

Presented at
PNWS AWWA Conference
Bellevue, WA
May 1, 2015

Submerged Membranes: Then, Now & What's Next

Mark Graham, P.E.



MWH[®]

BUILDING A BETTER WORLD

Acknowledgements



Advantages and Limitations of Submerged Membranes

Advantages

- Absolute barrier to pathogens
- Ease of operation
- Ability to use membrane tank for coagulation and flocculation of solids
- Small footprint
- Modular design

Limitations

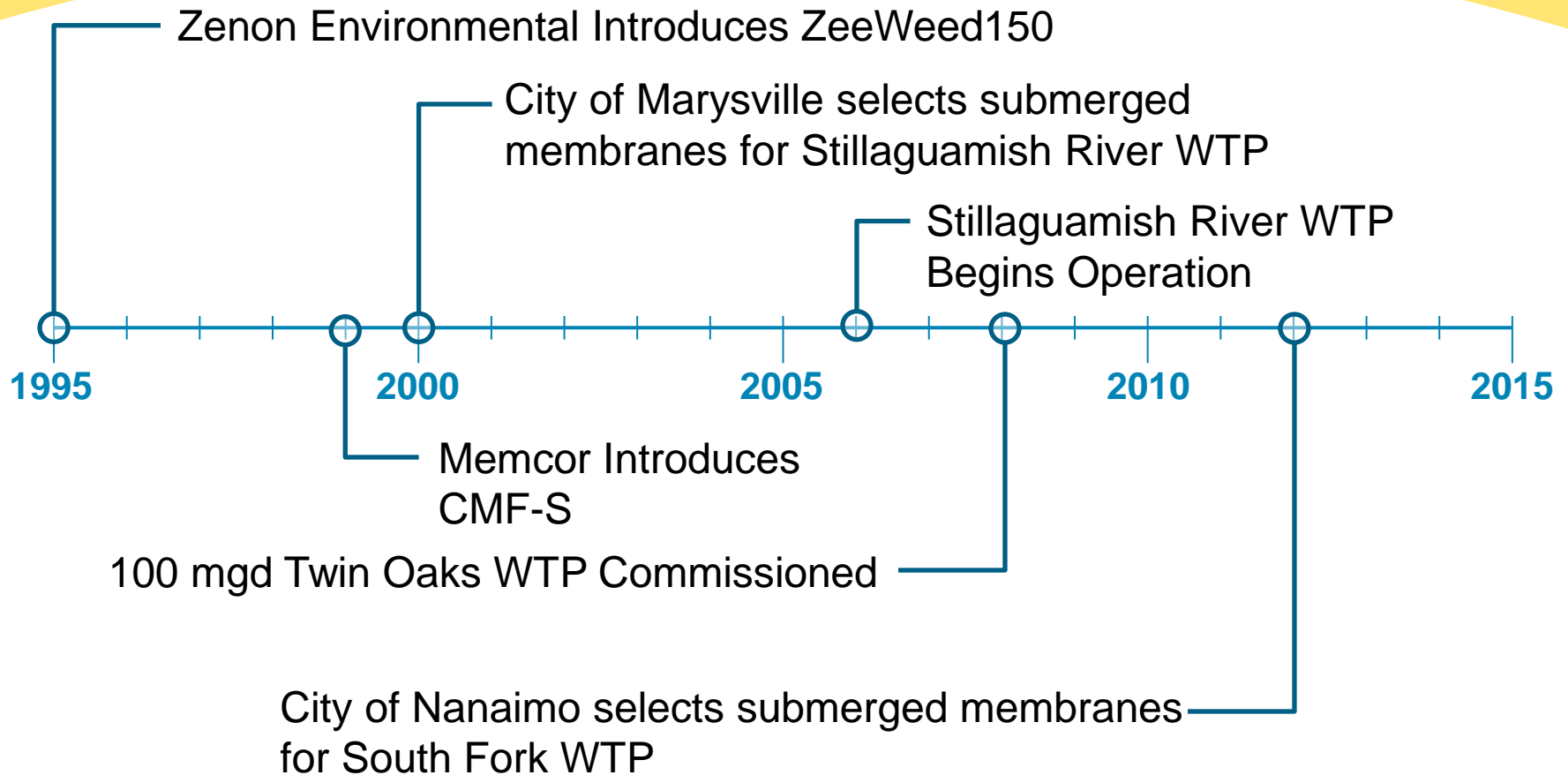
- Susceptible to physical and chemical damage
- Modular design



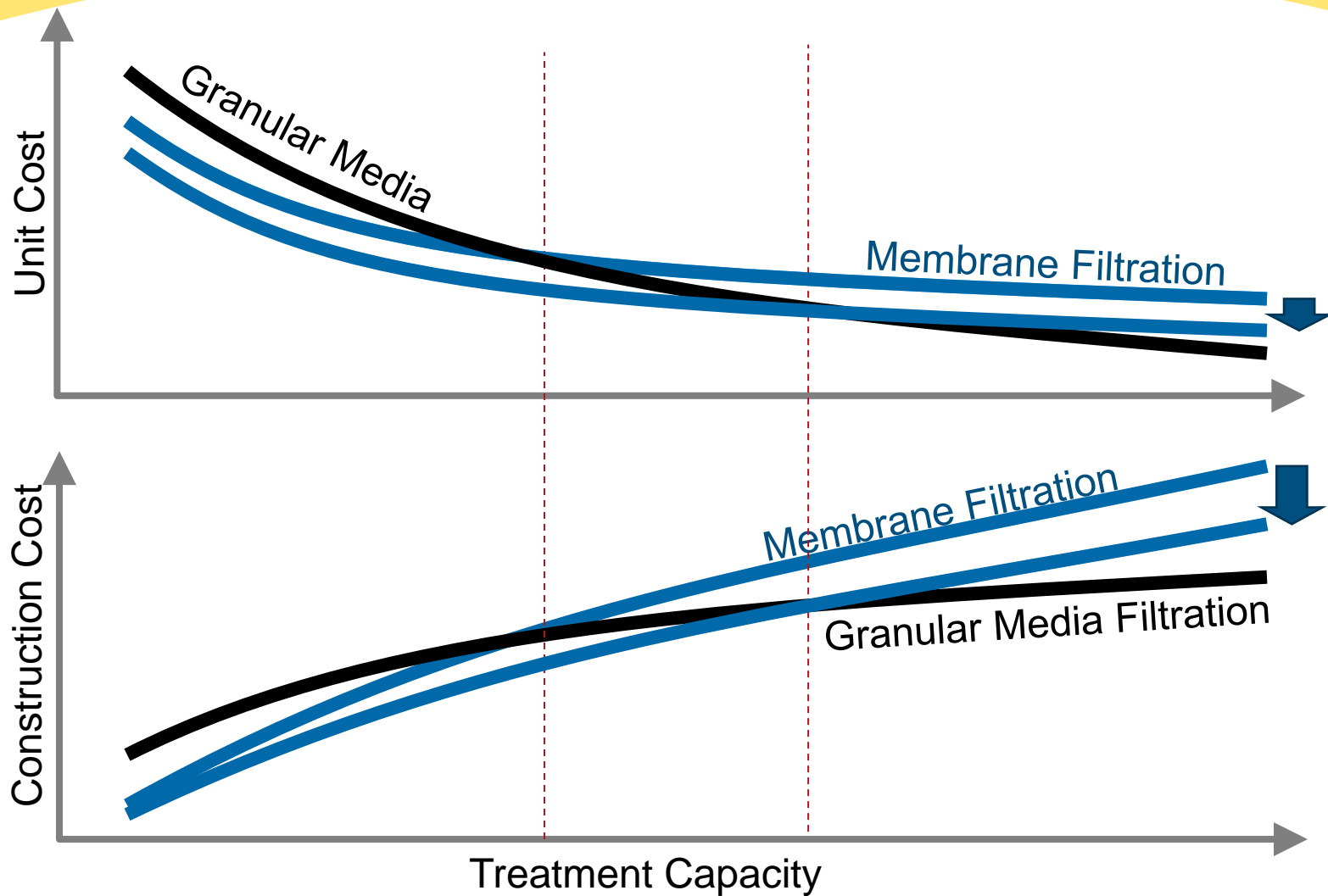
ZeeWeed 1000 Ultrafiltration Membrane



Timeline of Submerged Membranes for Drinking Water Treatment



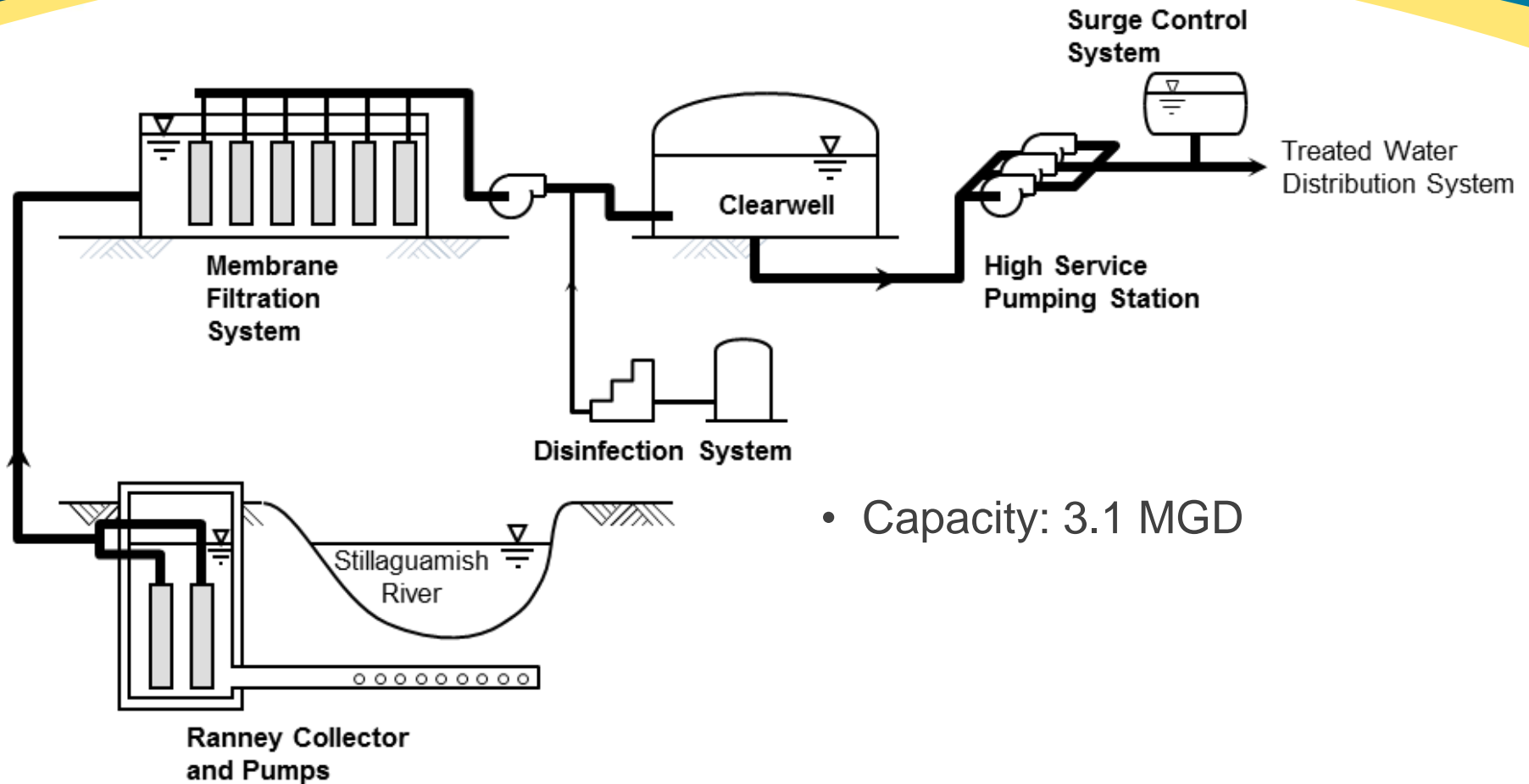
Relative Construction Cost of Membrane and Granular Media Filtration Varies with Capacity



Then



City of Marysville's Stillaguamish River WTP



- Capacity: 3.1 MGD



Stillaguamish River WTP Design Criteria

| Design Basis` | Criteria | |
|----------------------------------------------|----------------|--|
| Trains (No.) | 2 | |
| Membrane Model | ZeeWeed 500 | |
| Cassettes per Train (No.) | 6 | |
| Modules per Cassette (No.) | 26 | |
| Membrane Area per Module (ft ²) | 250 | |
| Membrane Area per Train (ft ²) | 39,000 | |
| Raw Water Flow (MGD) | 3.24 | |
| Treated Water Flow at Maximum Recovery (MGD) | 3.14 | |
| Maximum Operating TMP (psig) | -12 | |
| Design Flux (gal/ft ² /day) | >37.7 | |
| Wastewater Discharge | Sanitary Sewer | |

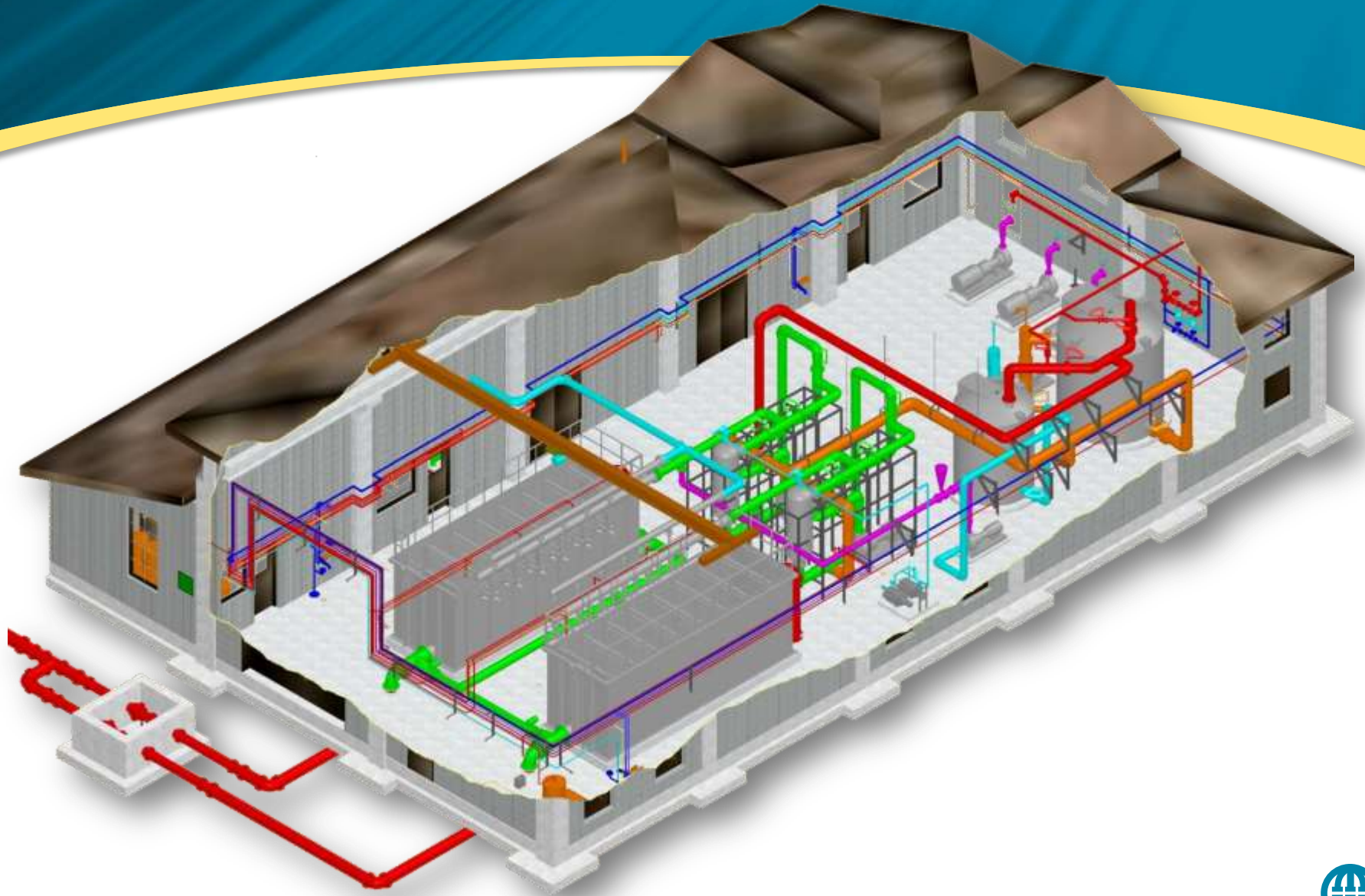


South Fork WTP Design Criteria

| Design Basis` | Primary Membrane | Secondary Membrane |
|-----------------------------------------------|--------------------|-----------------------|
| Trains (No.) | 8 | 4 |
| Membrane Model | ZW1000 | ZW500 |
| Cassettes per Train (No.) | 5 | 1 |
| Modules per Cassette (No.) | 84 | 56 |
| Membrane Area per Module (ft ²) | 450 | 420 |
| Membrane Area per Train (ft ²) | 189,000 | |
| Raw Water Flow (MGD) | 30.9 | 0.4 - 1.5 |
| Treated Water Flow at Maximum Recovery (MGD) | 30.9 | 0.4 |
| Maximum Operating TMP (psig) | | |
| Design Flux (gal/ft ² /day) @ 20°C | 26.2 | 18.3 |
| Wastewater Discharge | Secondary Membrane | Mechanical Dewatering |



Process Room at Stillaguamish River WTP



Seven Years of Operation at the Stillaguamish River Water Treatment Plant

- Plant continues to operate as designed
- No process disruptions
- No fiber breaks
- Near complete flux recovery after cleaning.



Ribbon Cutting



Current Operators



Now



Current Submerged Membrane Market for Drinking Water Treatment



MEMCOR® CS Submerged Membrane System



ZeeWeed® 500 and 1000 Modules



City of Nanaimo

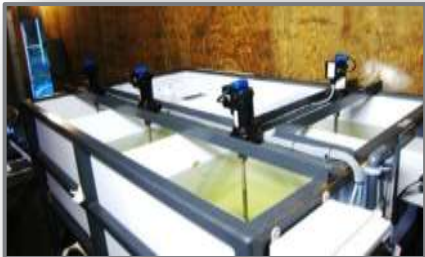
South Fork WTP



Submerged membranes were the highest-rated and lowest-cost option for the South Fork WTP



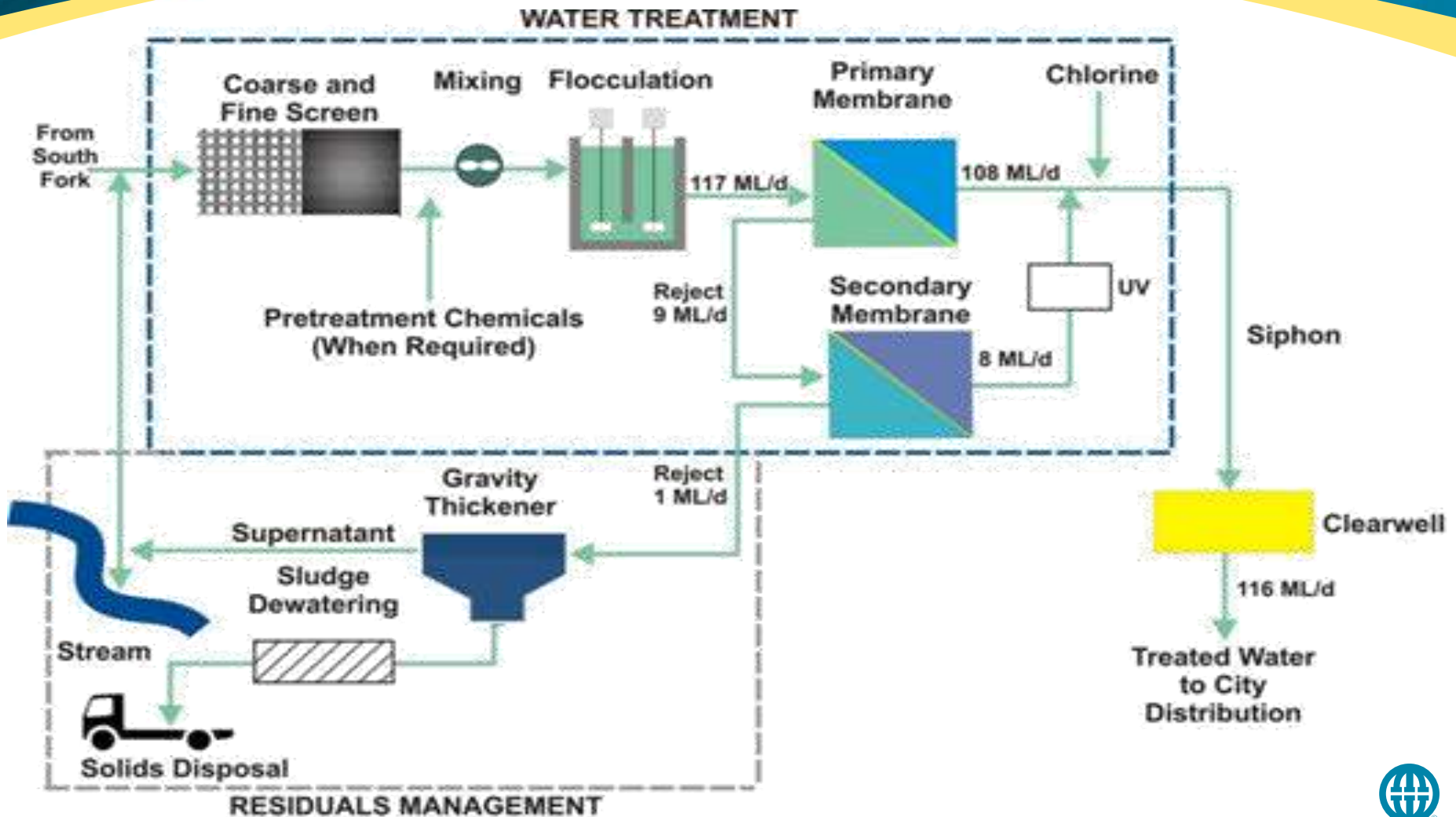
| Treatment Option | Capital Cost (\$ million) | Life Cycle Cost (\$ million) |
|---------------------|---------------------------|------------------------------|
| Direct Filtration | 58 | 94 |
| DAF/Filtration | 61 | 102 |
| Submerged Membranes | 58 | 87 |



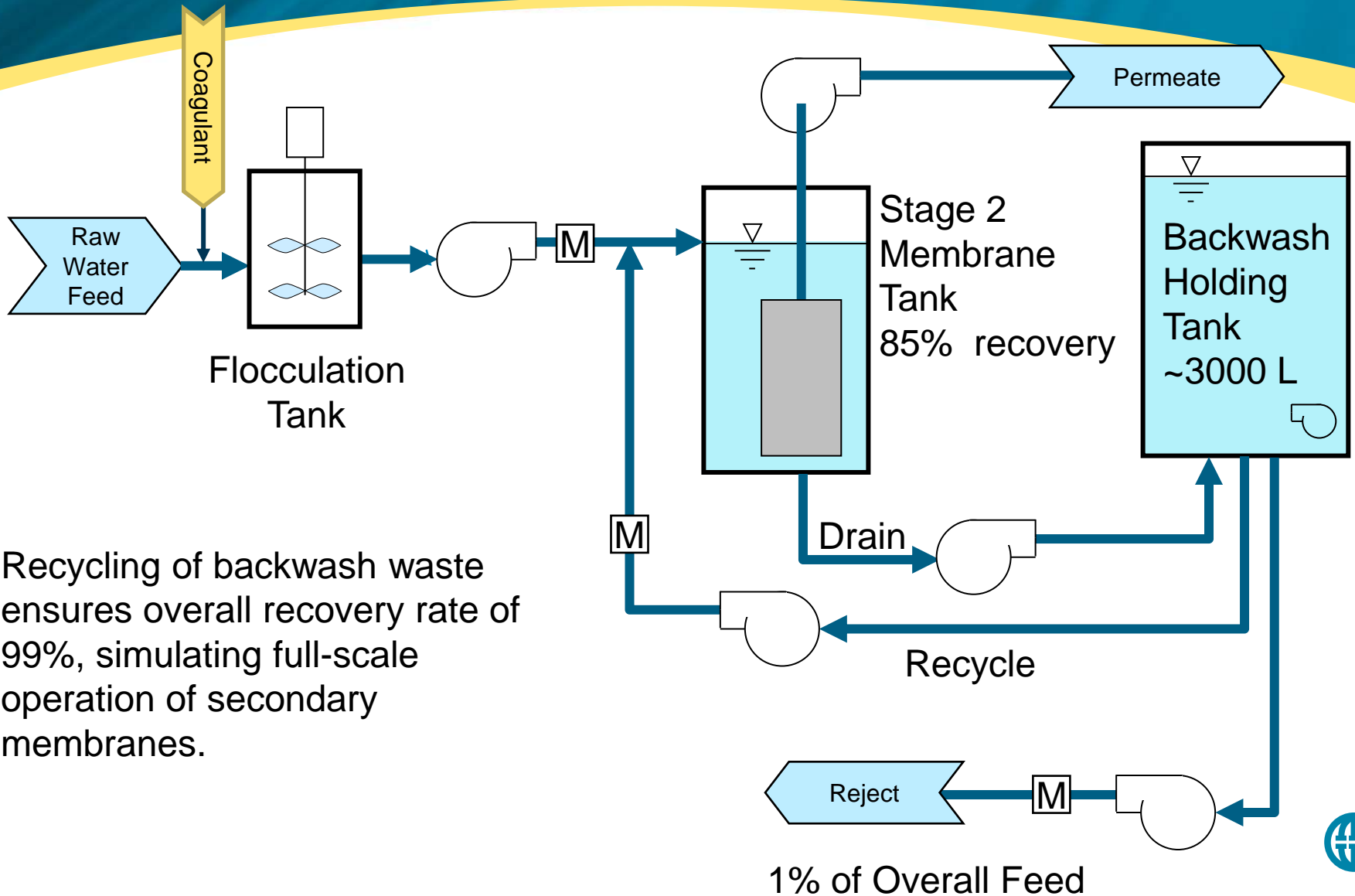
- All options successfully pilot tested
- Submerged membranes preferred
 - Ease of operation
 - Lower chemical use
 - Minimal residuals



South Fork WTP Process



Demonstration Testing 2nd Stage Process Flow Diagram



Recycling of backwash waste ensures overall recovery rate of 99%, simulating full-scale operation of secondary membranes.



Stage 1 Membrane System Design

| Parameter | Value | Comments |
|-------------------------------|-------------------------------------|------------------------------------------------------------------------|
| Stage 1 Permeate Flow | 111.3 MLD | |
| Number of Stage 1 Trains | 8 | Initially membranes for 7 |
| Stage 1 Recovery | 97% | |
| Stage 1 Design Flux | 44 l/mh @ 20degC 29 l/mh @ 3degC | 28 gfd; Two trains out of service 18 gfd; Two trains out of service |
| Permeate Driving Force | Siphon | |
| Installed membranes per train | 5 cassettes with 84 modules each | ZW1000 V4. Spare spaces for 12 more modules. |
| Backwash period | 49 to 77 minutes | |
| Maintenance Clean Period | 2 to 14 days | Hypochlorite cleans and HCl cleans |
| Recovery Clean Period | 30 to 60 days | Hypochlorite cleans and Citric/HCl cleans |

Stage 2 Membrane System Design

| Parameter | Value | Comments |
|-------------------------------|-------------------------------------|----------------------------------------------------------------------|
| Stage 2 Permeate Flow | 4.78 MLD | |
| Number of Stage 2 Trains | 4 | Initially membranes for 4. |
| Stage 2 Recovery | 85% | |
| Stage 2 Design Flux | 31 l/mh @ 20degC 20 l/mh @ 3degC | 19 gfd; One train out of service 13 gfd; One train out of service |
| TMP Range | 17 to 76 kPa | |
| Permeate Driving Force | Siphon | Primary reject pumped |
| Installed membranes per train | 1 cassettes with 54 modules each | Spare spaces for 8 additional modules if needed |
| Backwash period | 52 to 118 minutes | |
| Maintenance Clean Period | 2 to 7 days | Hypochlorite cleans |
| Recovery Clean Period | 30 to 60 days | Hypochlorite cleans and Citric/HCl cleans |

SFWTP Cutaway View



SFWTP Construction Photos



What's Next?



Future Membrane Technology and Applications

- Continued refinement of existing submerged membrane designs
- Replacement of original membrane cartridges
- New membrane materials
 - Ceramic
 - Carbon nanotubes
- Biological treatment of drinking water



Biological Treatment of Drinking Water with Submerged Membranes

- Granular media provides a substrate for growth of microbes
 - Potential issues with binding and sloughing
 - Substrate-enhanced biofiltration shows promise for removal of a range of pharmaceuticals and pesticides
- Submerged membranes commonly used for MBRs, but maintenance of a mixed liquor is not appropriate for drinking water treatment.
- New technologies fix microbes onto a biocatalyst, configured specifically for the contaminants of concern.



Questions?



Presented at
PNWS AWWA Conference
Bellevue, WA
May 1, 2015

Submerged Membranes: Then, Now & What's Next

Mark Graham, P.E.



MWH[®]

BUILDING A BETTER WORLD