



Maximizing Disinfection Reactor Ct via Integration of Chlorine Demand and Decay

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PNWS AWWA Conference | Spokane, Washington

May 7-10, 2013

Presentation Summary

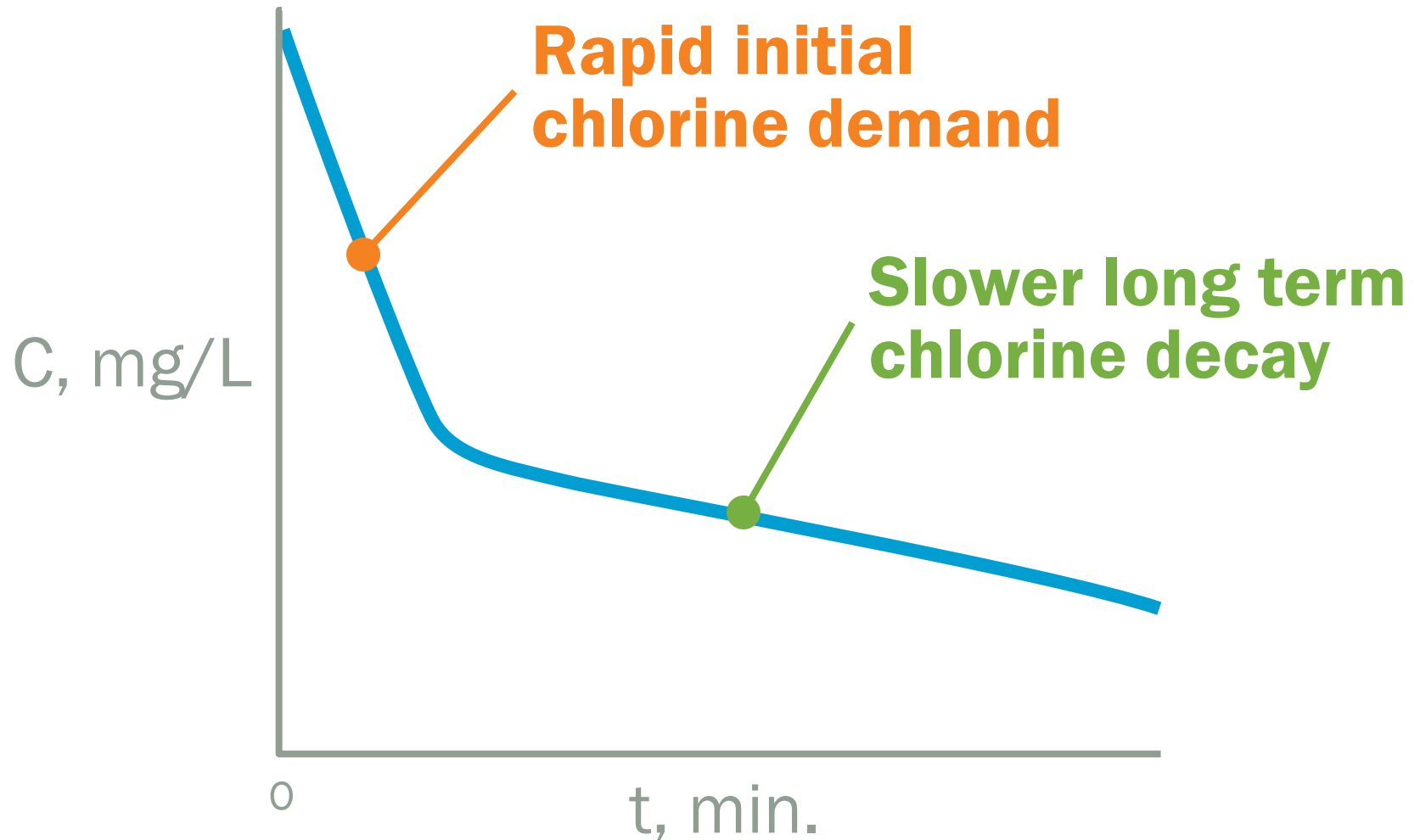
Free Chlorine Ct Computations

- Present Reactor Ct Computations
- Suggested Integration Method for Ct
- Two-stage Algorithm for Predicting CDD
- Integration of CDD Algorithm
- Application of CDD Algorithm Integration

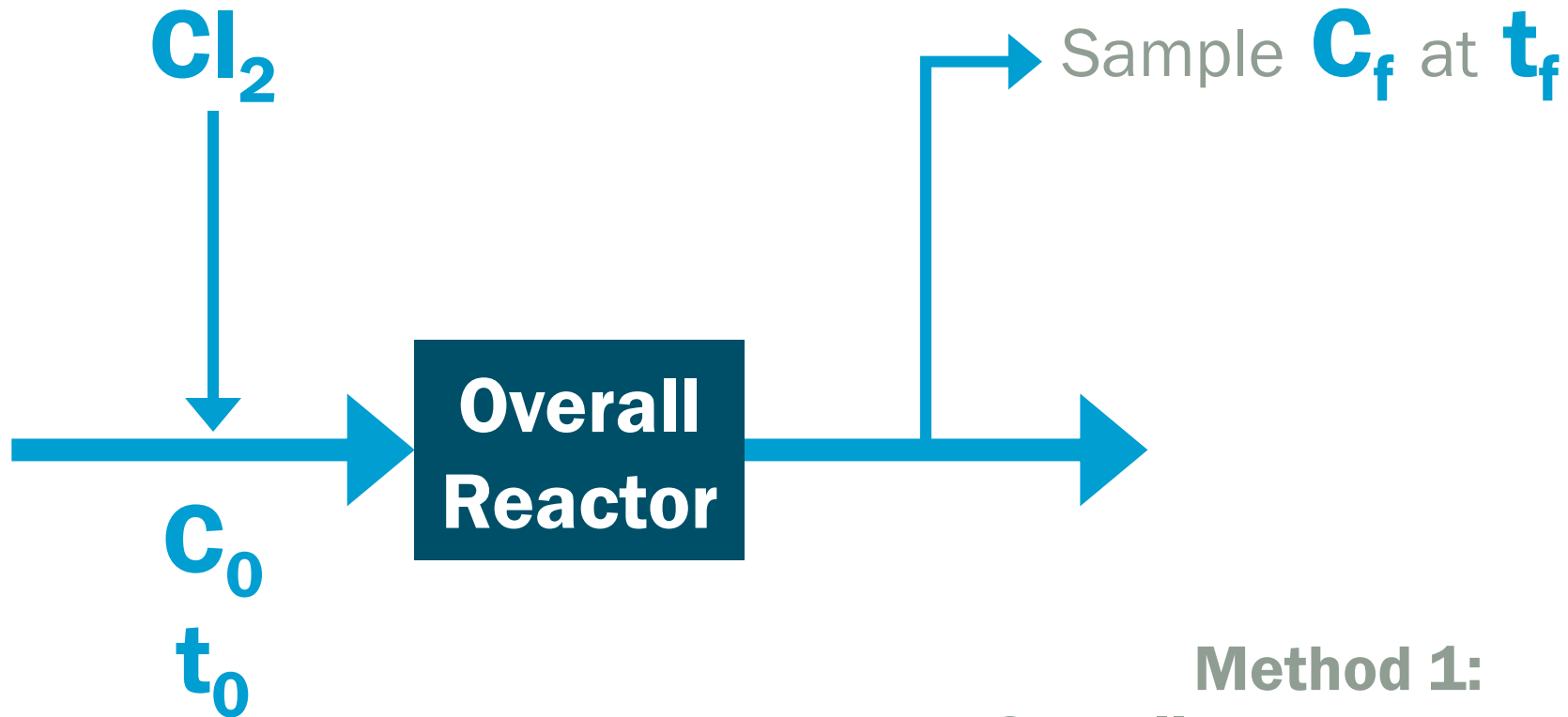
Importance of Ct Computations

- Protect Water Quality
 - Pathogen inactivation
 - DBP Minimization
- Assure compliance with disinfection regulations
- Meet regular reporting requirements

Typical CDD Profile

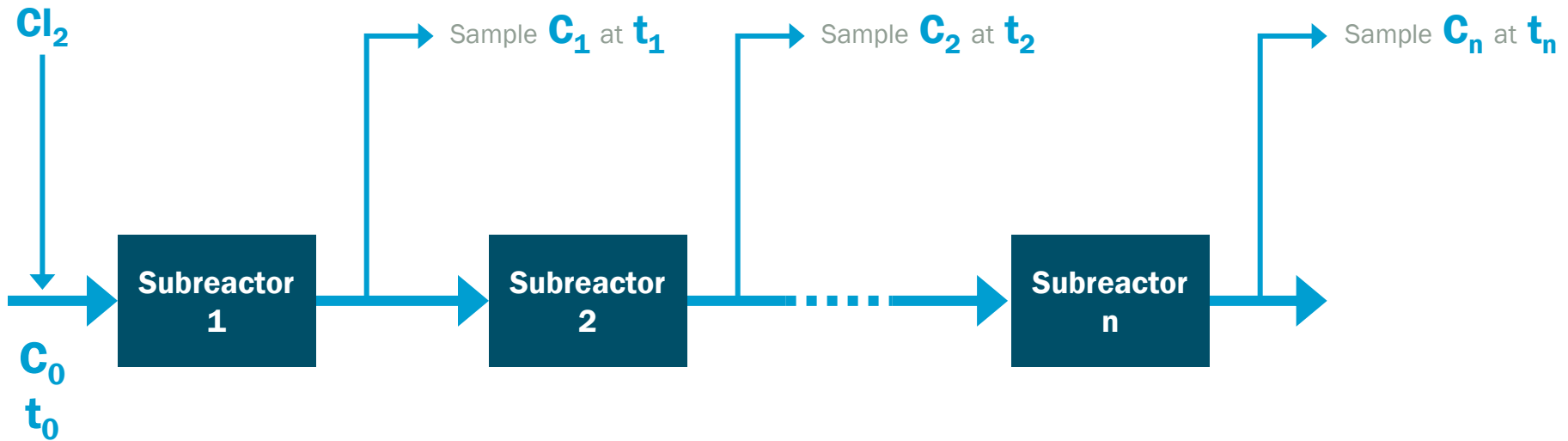


Two Existing Simple Methods to Compute Ct



Method 1:
Overall reactor sampling
 $Ct = C_f \times t_f$

Two Existing Simple Methods to Compute Ct



Method 2:
Intermediate reactor sampling

$$Ct = \sum_{j=1}^{j=n} C_j(t_j - t_{j-1})$$



Existing methods

- Only accounts for reactor discharge concentration
- Ignores added value of CDD within reactor

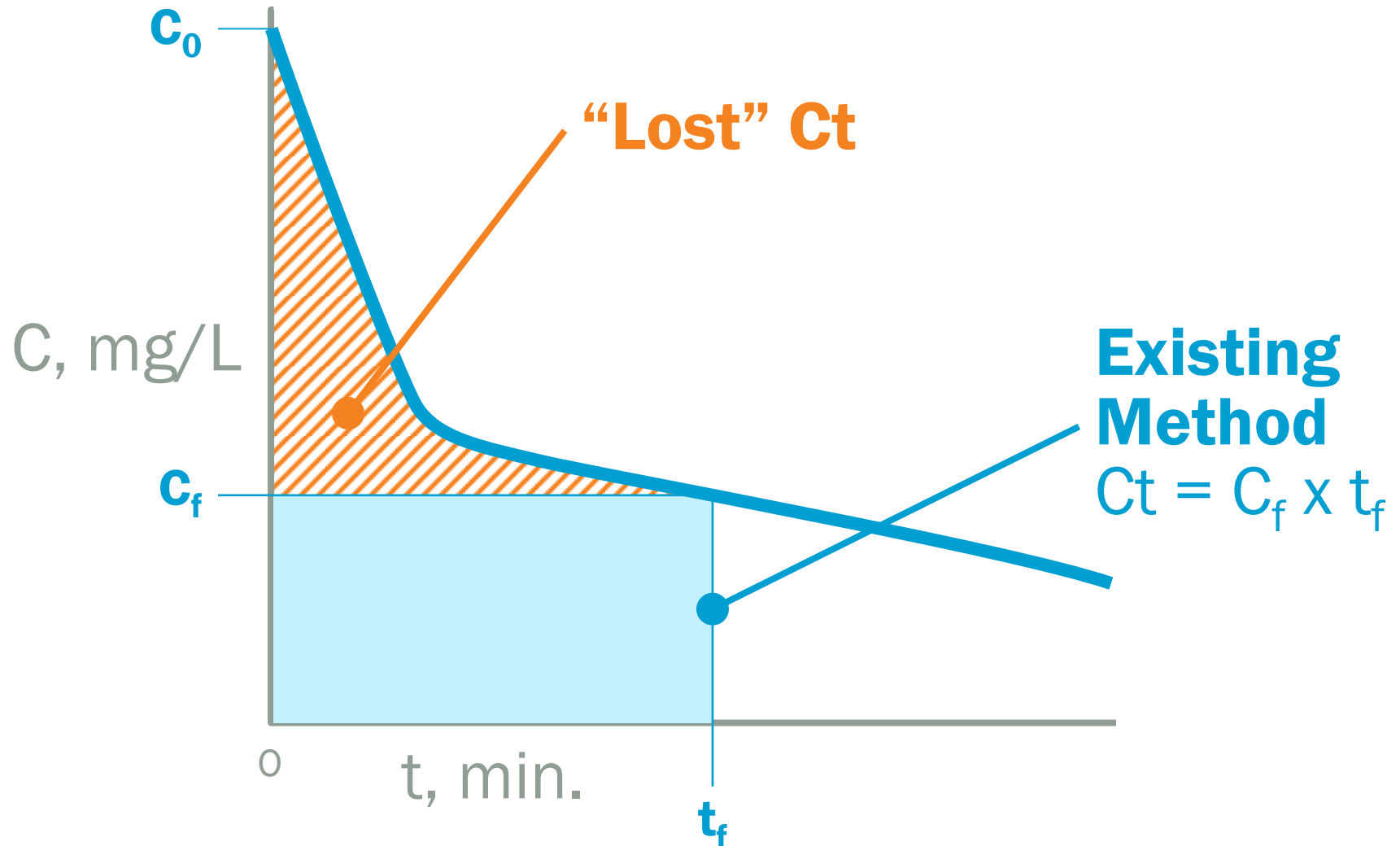
Is there a better way?

Yes!

New Method

- Mathematical model for CDD
- Integrate model
- Account for “lost” Ct value
- Helps when available Ct is “tight” or water is reactive

Existing Method vs. New



CDD Algorithms


General form to predict C versus t

$$C = f \left(\begin{array}{l} \text{time, temp, DOC, pH,} \\ \text{oxidizable substances, others} \end{array} \right)$$

CDD Algorithms

The most basic, simplified form

Where **k** is a rate constant

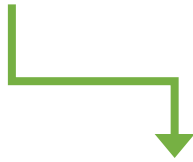
$$C = C_0 e^{-kt}$$


CDD Algorithms

A more elaborate and accurate form

A

proportionality constant between
rapid demand and slow decay



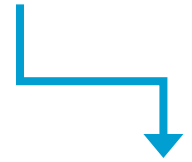
k

rate coefficient for
rapid initial demand



l

rate coefficient for
slower long term decay



$$C = C_0 A e^{-kt} + C_0 (1-A) e^{-lt}$$

For short term applications,
can set $A = 1$ and ignore 2nd term

Yet Another Algorithm Twist

Rate constants vary with temperature!

Higher temperatures increase CDD

- Use Arrhenius Law and van't Hoff equation

$$d(\ln k)/dT = \Delta H^0 / (R_g T^2)$$

$\Delta H^0 = 15,048$ cal/gm-mole; $R_g = 1.987$ cal/^oK-gm-mole
Std. State Enthalpy Change

$$k = k_s \text{EXP}[\Delta H^0 / (R_g T_s)] \text{EXP}[- \Delta H^0 / (R_g T)] \quad \text{eq. 2}$$

$$C = C_0 A e^{-kt} + C_0 (1-A) e^{-lt}$$

$$l = l_s \text{EXP}[\Delta H^0 / (R_g T_s)] \text{EXP}[- \Delta H^0 / (R_g T)] \quad \text{eq. 3}$$



Scare you?

It's not so bad!

Combine equations

1, 2, and 3.

It's simple to
integrate, right?

Not so fast!

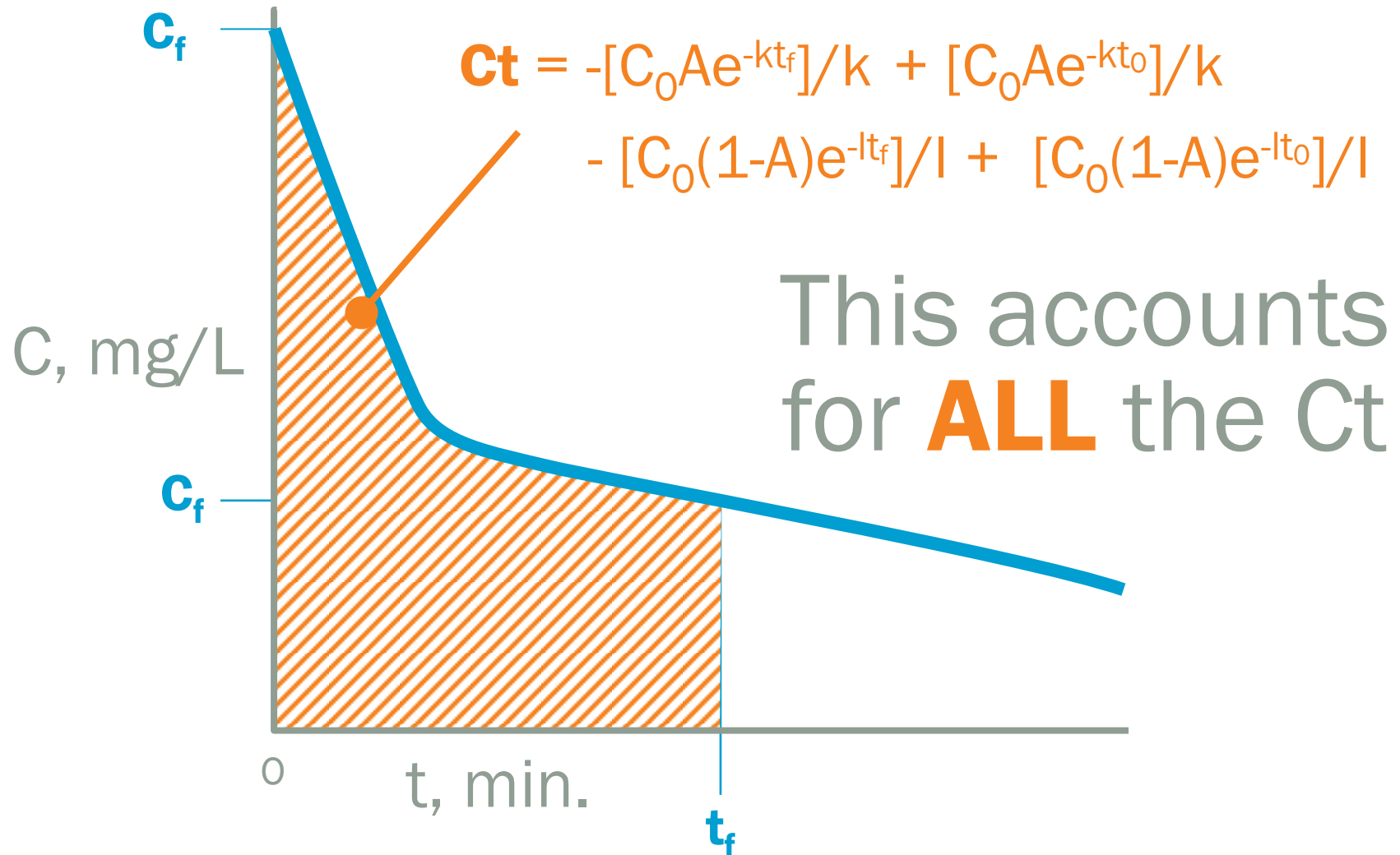
CDD Integration for Constant Temperature

$$Ct = \int C dt$$

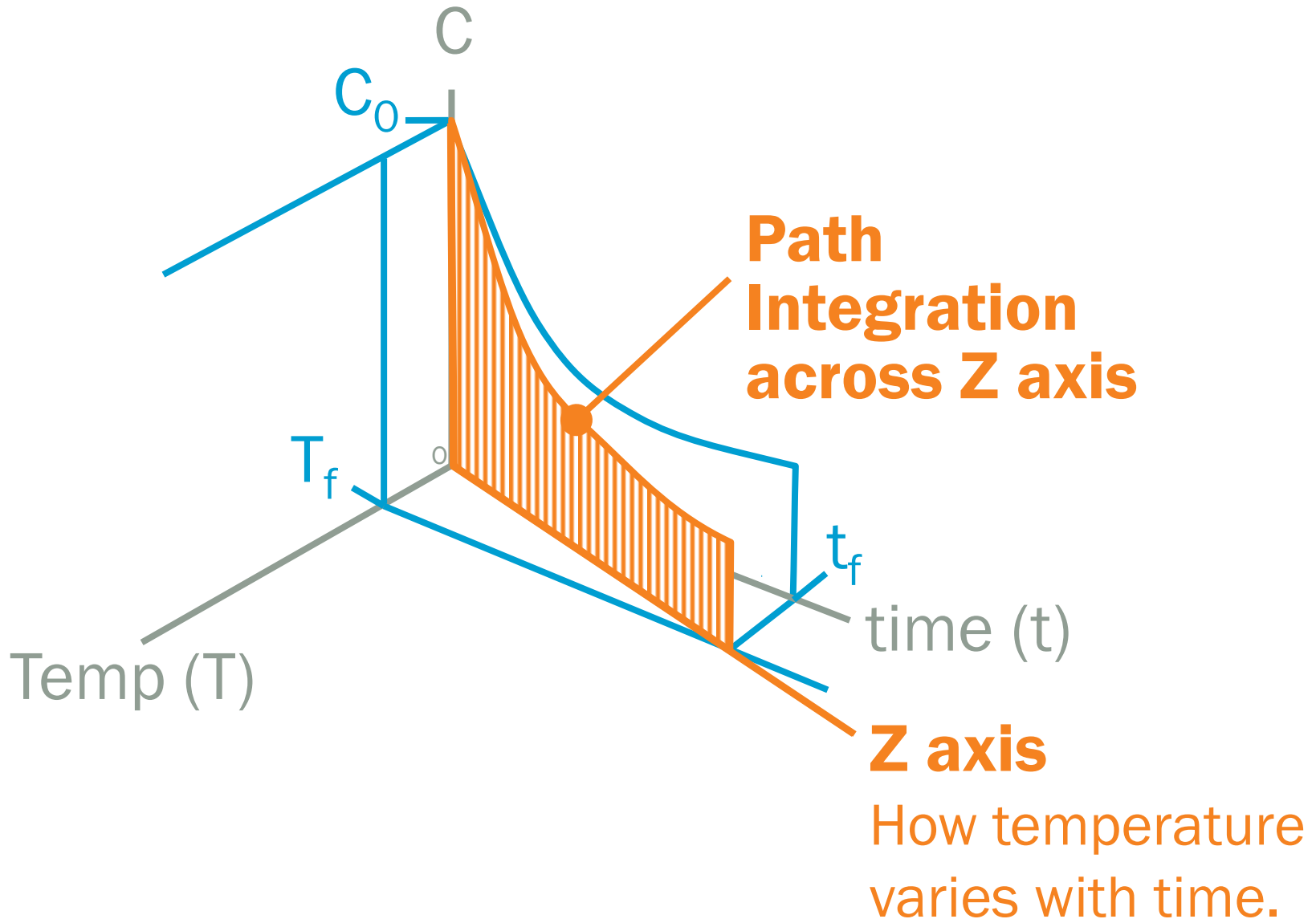
$$Ct = \int_{t=t_0}^{t=t_f} C_0 [Ae^{-kt} + (1-A)e^{-lt}] dt$$

- Analytical integration works at constant temperature
- Not true for varying temperature

CDD Integration for Constant Temperature

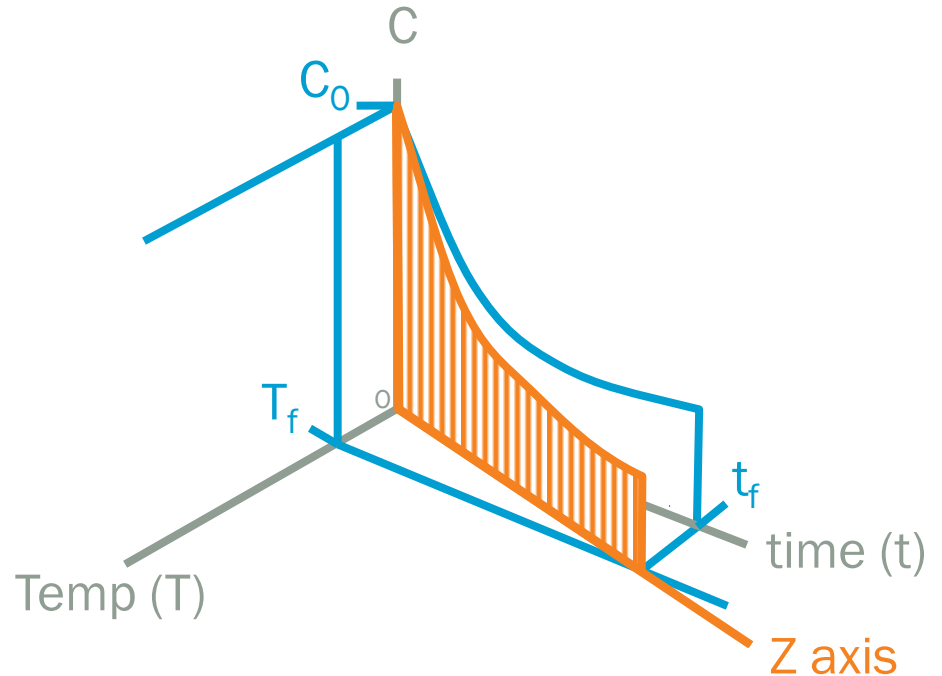


CDD Varies with Time and Temperature



Integration for Varying Temperature

- For simplicity, assume $T = \text{linear } f(t)$
- Re-express T and t in equations 1, 2, and 3 in terms of Z
- *Cannot integrate analytically*
- Resort to numerical integration
 - Use Simpson's Rule
 - Slice curve into numerous parabolic segments
 - Add up segment areas under the curve



Now what?

Next Steps

- Perform lab test to measure CDD constants
- Apply math
 - There's a free App for that!
- When to apply this method?
- Will regulators accept this method?

Example Computations

NW City “X” WTP

Existing Method

GIVEN:

- 1.0 log inactivation credit via disinfection (direct filtration)
- Clearwell Volume: 325,000 gallons
- $t_{10}/t = 0.51$
- Flow = 8.4 mgd (5,833 gpm)
- pH = 7.8
- Temperature $T_0 = 19^\circ\text{C}$ (292° K)
- Temperature $T_f = 20^\circ\text{C}$ (293° K)
- $C_f = 0.8$ mg/L as Cl_2

Integration Method

GIVEN:

- Same clearwell conditions
- $A = 0.314$
- $k_s = 0.0163$ min⁻¹
- $I_s = 0.00017$ min⁻¹
- $T_s = 292^\circ\text{K} = 19^\circ\text{C}$

Empirical values determined from City “X” CDD Study

Example Computations

NW City “X” WTP

Existing Method

- $t_f = (325,000)(0.51)/5,833$
= 28.4 minutes
- $Ct \text{ (available)} = C_f \times t_f = (0.8)(28.4) =$
22.7 mg-min/L
- $Ct \text{ (required)} = 24.4$ mg-min/L from
Ct tables for 1.0 log inactivation
- **Log inactivation achieved =**
22.7/24.4 = 0.9
- Just barely miss the inactivation
target
- Causes City “X” to prechlorinate for
added Ct
- This practice aggravates DBPs

Integration Method

- $t_f = (325,000)(0.51)/5,833$
= 28.4 minutes
- $Ct \text{ (available)} =$ **24.4** mg-min/L
- $Ct \text{ (required)} = 24.4$ mg-min/L from
Ct tables for 1.0 log inactivation
- **Log inactivation achieved =**
24.4/24.4 = 1.00
- Improvement in log inactivation
over traditional method > 7%
- Improvement may be small, but
important in some circumstances
- In this case...
no need to prechlorinate!

Summary

- Account for **ALL** reactor Ct, not just discharge value
- Determine CDD reaction variables
- Integrate CDD operating equations
- More useful for reactive waters
- Optimize disinfection reactor performance
 - Use less chlorine
 - Reduce disinfection byproducts

Spend same time
on the math...

**with better
results!**



Questions?

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