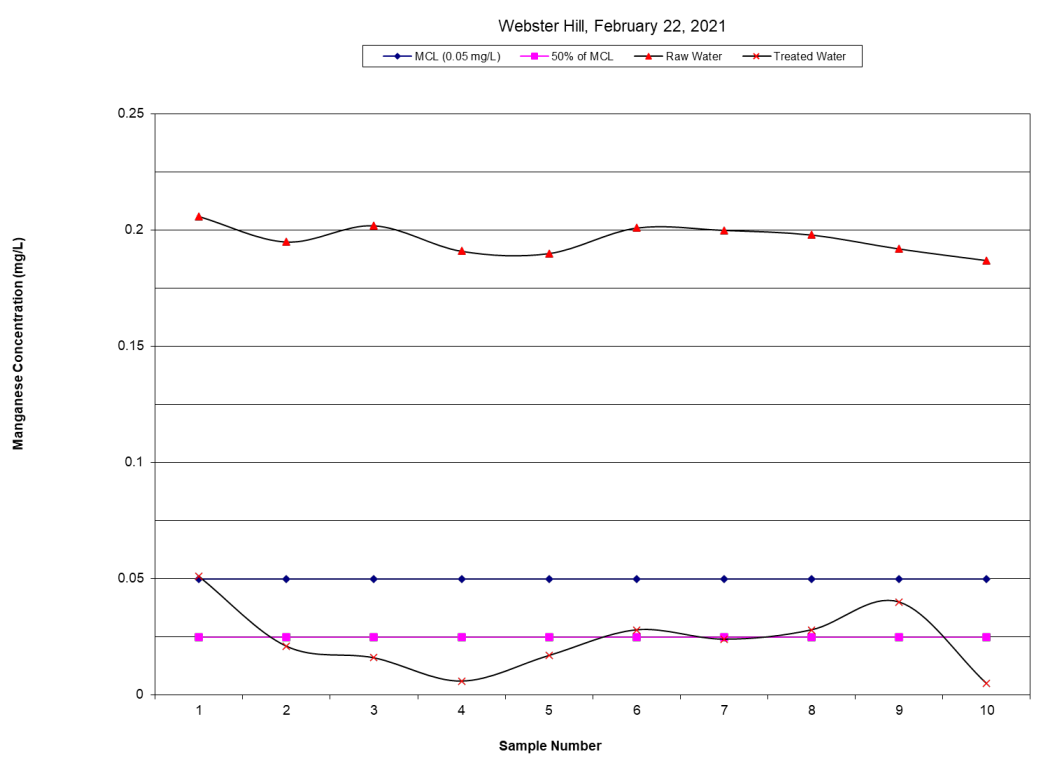


Armstrong

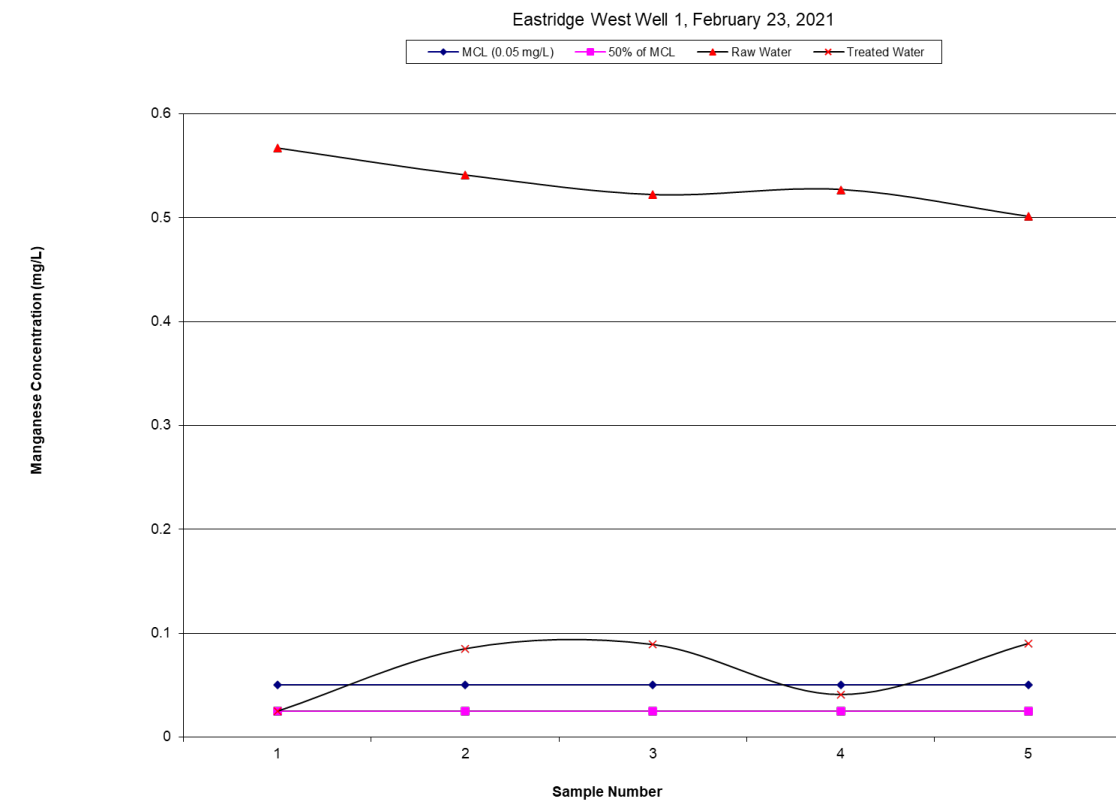


Manganese Removal

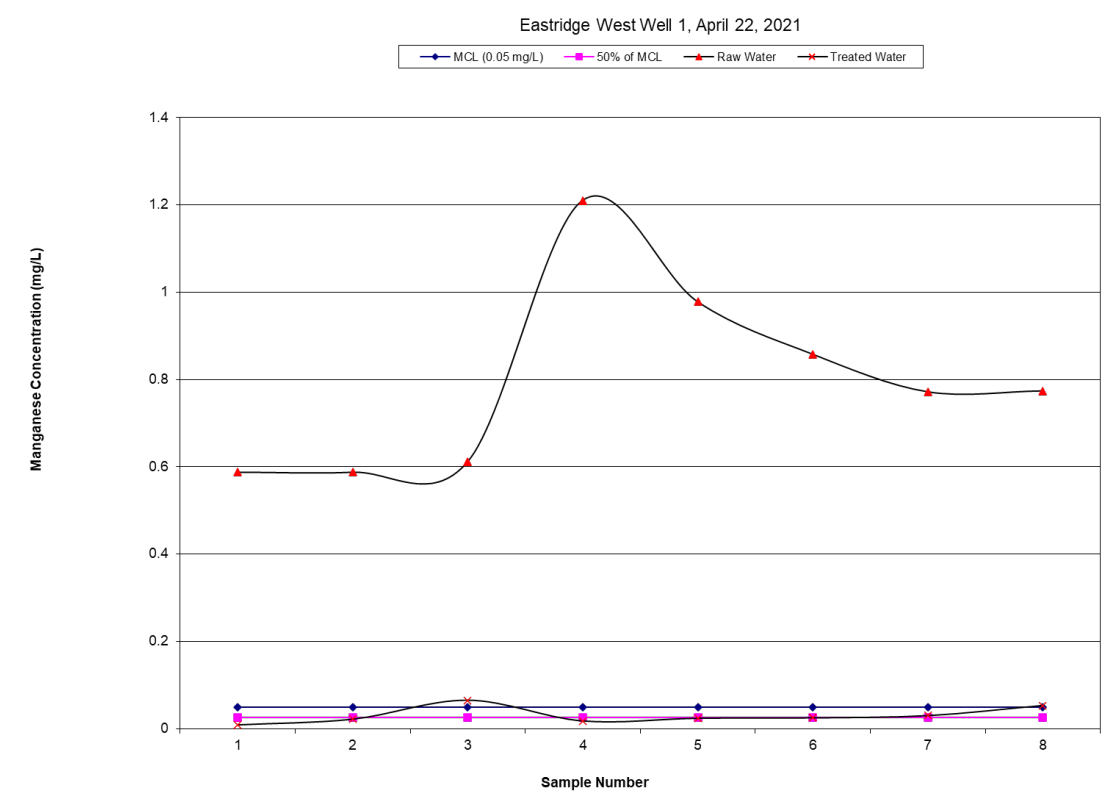
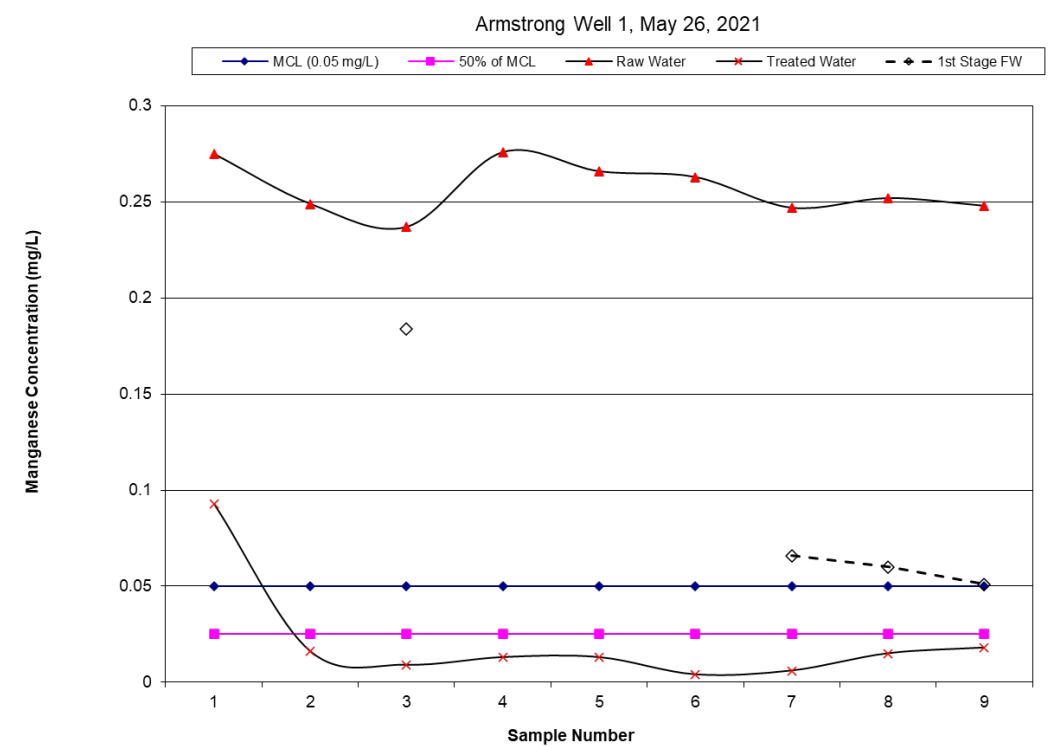
Webster Hill



Eastridge West



Armstrong



4 - Rockwood WPUD: *Pilot Testing and Results*

Piloted Wells & Planned Treatment Facilities Testing Completed between Dec. '20-Apr. '21

- Cascade Facilities
 - Well 3 – 3.6 MGD (Piloted)
 - Well 4 – 6.6 MGD (Piloted)
 - Well 5 – 7.8 MGD (Piloted)
 - Well 7 – 5.7 MGD
 - Well 9 – 4.3 MGD (Piloted)
 - Total = 30 MGD peak capacity**
- 141st WTP
 - Not Piloted
 - 2-5 MGD
- Cascade Well 6 Plant
 - Not Piloted
 - 5 MGD



4

Testing Approach:

- Tested 2 Types of Media
 - Prince Minerals
 - Pyrolox
 - Pyrolox Advantage
- Cl₂ Adjustment: 2-4 mg/L
- Loading Rates: 4-12 gpm/sf



- ADVANTAGES**
- Effective reduction of iron, manganese and hydrogen sulfide
 - Durable media with long service life
- PHYSICAL PROPERTIES**
- Color: Black
 - Bulk Density: 120 lbs./cubic foot
 - Mesh Sizes: US 8 x 20, US 20x40, UK 18/44
 - Specific Gravity: 3.8
 - Packaging: 60 lb. bags, 2,000 or 2,205 lb. super sacks
- CONDITIONS FOR OPERATION**
- pH: 6.5-9.0
 - Bed Depth: Suggested depth 18 inches. Dependent on application and water quality.
 - Backwash Flow Rate: 25-30 gpm/sq.ft.
 - Freeboard: 40% of bed depth (min.)
 - Underbed: Garnet #8, #8-#12. #3 Silica. Other materials are also suitable but must keep media from migrating downward and be heavy enough to remain in place during backwash.
 - Service flow rate: 5 gpm/sq. ft.

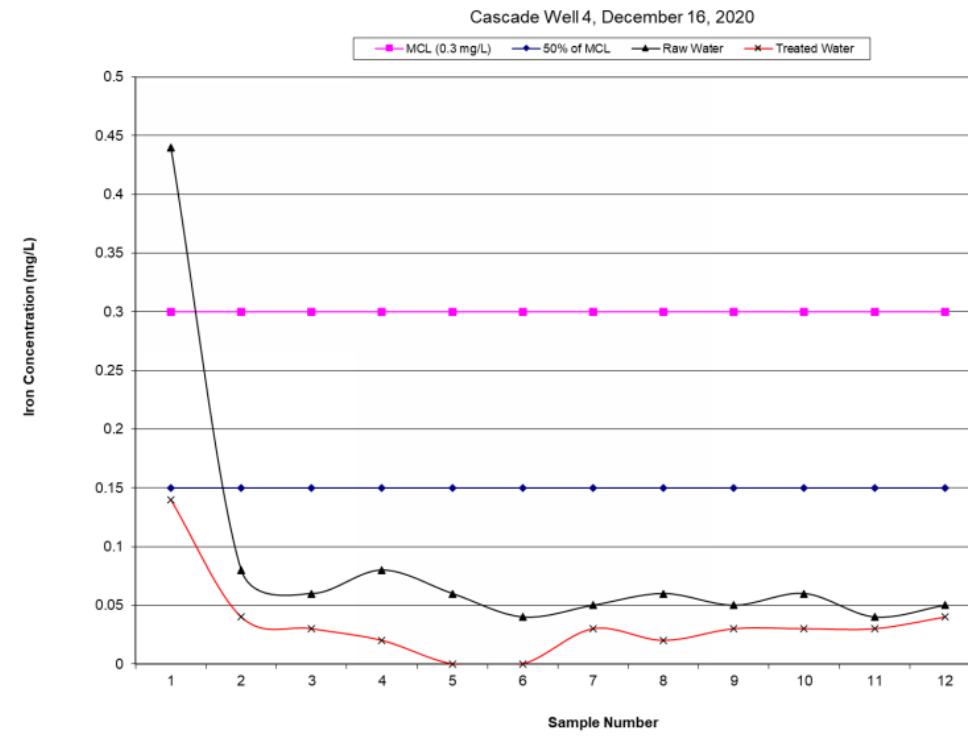


Physical	Black granular media
pH Range	6.4–9.5
Max. Water Temp	115 degrees F
Specific Gravity	
Minimum Bed Depth	24"
Effective Size	
Freeboard	Minimum 40%
Uniformity Coefficient	< 1.8
Service Flow Rate	2 - 12 gpm/sq. ft.
Mesh Size	20 x 40
Bulk Density	88 lbs./sq. ft.
Backwash Flow Rate	10-20 gpm/sq. ft.
Backwash Expansion	15 - 50%
Packaging	20 or 1,000 kilo bags

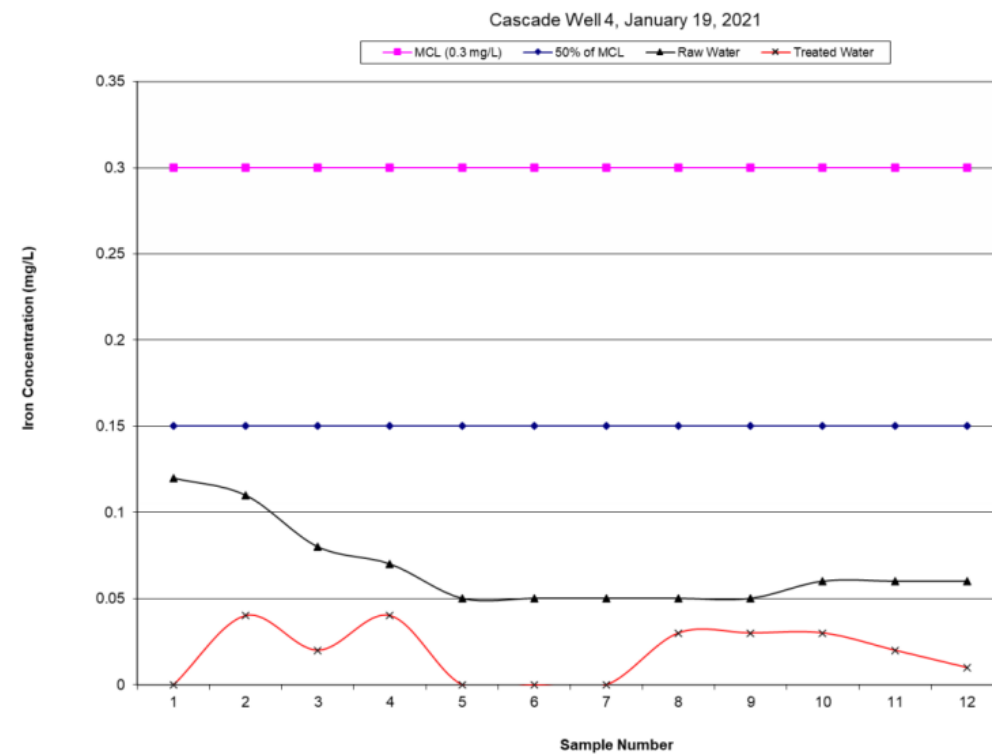
Results of Well 4 (Highest Mn Concentrations)

Iron

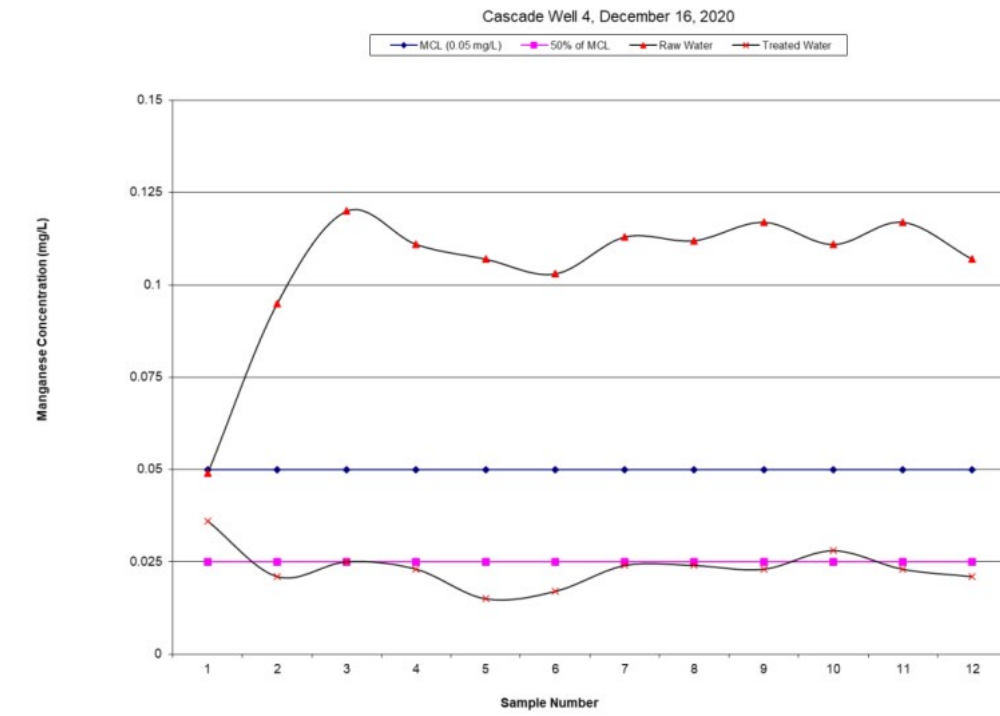
Manganese



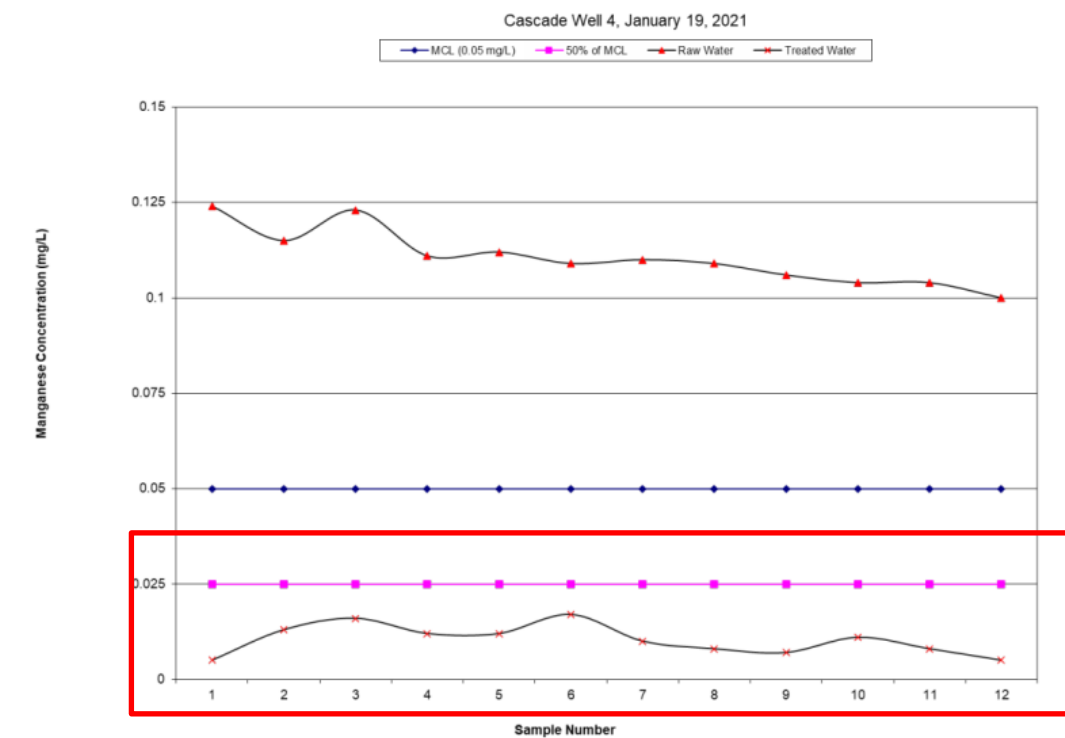
Pyrolox



Pyrolox Advantage



Pyrolox



Pyrolox Advantage

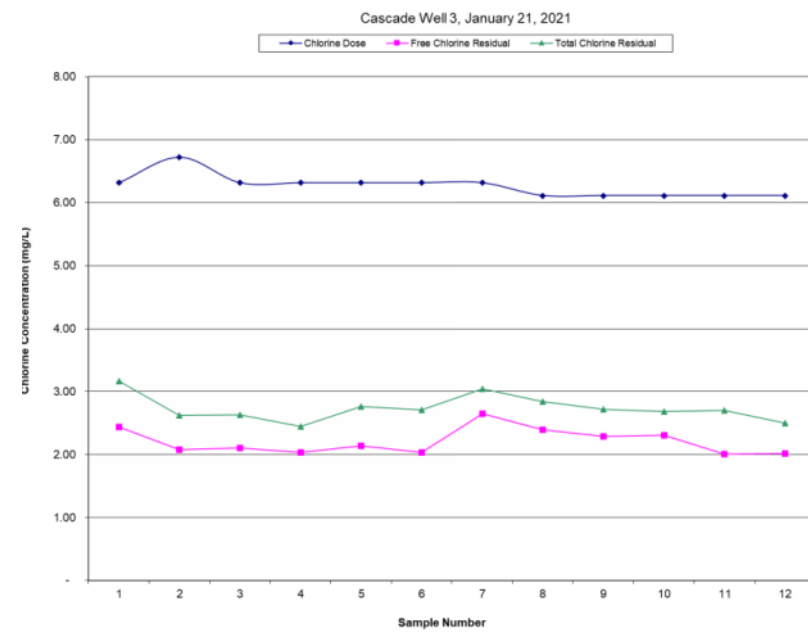


Figure 4-3. Well 3 Free and Total Chlorine Residual Concentrations

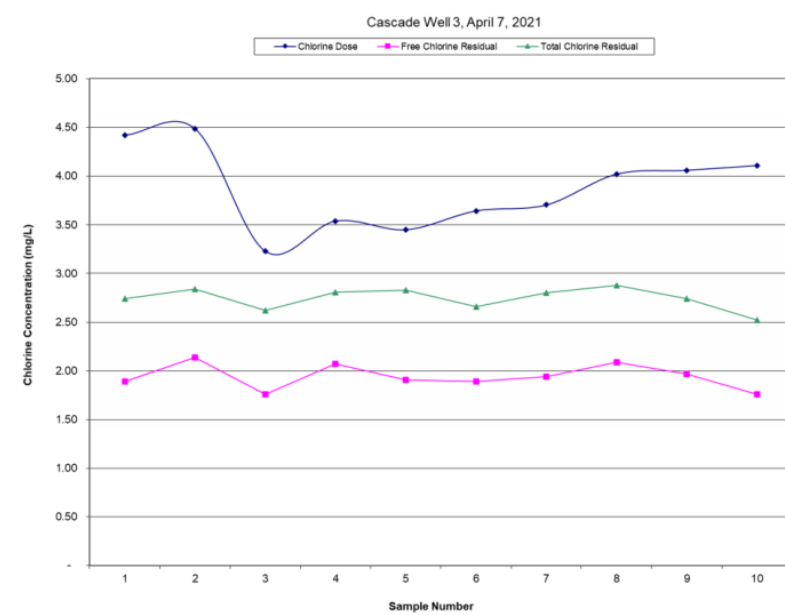


Figure 4-4. Well 3 (with High Loading Rate) Free and Total Chlorine Residual Concentrations

Well 3

Typical Chlorine Demands

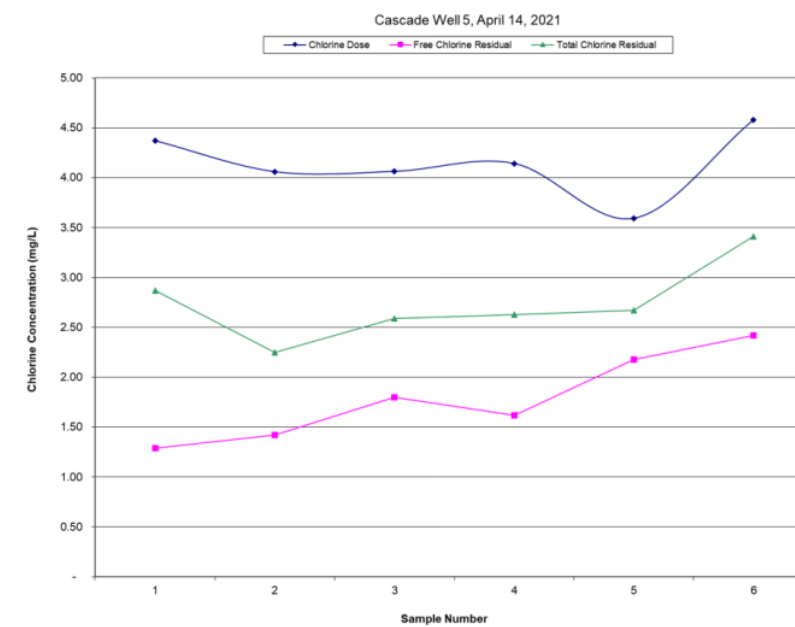
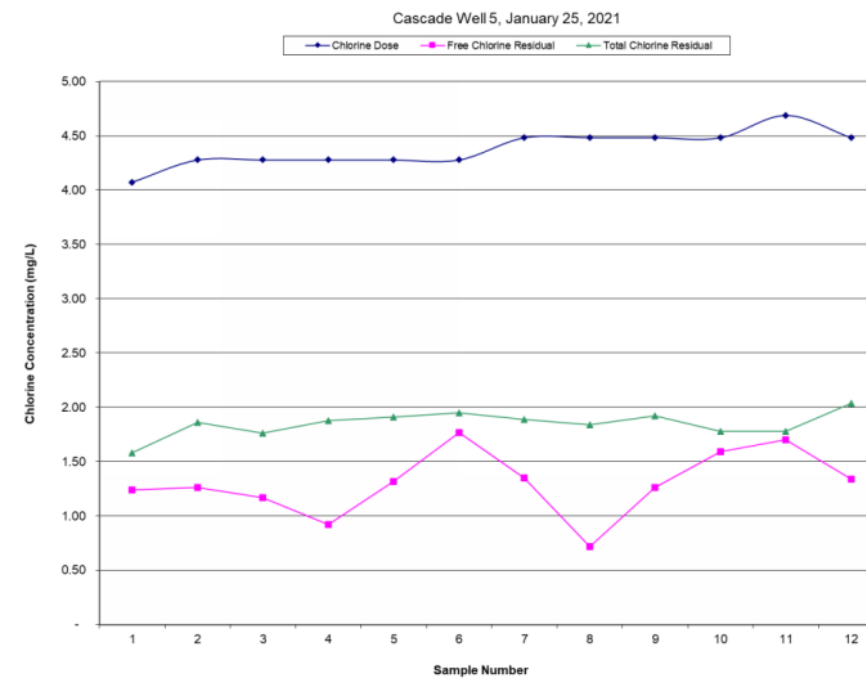


Figure 4-8. Well 5 (with High Loading Rate) Free and Total Chlorine Residual Concentrations

Well 5

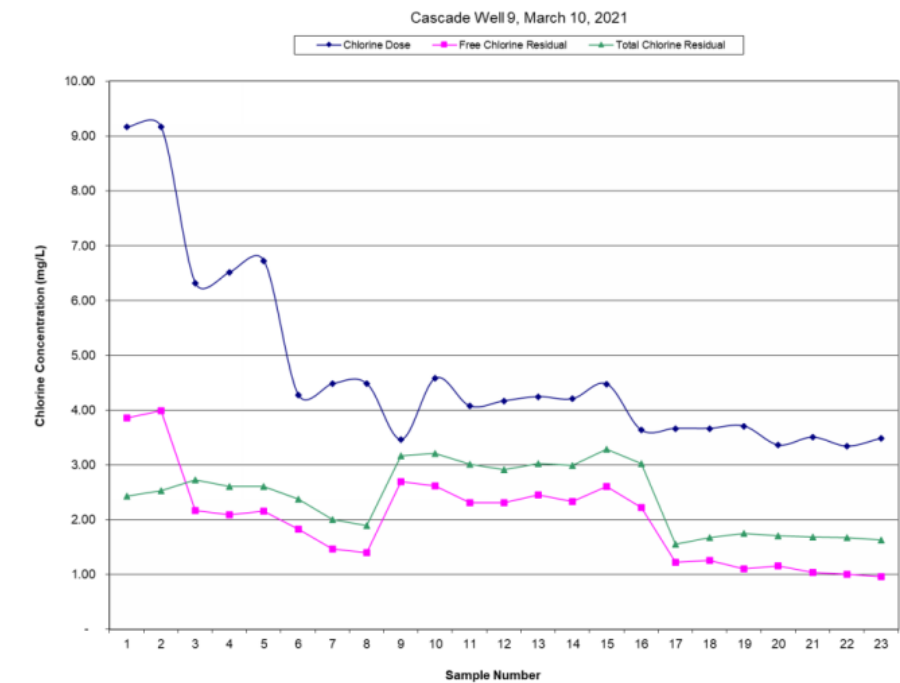


Figure 4-9. City of Gresham Well 9 Free and Total Chlorine Residual Concentrations

Well 9

4

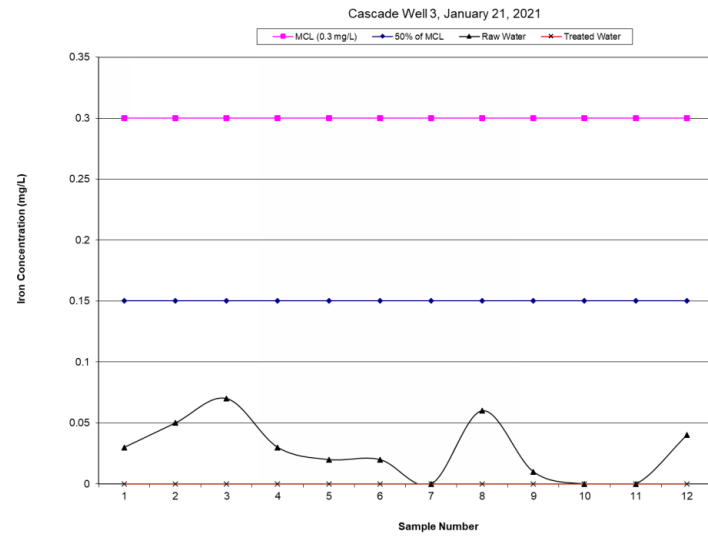


Figure 4-10. Well 3 Iron Concentrations

5.92 gpm/sf (avg)

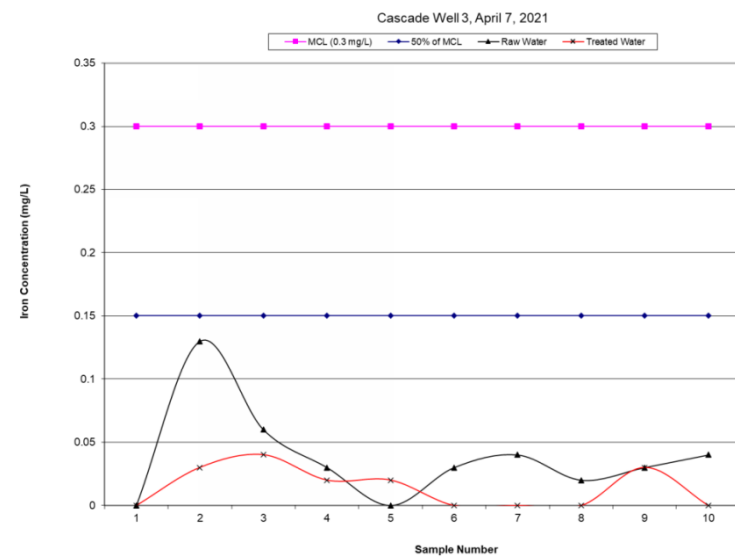


Figure 4-11. Well 3 (with High Loading Rate) Iron Concentrations

12.23 gpm/sf (avg)

Well 3

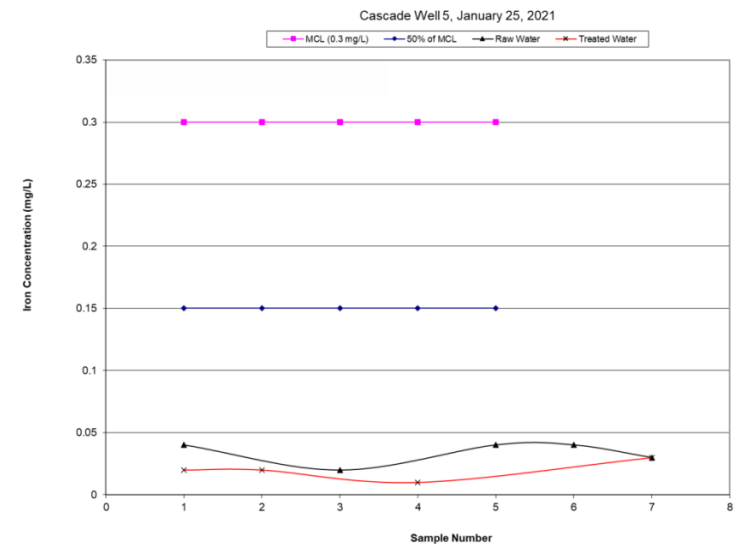


Figure 4-14. Well 5 Iron Concentrations

7.78 gpm/sf (avg)

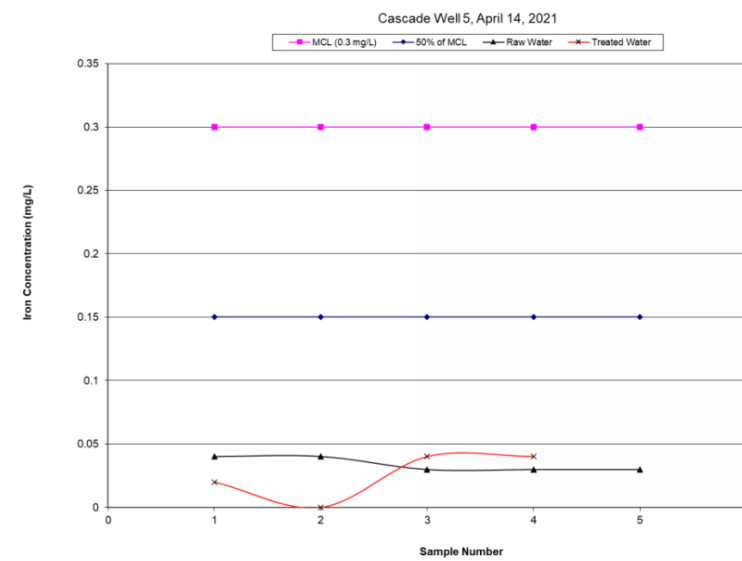


Figure 4-15. Well 5 (with High Loading) Iron Concentrations

11.09 gpm/sf (avg)

Well 5

Iron Removal

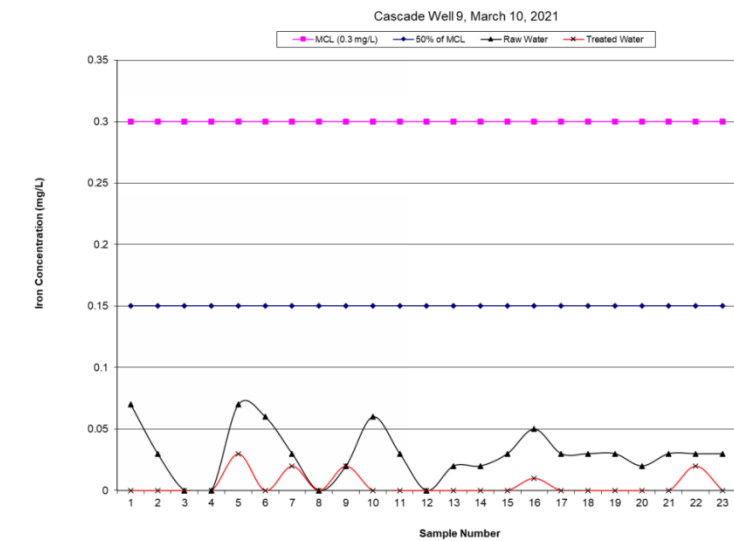


Figure 4-16. City of Gresham Well 9 Iron Concentrations

8.78 gpm/sf (avg)

Well 9

4

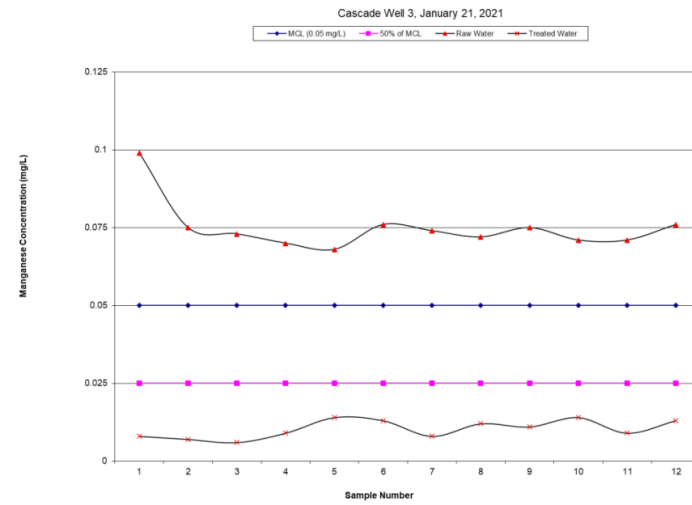


Figure 4-17. Well 3 Manganese Concentrations

5.92 gpm/sf (avg)

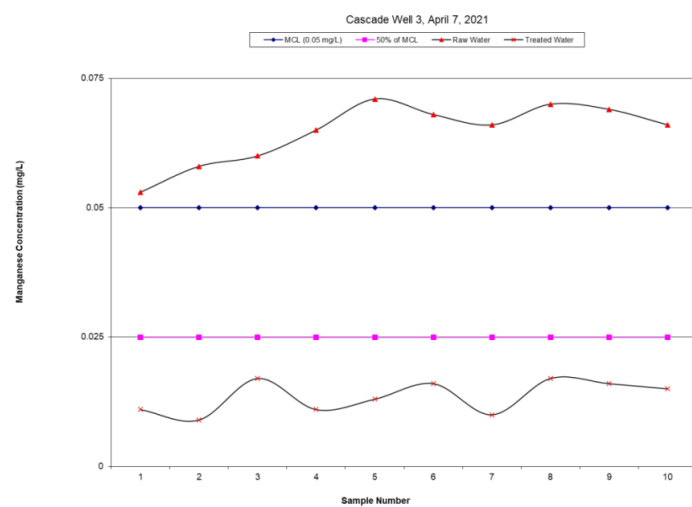


Figure 4-18. Well 3 (with High Loading Rate) Manganese Concentrations

12.23 gpm/sf (avg)

Well 3

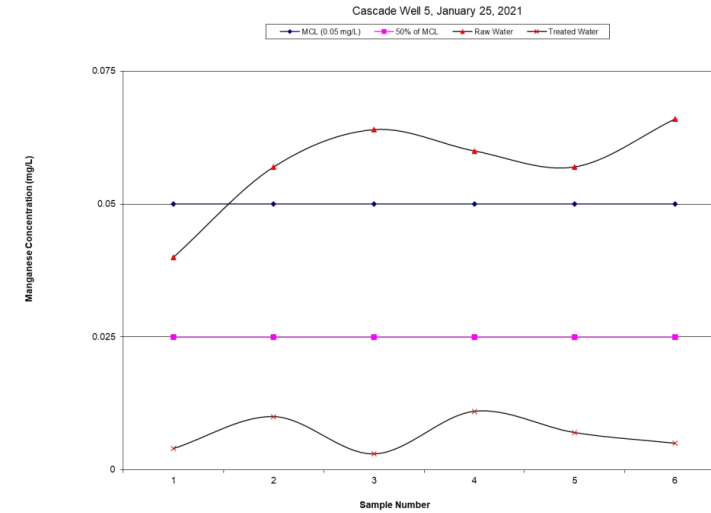


Figure 4-21. Well 5 Manganese Concentrations

7.78 gpm/sf (avg)

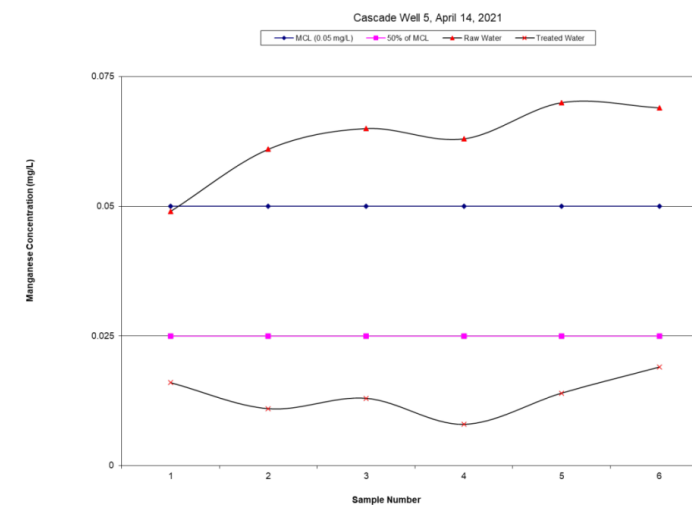


Figure 4-22. Well 5 (with High Loading Rate) Manganese Concentrations

11.09 gpm/sf (avg)

Well 5

Manganese Removal

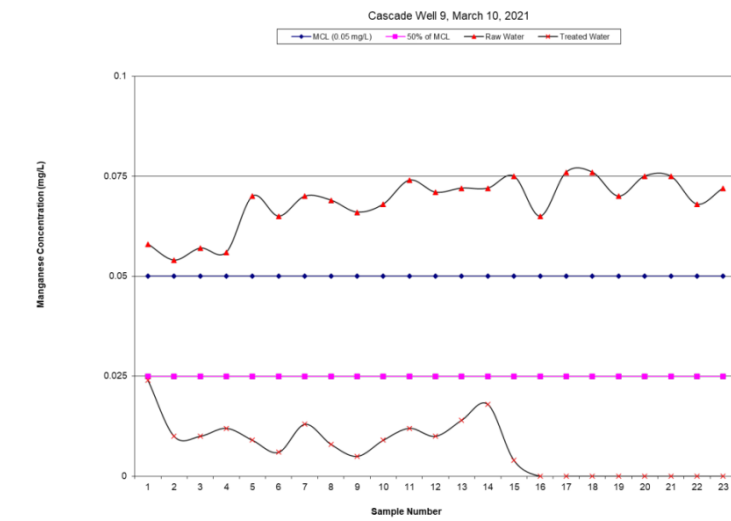


Figure 4-23. City of Gresham Well 9 Manganese Concentrations

8.78 gpm/sf (avg)

Well 9

Manganese Removal Efficiency vs Loading Rate

4

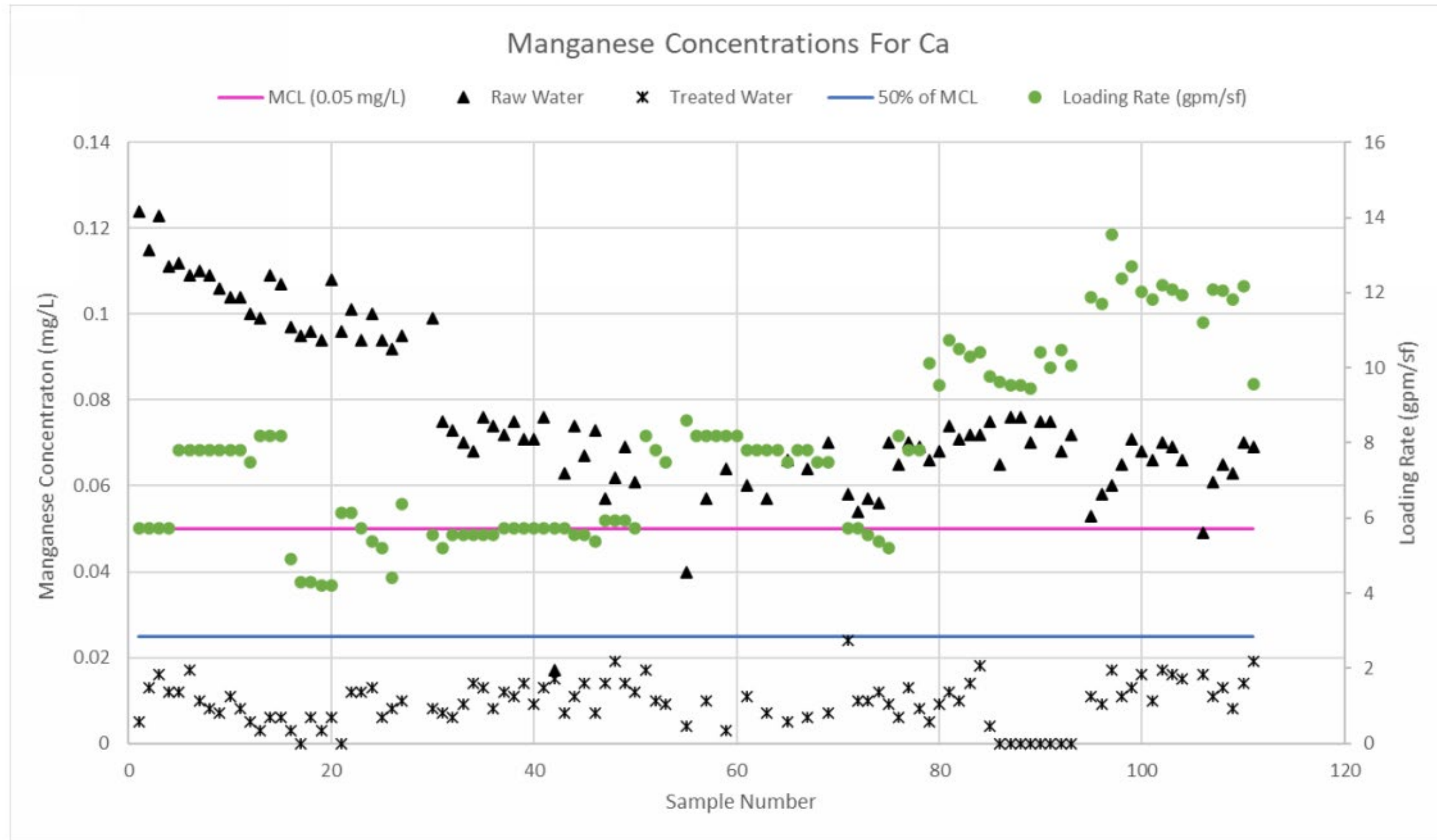
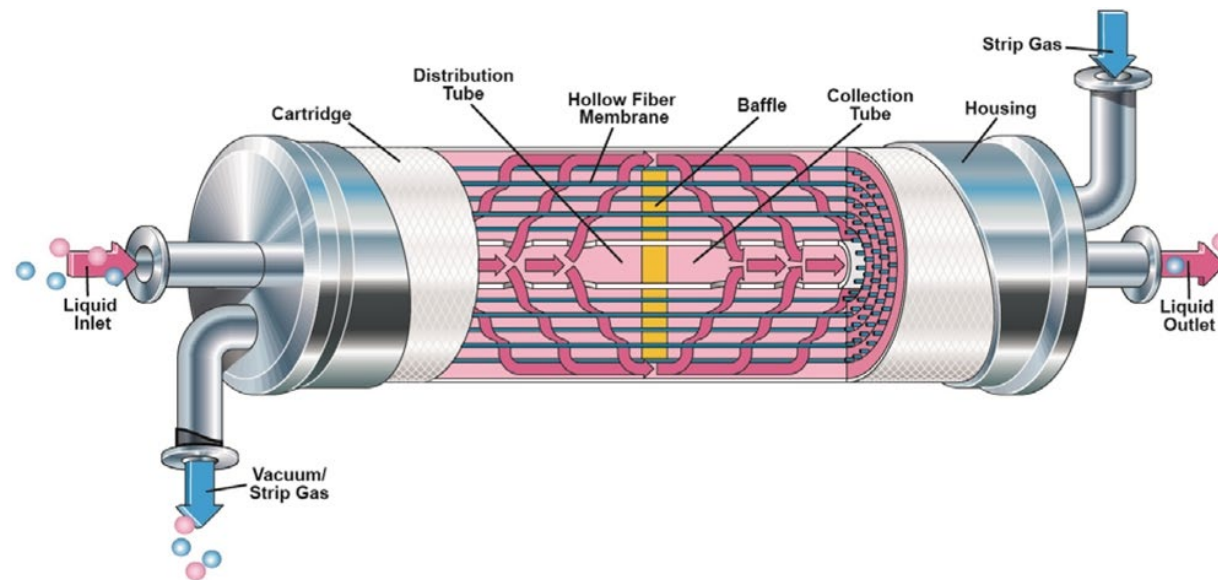


Figure 4-24. Manganese Removal vs Filter Loading Rate (with Pyrolox Advantage)

Additional Piloting

Constituent of Concerns

- Radon



Air Stripping

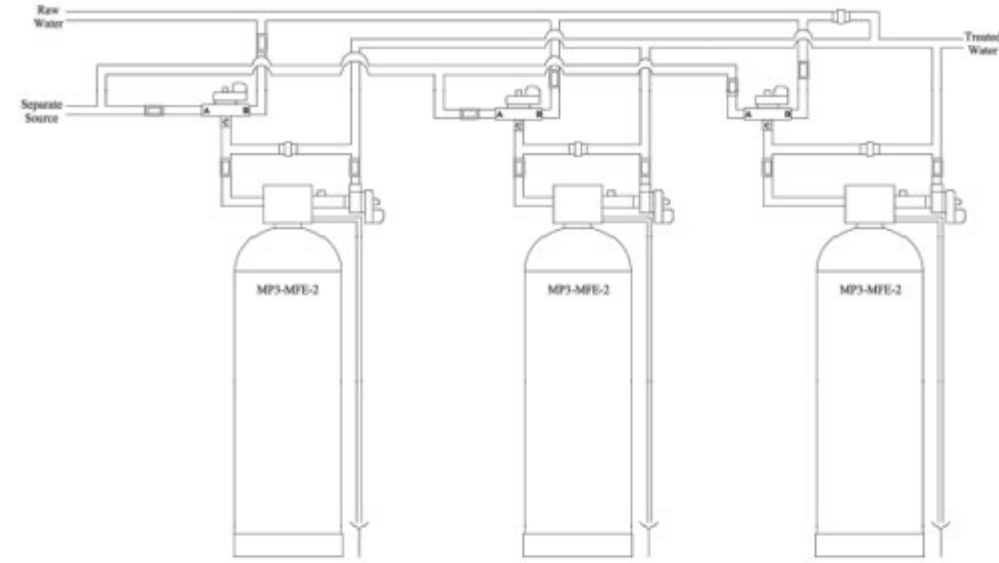


Packed Tower

Table 4-18. Radon Testing Results (4/19/2021)

Radon Testing Summary	Raw Water	Degassing Membrane	Air Stripping 50:1 Air to Water	Air Stripping 100:1 Air to Water	Air Stripping 200:1 Air to Water
Concentration, pCi/L	327	74	78	<1.0	<1.0
Percent Removal	-	77%	76%	100%	100%

Summary



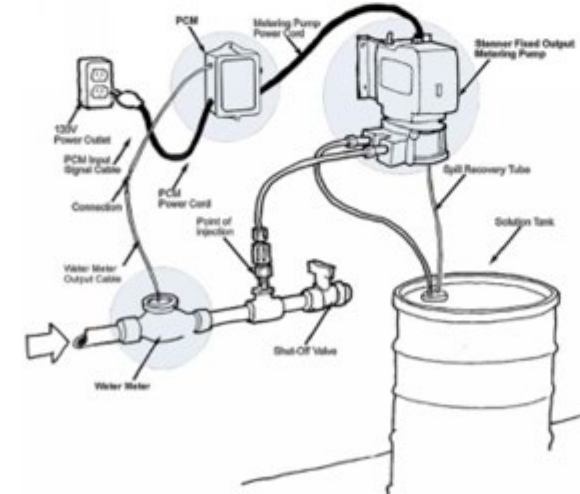
FILTER CONNECTION PIPING WITH CLEAN WATER BACKWASH (TYP)

SCALE: NTS

1

FILTER MEDIA:

1. FILTER MEDIA SHALL BE PYROLX ADVANTAGE OR APPROVED EQUAL.
2. EACH FILTER SHALL BE PROVIDED WITH GRAVEL UNDER-BEDDING TO COVER THE HUP AND LATERAL UNDERTRAIN INCLUDING AN 1/8" X 1/16" BARRIER GRAVEL BETWEEN THE GRAVEL AND FILTER MEDIA.
3. THE MEDIA LAYERS SHALL BE SUBMITTED TO THE ENGINEER FOR APPROVAL.



PUMP CONTROL MODULE

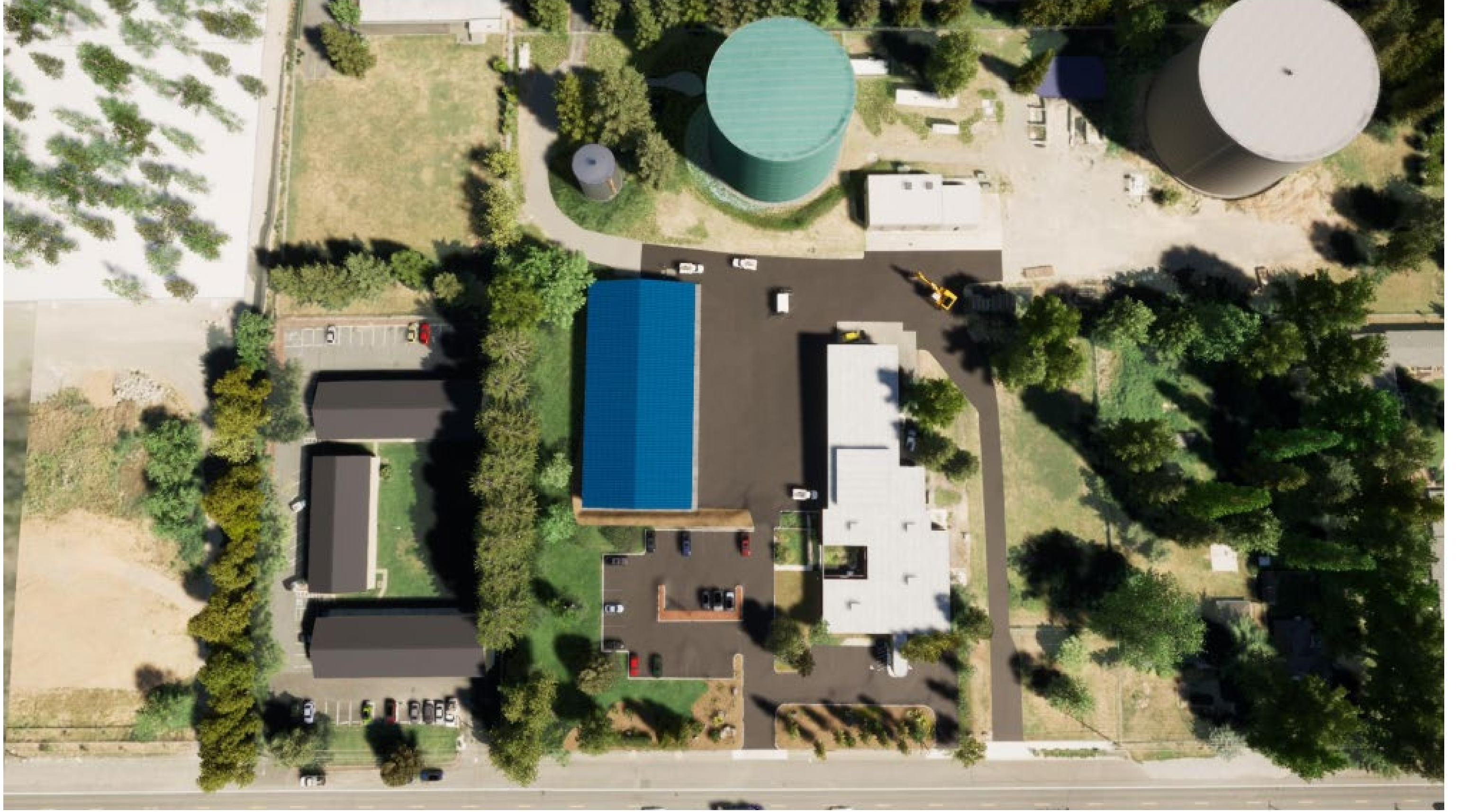
SCALE: NTS

2









Rockwood WPUD

Cascade Facility

5



Rockwood WPUD

Design Criteria: Thurston PUD

Equipment	Design Criteria
	Webster Hill Well 1
Initial Plant Capacity, gpm	100
Operating Pressure, psig	75
Run Time, hrs/day	24
Average Day Run Time, hrs/day	12
Filters	
Diameter of Vessels, ft	2
Surface areas, per vessel, sq ft	3.14
Number of Vessels for Initial Plant Capacity	4
Loading Rate, gpm/sq ft	8.0
Media Depth, in	42
Media Volume, cubic ft	11
EBCT, min	3.3
Backwash	
Backwash Loading Rage, gpm/sf	15
Backwash Flow Rate, Each Vessel	47
Approximate Backwash Frequency, hrs	14
Backwash Duration, min	5
Backwash Volume, gal/backwash (each vessel)	236
Total Backwash Volume (Buildout)	942
Backwash Frequency, #/day	1
Backwash % of Production	0.16%
Recommended Backwash Tank Volume, gal	1,413
Settling Time, min	1,416
Backwash recycle time, min/day	94
Chlorine (Sodium Hypochlorite)	
Dose, mg/L	2
Dose, lbs/day	2
Solution Strength	12.5%
Solution Feed Rate, gal/hr (each)	0.1
Solution Feed Pumps, #	2
Solution Feed Pump Capacity, gph (each)	0.19
Chemical Feed Tanks, #	1
Chemical Feed Tank Volume, gal	100
Tank Storage, days	43

Equipment	Design Criteria
	Eastridge West Well 1
Initial Plant Capacity (gpm)	20
Operating Pressure, psig	75
Run Time (hours/day)	24
Average Day Run Time (hours/day)	12
Filters (First Stage)	
Diameter of Vessels, ft	1
Surface areas, per vessel, sq ft	0.79
Number of Vessels for Initial Plant Capacity	4
Loading Rate, gpm/sq ft	6.0
Media Depth, in	42
Media Volume, Cubic ft	3
EBCT, min	4.1
Filters (Second Stage)	
Diameter of Vessels, ft	1
Surface areas, per vessel, sq ft	0.79
Number of Vessels for Initial Plant Capacity	4
Loading Rate, gpm/sq ft	6.0
Media Depth, in	42
Media Volume, Cubic ft	3
EBCT, min	4.1
Backwash	
Backwash Loading Rage, gpm/sf	15
Backwash Flow Rate, Each Vessel	
Backwash Frequency, Hrs	14
Backwash Duration (min)	5
Backwash Volume, Gal/Backsash (each vessel)	59
Total Backwash Volume (Buildout)	472
Number of Backwashes Per Day	1
Backwash % of Production	0.16%
Recommended Backwash Tank Volume, Gal	1,413
Settling Time (min)	1,416
Backwash recycle time, min/day	94
Chlorine (Sodium Hypochlorite)	
Dose, mg/L	12
Dose (lbs/day)	3
Solution Strength	12.5%
Solution Feed Rate (gal/hr) each	0.12
Solution Feed Pumps	2
Solution Feed Pump Capacity (gph) each	0.23
Chemical Feed Tanks	1
Chemical Feed Tank Volume (gal)	100
Tank Storage (days)	36

Equipment	Design Criteria
	Armstrong Well 1
Initial Plant Capacity (gpm)	30
Operating Pressure, psig	75
Run Time (hours/day)	24
Average Day Run Time (hours/day)	12
Filters (First Stage)	
Diameter of Vessels, ft	1.5
Surface areas, per vessel, sq ft	1.77
Number of Vessels for Initial Plant Capacity	3
Loading Rate, gpm/sq ft	5.7
Media Depth, in	42
Media Volume, Cubic ft	6
EBCT, min	4.6
Filters (Second Stage)	
Diameter of Vessels, ft	1.5
Surface areas, per vessel, sq ft	1.77
Number of Vessels for Initial Plant Capacity	3
Loading Rate, gpm/sq ft	5.7
Media Depth, in	42
Media Volume, Cubic ft	6
EBCT, min	4.6
Backwash	
Backwash Loading Rage, gpm/sf	15
Backwash Flow Rate, Each Vessel	26
Backwash Frequency, Hrs	14
Backwash Duration (min)	5
Backwash Volume, Gal/Backsash (each vessel)	132
Total Backwash Volume (Buildout)	397
Number of Backwashes Per Day	1
Backwash % of Production	0.31%
Recommended Backwash Tank Volume, Gal	1,000
Settling Time (min)	1,396
Backwash recycle time, min/day	132
Chlorine (Sodium Hypochlorite)	
Dose, mg/L	6
Dose (lbs/day)	2
Solution Strength	12.5%
Solution Feed Rate (gal/hr) each	0.09
Solution Feed Pumps	2
Solution Feed Pump Capacity (gph) each	0.17
Chemical Feed Tanks	1
Chemical Feed Tank Volume (gal)	50
Tank Storage (days)	48

Design Criteria: Cascade Facility (Initial and Buildout Capacity)

Design Criteria	Phase 1 - Initial Capacity: (20 mgd)	Total Capacity at Buildout (30 mgd)
Initial Plant Capacity (mgd)	20	30
Operating Pressure, psig	75	75
Run Time (hours/day)	24	24
Average Day Run Time (hours/day)	12	12
Filters		
Diameter of Vessels, ft	4	4
Surface areas, per vessel, sq ft	12.56	12.56
Number of Vessels for Initial Plant Capacity	100	140
Loading Rate, gpm/sq ft	11.15	12
Media Depth, in	42	42
Media Volume, Cubic ft	44	44
EBCT, min	2	2
Backwash		
Backwash Loading Rage, gpm/sf	15	15
Backwash Flow Rate, Each Vessel	188	188
Backwash Frequency, Hrs	14	14
Backwash Duration (min)	5	5
Backwash Volume, Gal/Backwash (each vessel)	942	942
Total Backwash Volume (Buildout)	95,000	132,000
Number of Backwashes Per Day	1	1
Backwash % of Production	0.01%	0.4%
Recycle Rate, gpm	500	500
Recommended Backwash Tank Volume, Gal	200,000	300,000
Settling Time (min)	1252	1776
Backwash recycle time, min/day	188	264
Chlorine (Sodium Hypochlorite)		
Dose, mg/L	3.5	3.5
Dose (lbs/day)	437	875
Solution Strength	12.5%	12.5%
Solution Feed Rate (gal/hr) each	17.47	34.94
Solution Feed Pumps	2	3
Solution Feed Pump Capacity (gph) each	34.94	69.89
Chemical Feed Tanks	1	2
Chemical Feed Tank Volume (gal)	5,800	6000
Tank Storage (days)	14	14

Thurston PUD

- Construction
- Operation

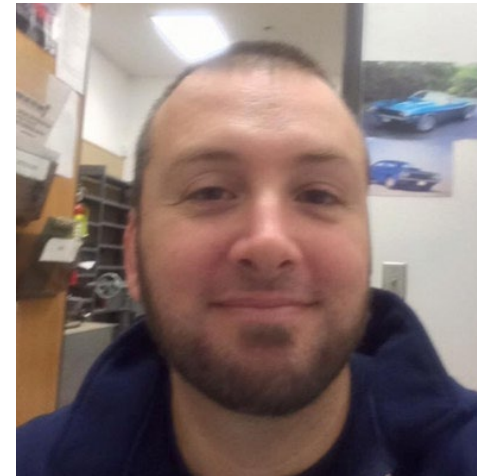
Next Steps

Rockwood WPUD

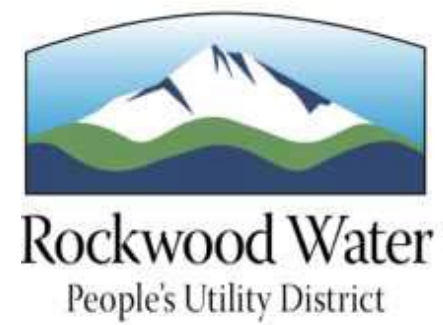
- Planning
 - Corrosion Control
 - Pilot Loop Testing
- Design
- Construction

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Thank you!





Q&A