



# PumpTech Customer Education

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Pump Ed 101

# Centrifugal Pump Hydraulics

Three Reasons BEP Operation is Important

Joe Evans, Ph.D

<http://www.PumpEd101.com>

# Centrifugal Pumps

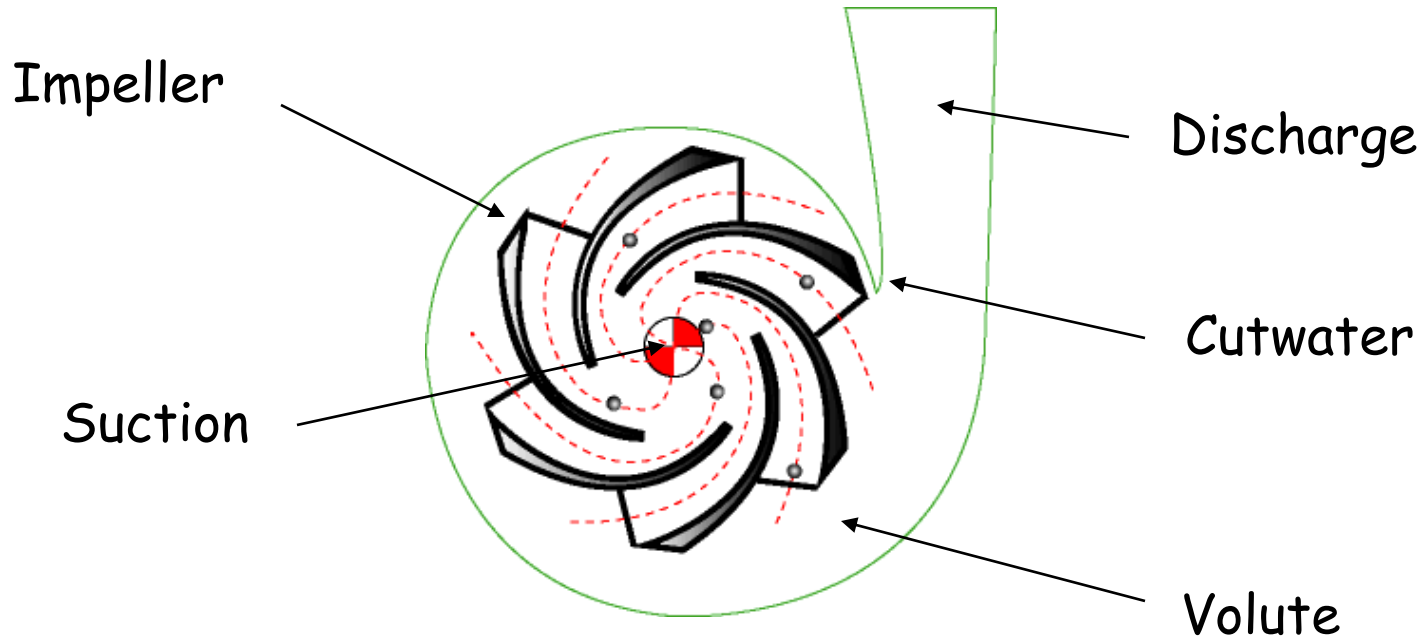


# Impellers



Hint

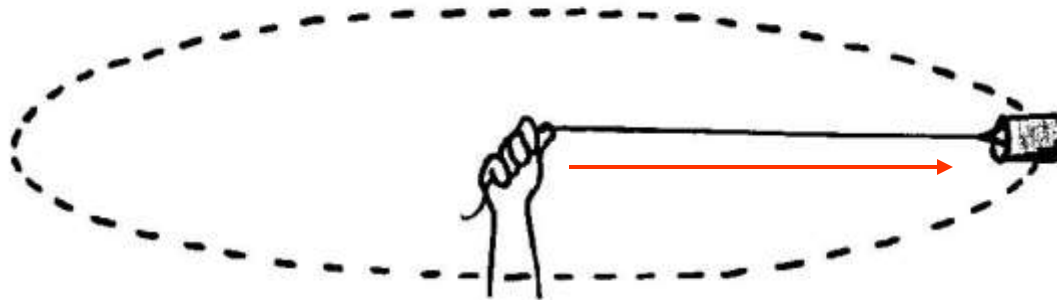
# Centrifugal Pump Dynamics



What Type of Energy is Added by the Impeller ?

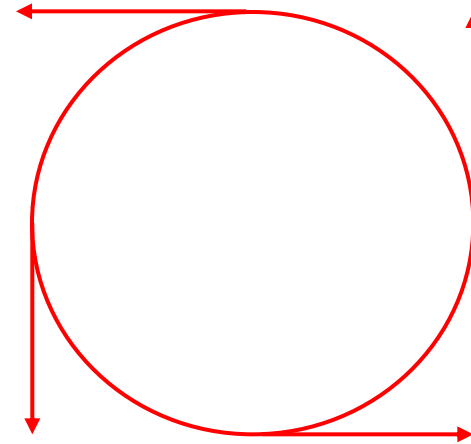
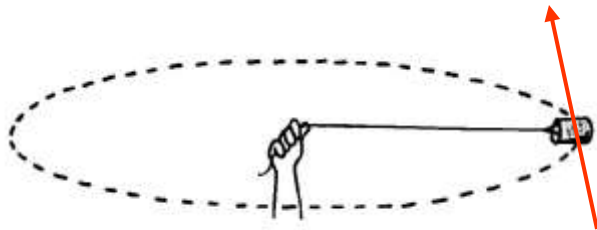
# Centrifugal Force

- It is defined as "center fleeing"



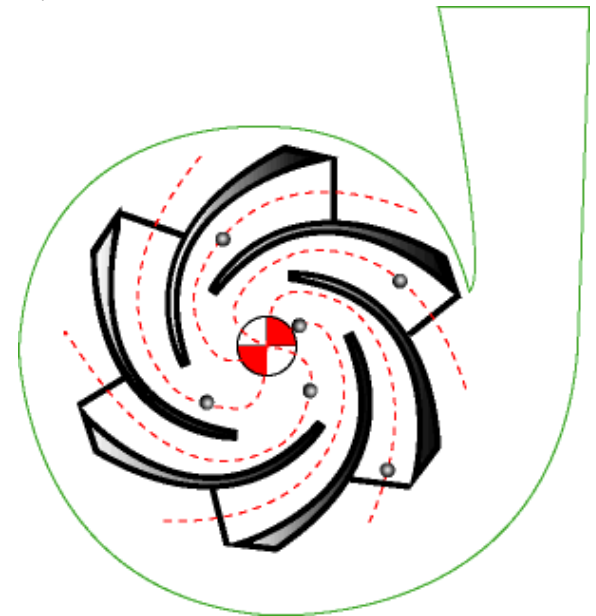
# Centrifugal Force

- Instead it actually moves in the same direction it was traveling at the exact instant it is released.
- When an object is traveling in a circle, it is actually moving in a straight line at any single point in time.



# So, How Does It Work ?

- 1 Rotation of the impeller forces water from its entry point, at the eye, into its vanes.
- 2 Water moving through the vanes creates a partial vacuum at the eye allowing atmospheric, or some other outside pressure, to force more water into the eye.
- 3 As water travels through the vanes, it gains rotational **velocity** (kinetic energy) and reaches its maximum velocity just as it exits the vanes.
- 4 Upon exiting the vanes, water enters the volute where **most** of its kinetic energy of motion is transformed into pressure energy.



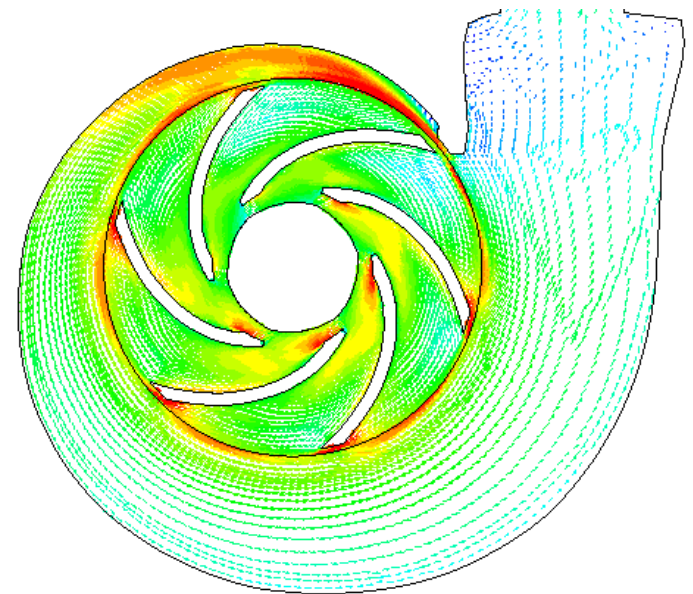


# The Volute and its Function

The volute houses the impeller and is the "receptacle" for the water exiting its vanes.

Its smooth, nearly circular, geometry guides the flow from the impeller towards its discharge. During this trip, the flow encounters an ever increasing volume.

The volute **converts** the **kinetic energy (velocity)** imparted by the impeller **into pressure**.



# The Performance Curve

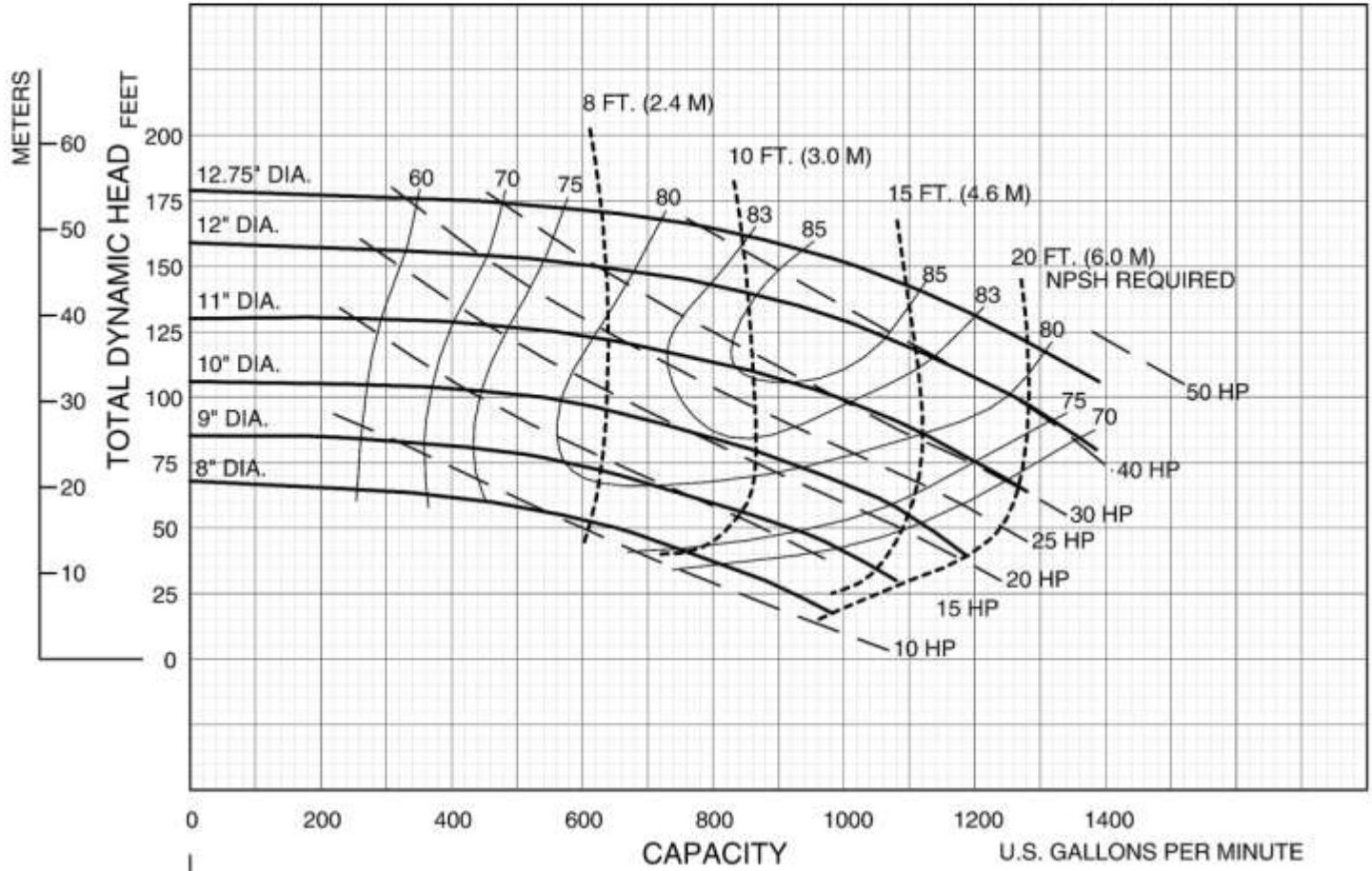
- Pump Information
- Flow and Pressure at Several Points
  - Hydraulic Efficiency
  - Horsepower
- Net Positive Suction Head Required (NPSHr)

# The Performance Curve

Feet x .305 = Meters  
 Inches x 25.4 = Millimeters  
 GPM x .227 = Cubic Meters/Hour  
 GPM x 3.785 = Liters/Minute  
 HP x .746 = KW

Speed	Impeller Dia.	Style	Solids Dia.	N <sub>S</sub>	Suction	Discharge	No. vanes
1775	VARIOUS	ENCLOSED	.84"	1332	6"	4"	7

SINGLE VOLUTE MOUNTING CONFIG.: CC, VM, F, VF, EM, VC



are for cool water, close-  
 rification with packing.  
 ies or liquids may require  
 performance adjustments.



# The Performance Curve

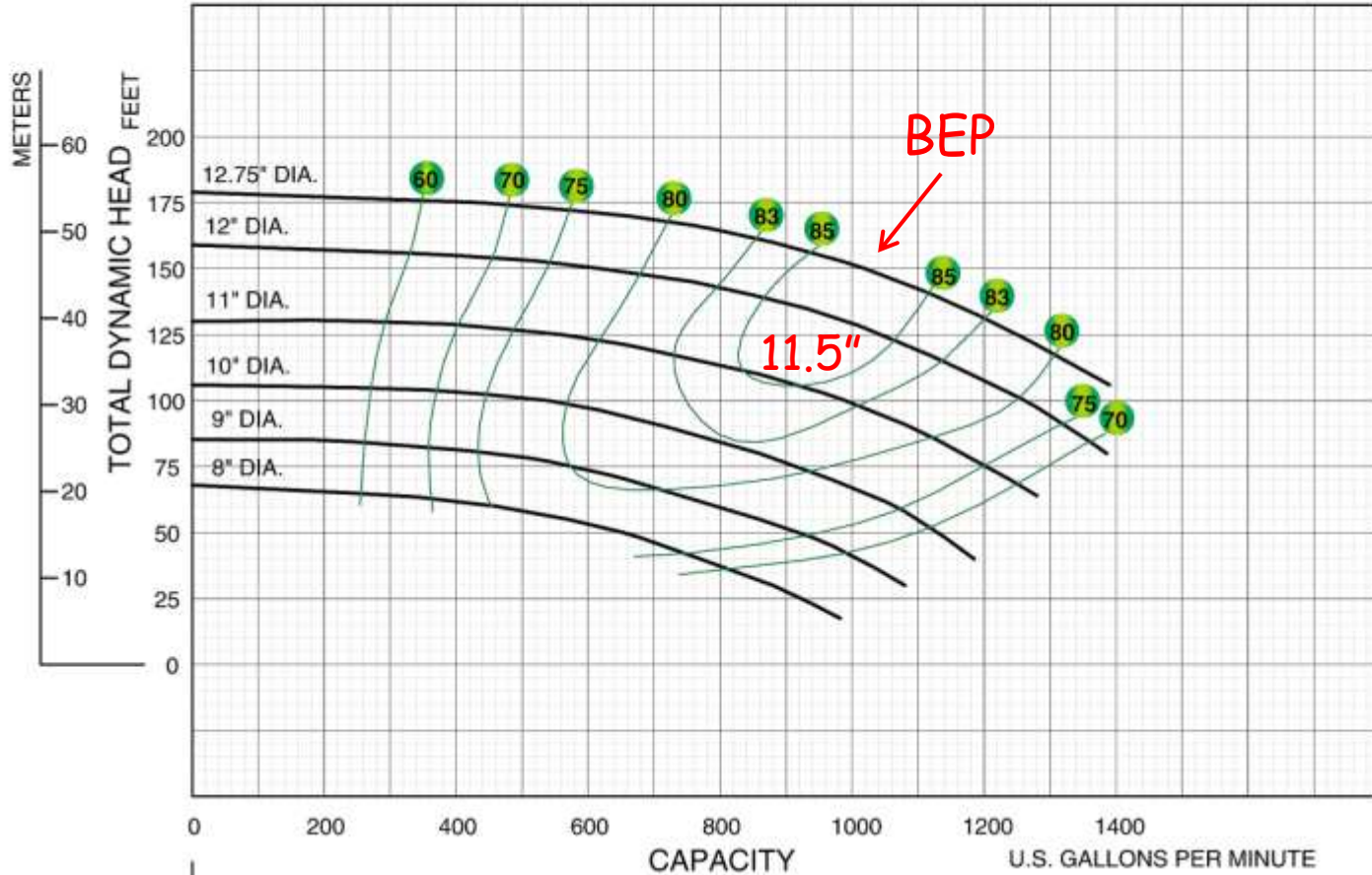
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NEW PAGE

SINGLE VOLUTE

MOUNTING CONFIG.: CC, VM, F, VF, EM, VC



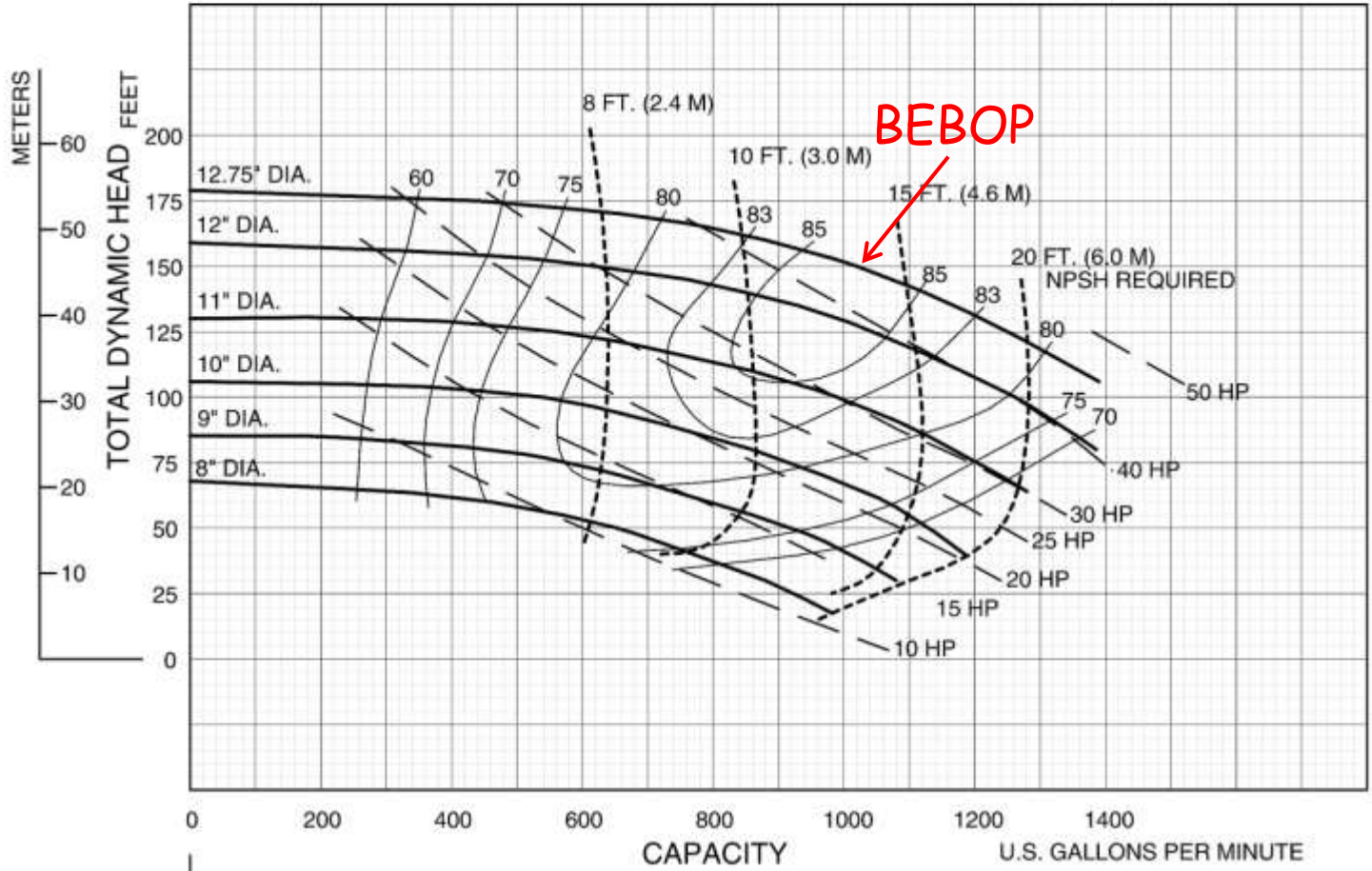
Use only for cool water, close-  
 antipollution with packing.  
 styles or liquids may require  
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# The Performance Curve

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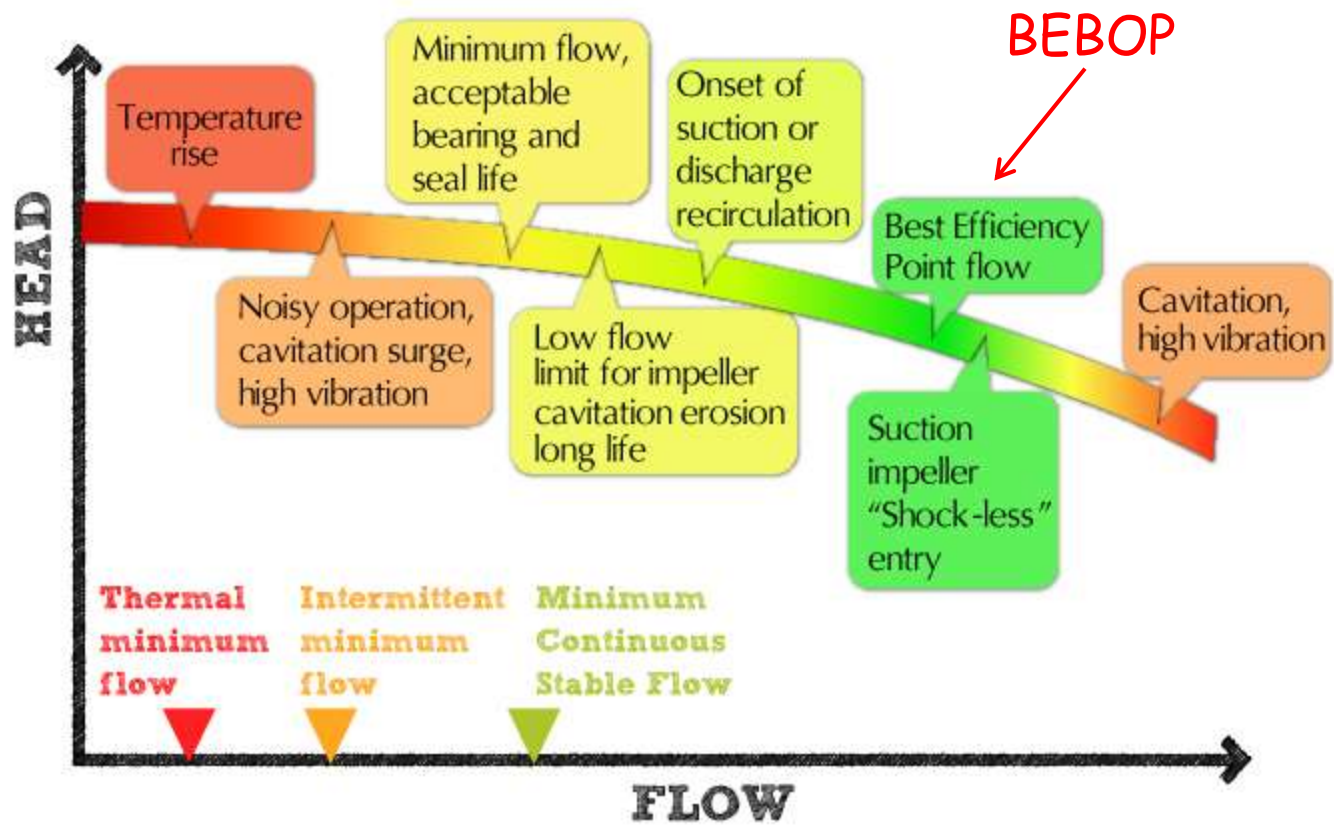
SINGLE VOLUTE MOUNTING CONFIG.: CC, VM, F, VF, EM, VC



Use only for cool water, close-  
 configuration with packing.  
 Use for liquids may require  
 performance adjustments.



# The Performance Curve

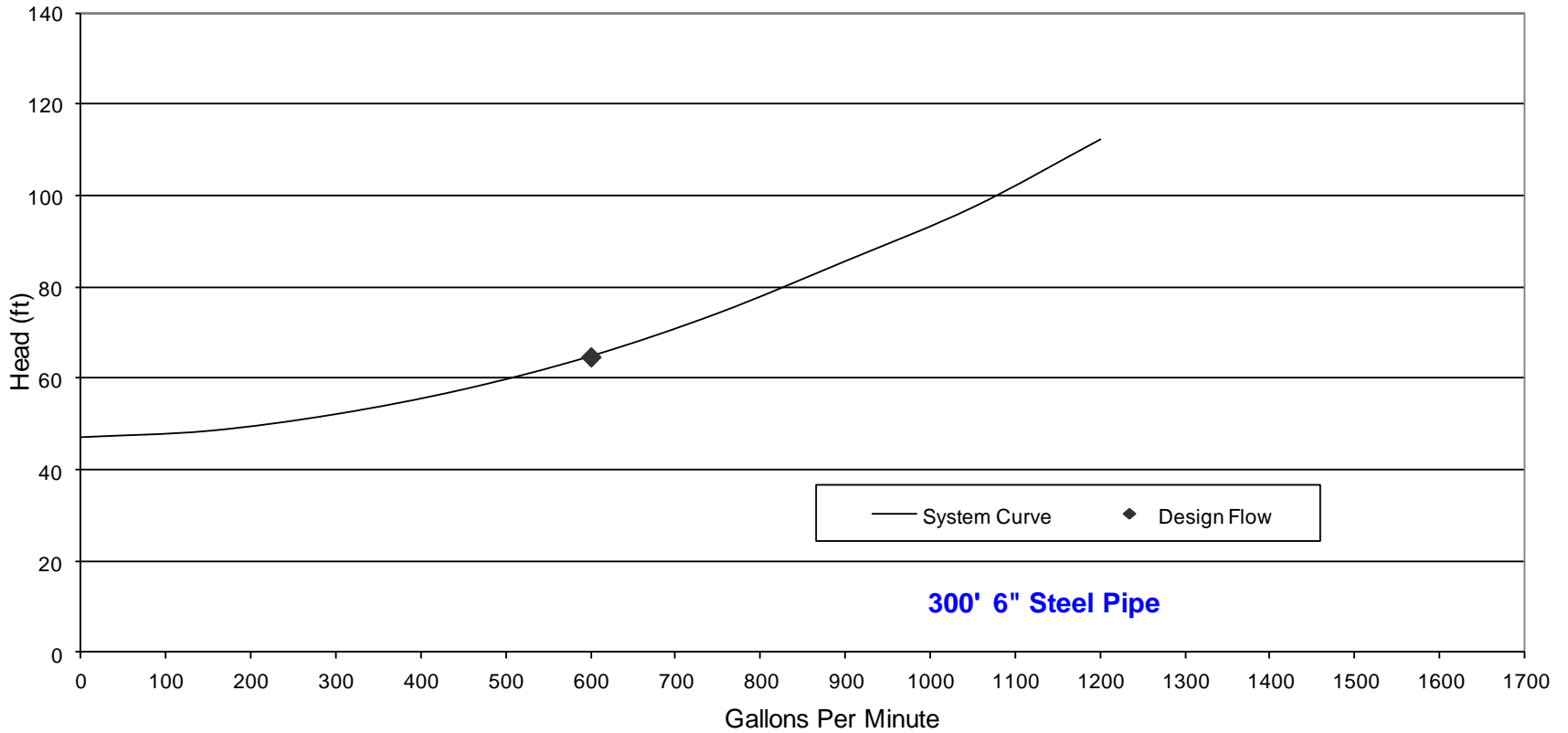


# BEBOP & The Cost of Pump Operation

When a centrifugal pump is operated at BEBOP

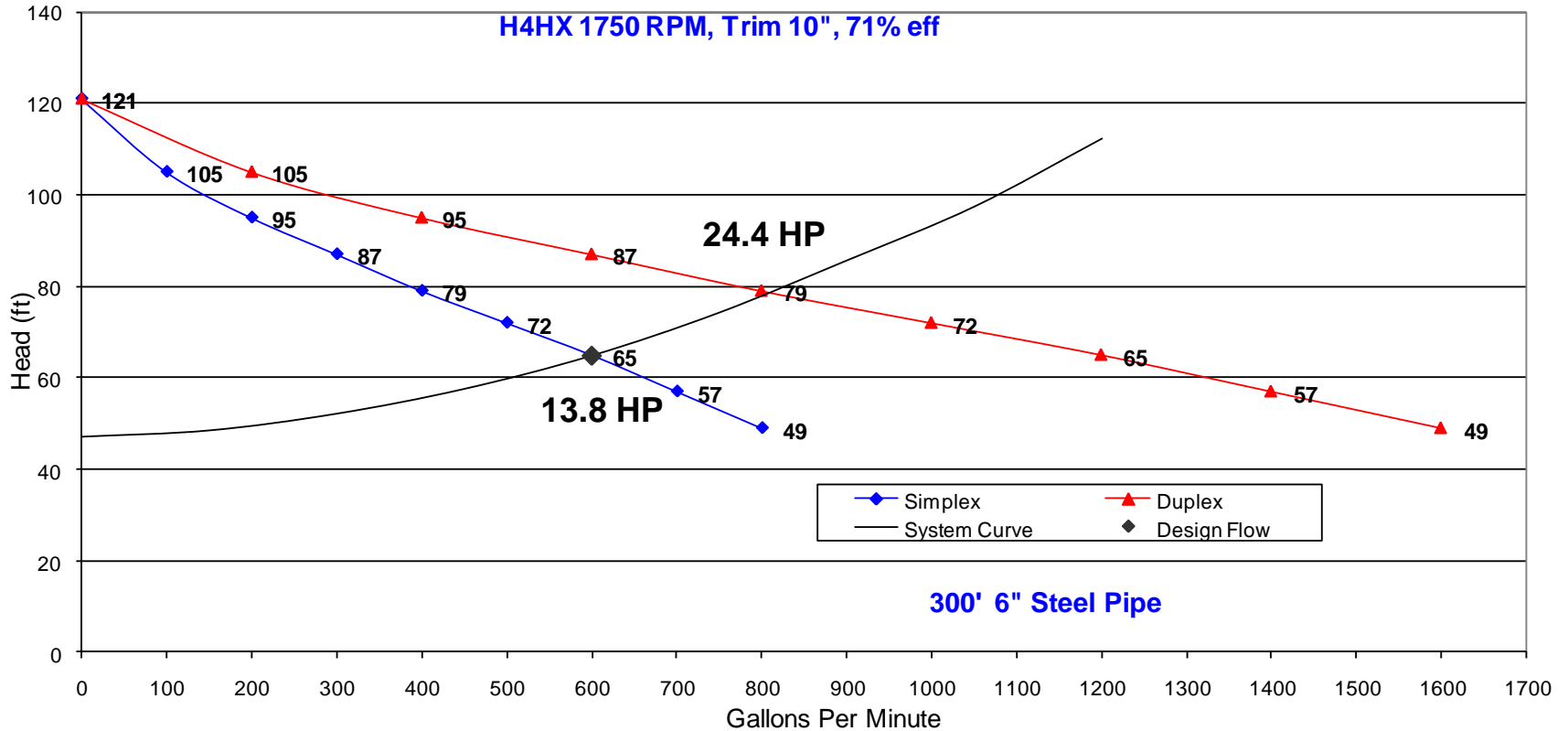
- Power consumption is at its lowest
- Maintenance costs are their lowest
  - Useful life is at its maximum

# The System Curve

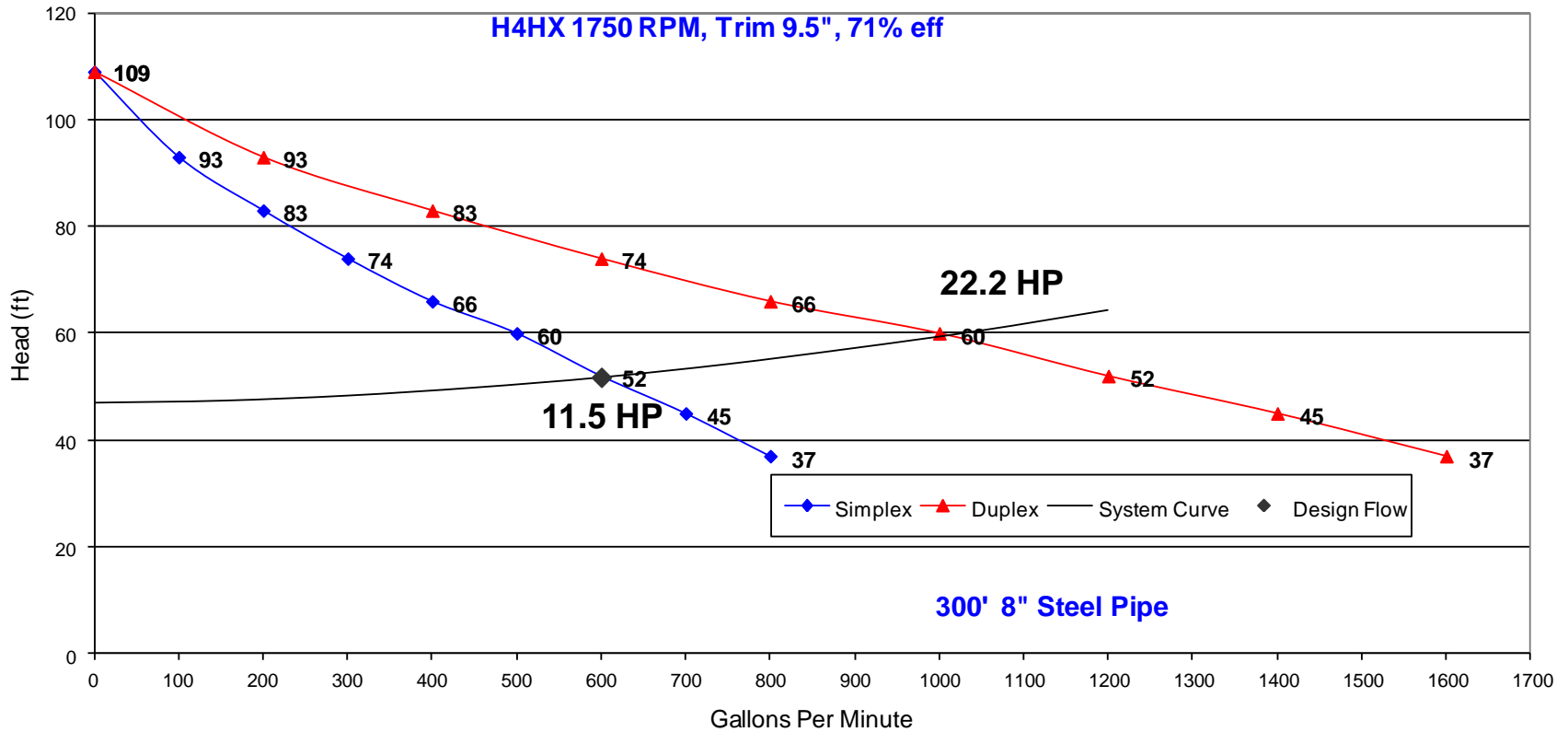




# The System Curve



# The System Curve

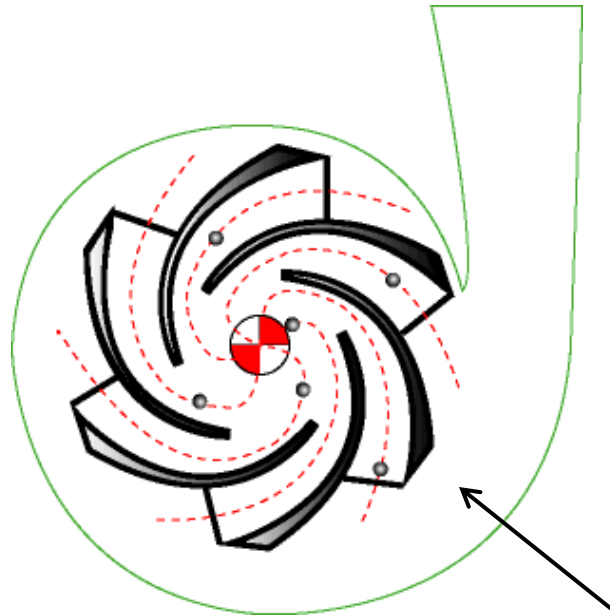


# System Hydraulics - Radial Thrust

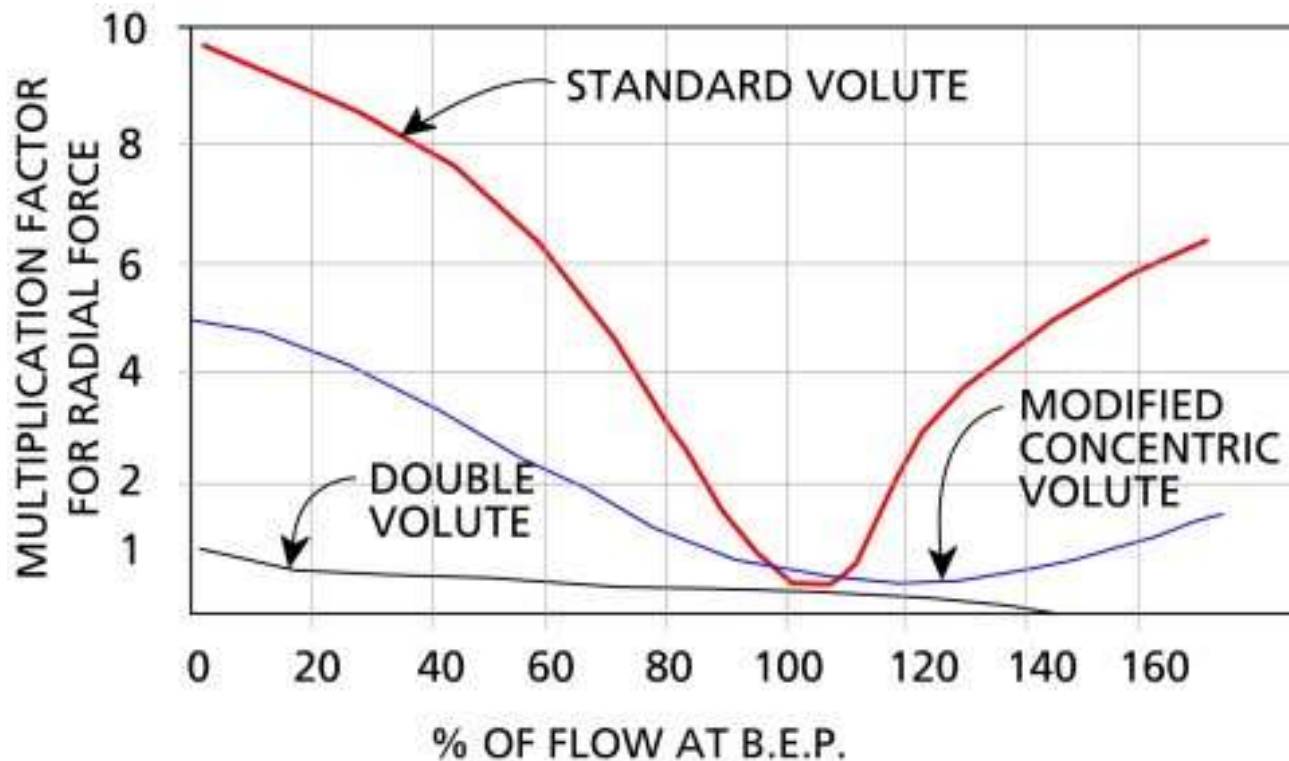
- Ideally a pump should operate between 90% and 110% of its BEBOP.
- If it does not, the radial forces that act upon a centrifugal pump's impeller can account for a large percentage of premature failures.
- The increased shaft deflection will decrease **mechanical seal, wear ring, and bearing** life.
- Worse case - **shaft breakage**

# Radial Thrust

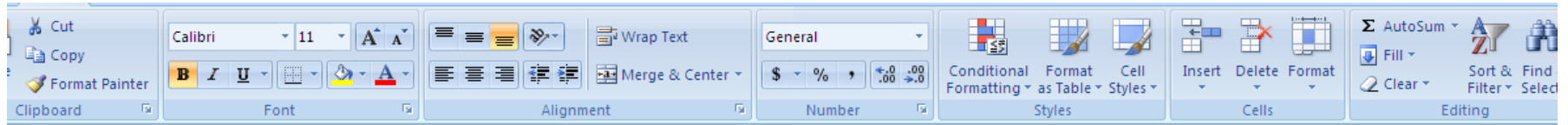
- Forms about the periphery of the impeller due to uneven volute geometry
- A function of **total head, width and diameter** of the impeller
- Usually reaches a maximum at or near shut off head



# Radial Thrust Factor



# Radial Thrust Calculator



A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q	R	S
---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---	---

Radial Thrust Calculator - Joe Evans [www.PumpEd101.com](http://www.PumpEd101.com)

Radial Thrust (PSI):  $F_R = K_R \times (H \times s / 2.31) \times D_2 \times b_2$

Enter the required data in the highlighted cells. If you do not know the pump specific speed use the Ns calculator below.

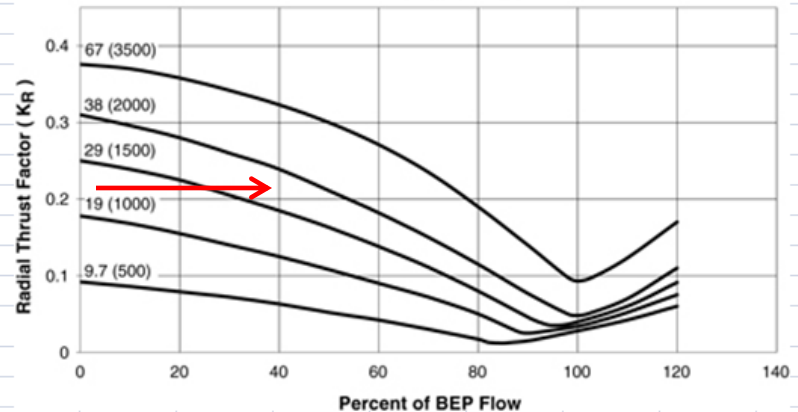
Thrust Factor (K <sub>R</sub> ) @ flow point (from graph)	0.21
Head (H) per Stage @ flow point in feet	138
Specific Gravity (S)	1
Impeller Diameter (D <sub>2</sub> ) in inches	11.88
Impeller Width (b <sub>2</sub> ) @ discharge in inches	3.5
<b>F<sub>R</sub> (Unbalanced Radial Thrust in lbf) =</b>	<b>522</b>

Pump Specific Speed:  $N_s = N \sqrt{Q} / H^{0.75}$

Enter the required data in the highlighted cells

Pump RPM (N)	1750
Flow (Q) @ BEP	1200
Head (H) @ BEP	110
<b>N<sub>s</sub> =</b>	<b>1785</b>

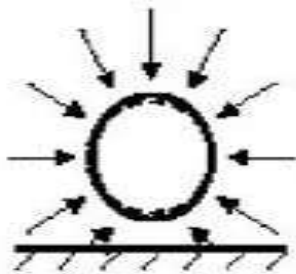
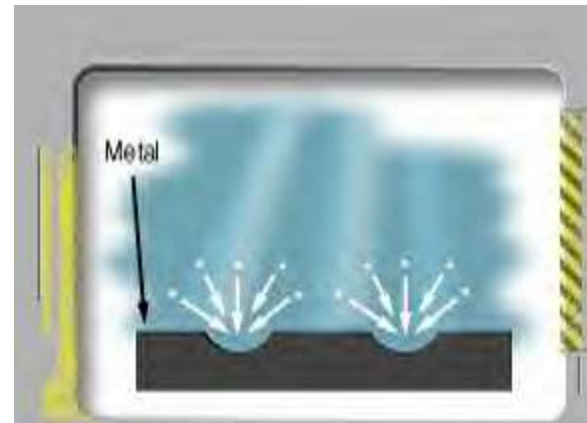
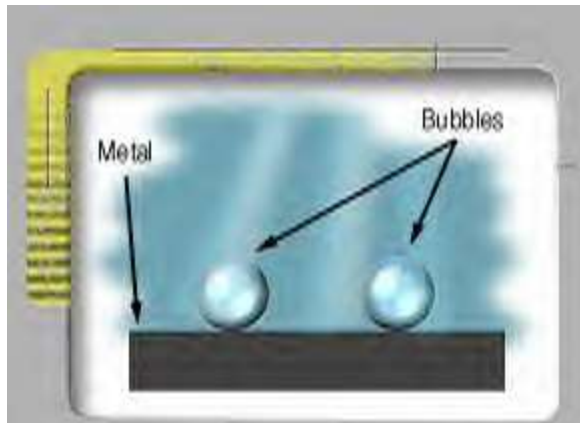
Radial Thrust Factor Single Volute



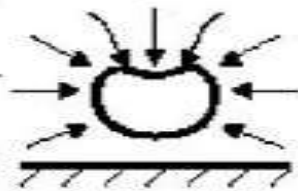
**Instructions**

The numbers in ( ) are Pump Specific Speed (Ns). The curves represent the radial thrust factor from 0 to 120% of BEP flow for that particular specific speed. Select a point on the X axis that corresponds to the point to be evaluated on the pump H/Q curve. The thrust factor is the value on the Y axis where the curve intersects the selected X axis value. For values of Ns that fall between the ones shown you may interpolate the intersection. Impeller width (b<sub>2</sub>) is the width in inches at the discharge including the shroud(s). The example shown is for a sewage pump with a specific speed of 1785, operating at 40% of BEP flow. At 100% of BEP flow, radial thrust is reduced to 59 lbs. Worst case? This pump is approved by the manufacturer for flows as low as 21% of BEP. At that flow point, radial thrust reaches 660 lbs.

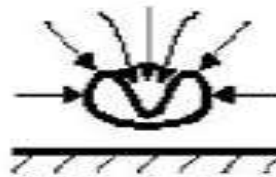
# Cavitation



*Initial bubble*



*Initiation of bubble collapse*



*Forming of liquid microjet*



*Microjet*



*Impact & metal extrusion*

# Types of Cavitation

Normal Cavitation - Low NPSHa

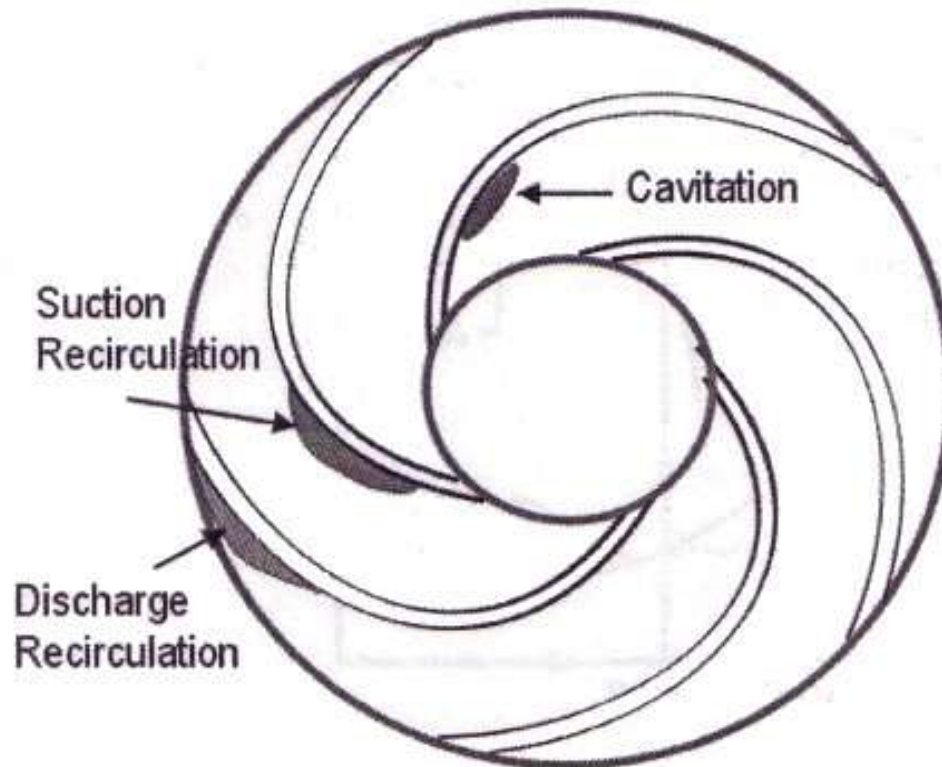
Wear Ring Recirculation - Low Flow

Discharge Recirculation - Low Flow

Suction Recirculation - Low Flow



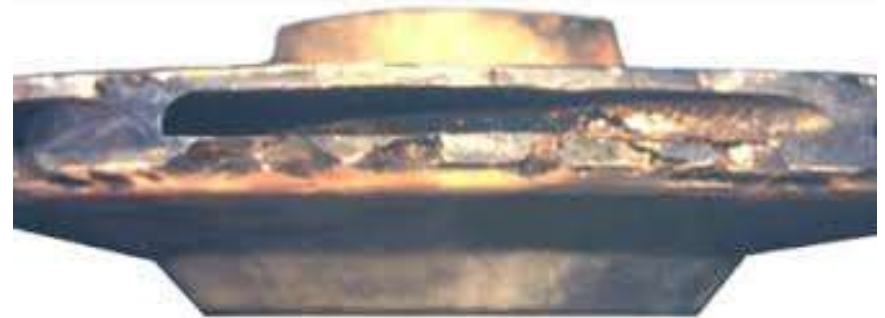
# Types of Cavitation



# Wear Ring Recirculation Cavitation



# Discharge Recirculation Cavitation



Occurs on the high pressure  
side of the vane

# Discharge Recirculation Cavitation Two Vane



# Suction Recirculation Cavitation

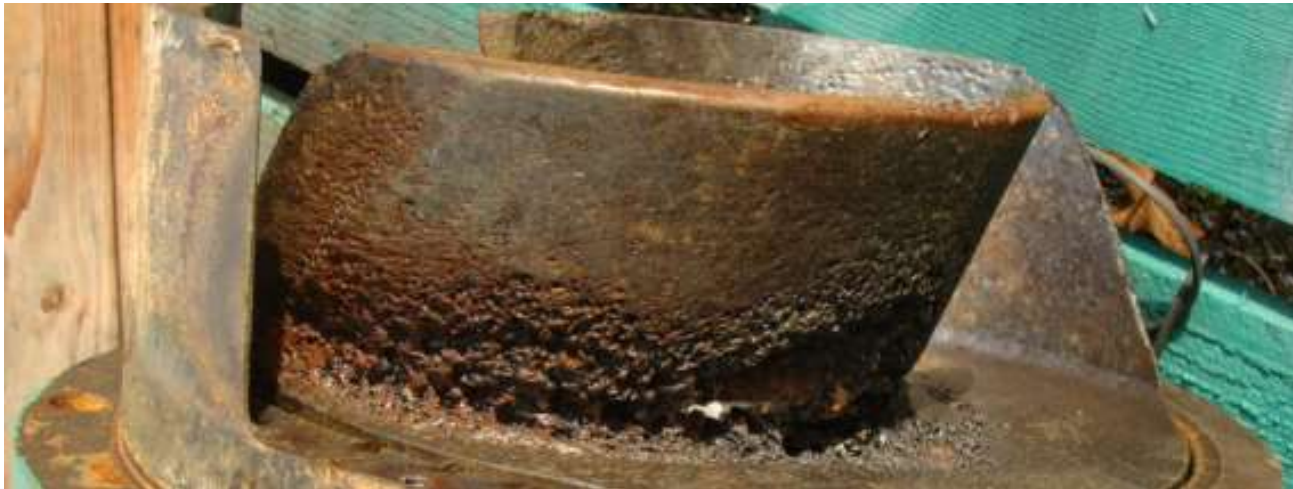


Occurs on the high pressure  
side of the vane

# Suction Recirculation Cavitation

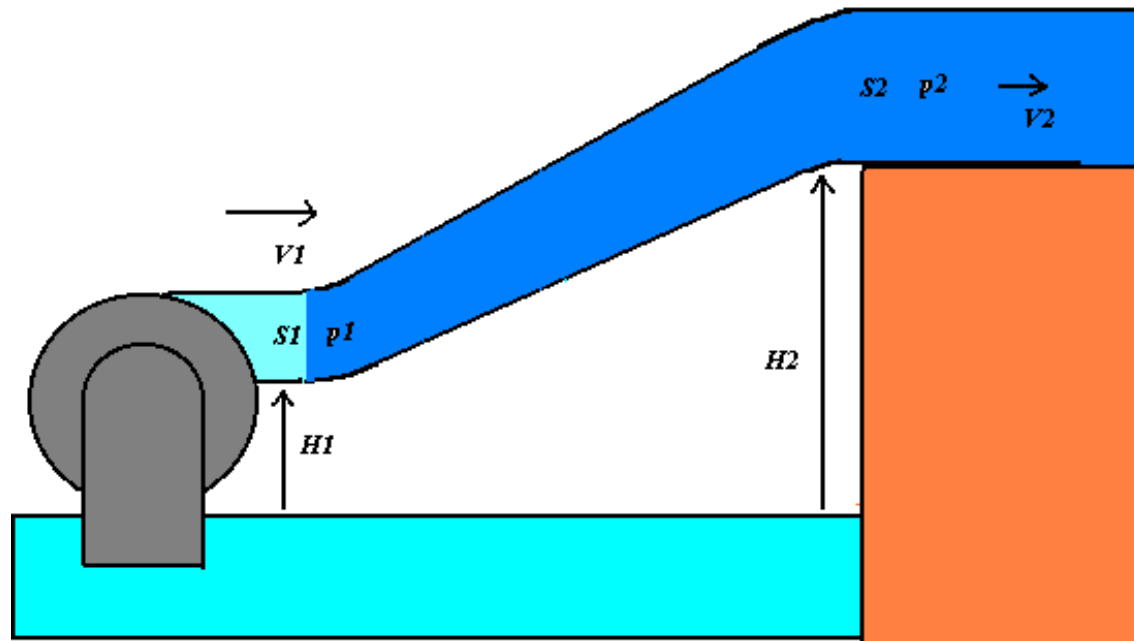


# Suction & Discharge Recirculation Cavitation



# Conservation of Energy

**Bernoulli's** theorem states that, during steady flow, the energy at any point in a conduit is the sum of the velocity head, pressure head, and elevation head. It also states that this sum will remain constant if there are no losses. Daniel Bernoulli 1700-1782





# Total Dynamic Head

Total Dynamic Head

$$H = h_d - h_s$$

Where:

$h_d$  = discharge head

$h_s$  = suction head

Total Suction Head

$$h_s = \pm h_{gs} + h_{vs} \pm Z_s$$

Where:

$h_g$  = gauge head

$h_v$  = velocity head

$Z$  = gauge distance  
above or below  
datum

Total Discharge Head

$$h_d = h_{gd} + h_{vd} \pm Z_d$$

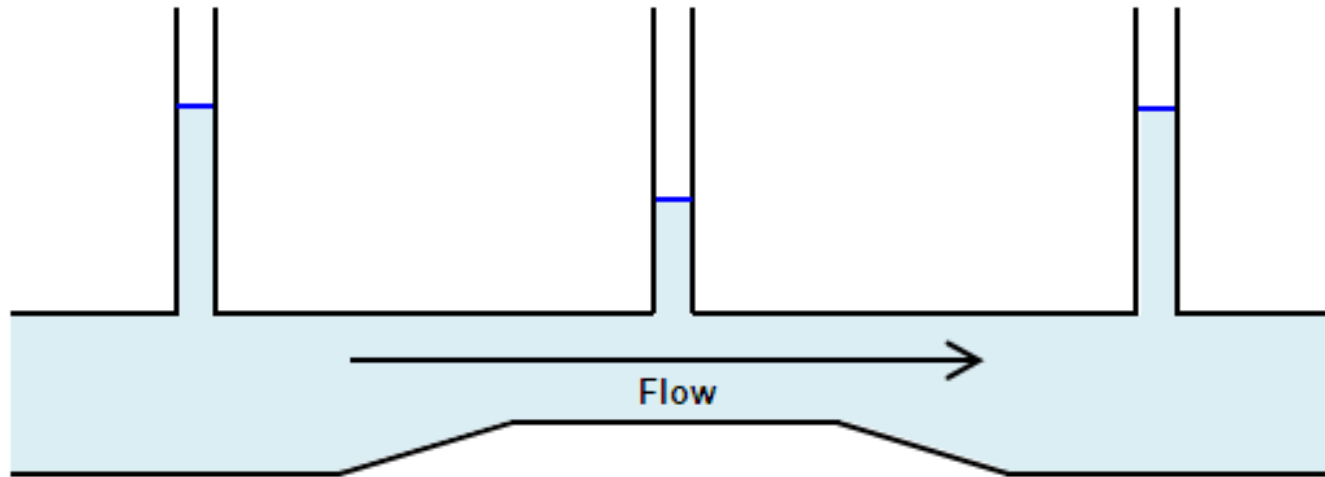
## What is Velocity Head ?

It is a form of energy that cannot be measured with a pressure gauge.

## Why is It Important ?

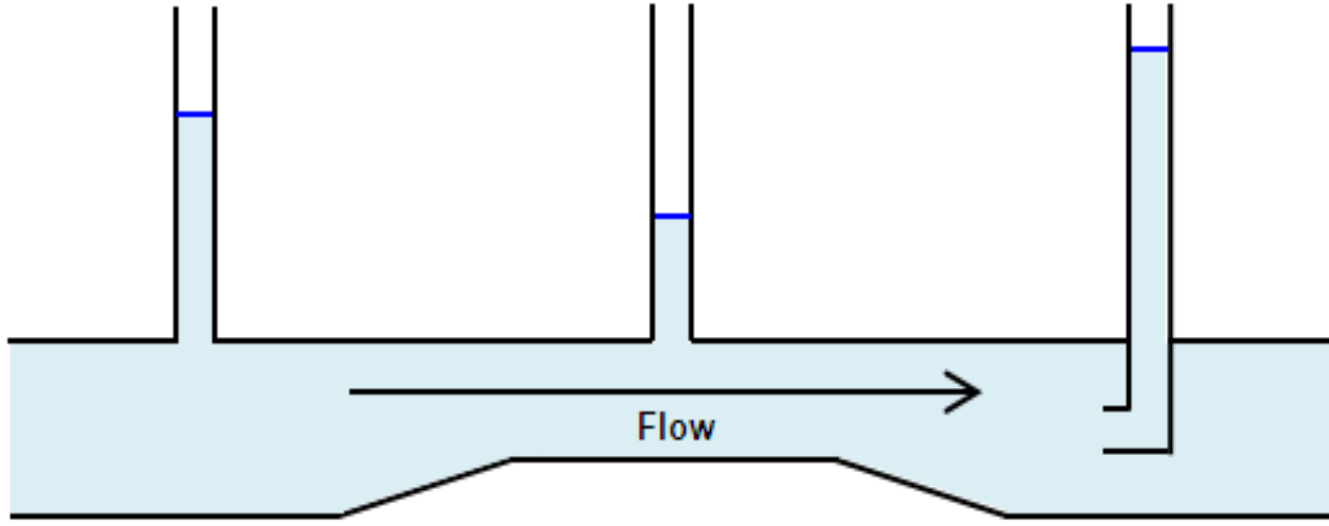
If it is not measured, pump test results will be inaccurate.

$$\text{Energy} = v + P + z = \text{Constant}$$



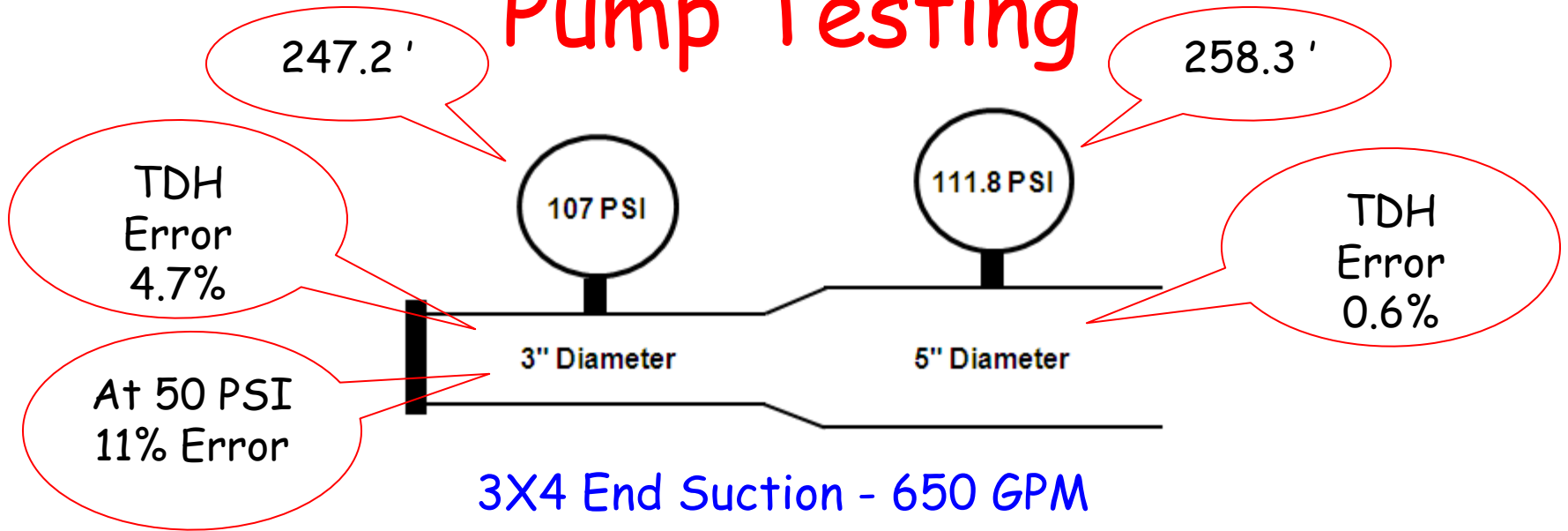
## Piezometer Measurement

$$\text{Energy} = v + P + z = \text{Constant}$$



## Piezometer & Pitot Tube Measurement

# Pump Testing



Velocity 3" = 28.2 ft/sec

Velocity 5" = 10.4 ft/sec

$$h_v = V^2 / 2g$$

3" Section  $h_v = 12.4$  ft

5" Section  $h_v = 1.7$  ft

Actual Pressure = 112.5 PSI (260 ft)



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